

# Mitigation of H2S Spikes in Molecular Sieves Gas Drying

Arkema Molecular Sieves

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### Introduction

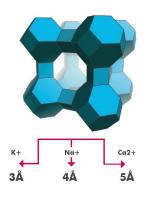
- Molecular sieves are used to dry gas to very low dew points (0.1 ppmv)
- Reliable, but not free of operational challenges (contamination, process limitations, process upsets)
- One of those challenges is H<sub>2</sub>S spikes
  - Off-spec gas
  - Disruption to downstream equipment
  - Metallurgy selection/corrosion
  - Dealumination of sieves
  - Safety concerns
- H<sub>2</sub>S spikes can be mitigated
  - Operation
  - Design

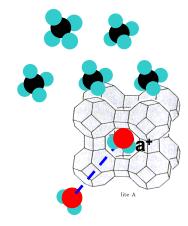




## What are Molecular Sieves?

- Zeolite based adsorbents
  - Crystalline structure with pores/channels
  - Electronic Activity
  - Large Surface Area
- Zeolite + binding clay → MS Beads/Pellets
  - Type
  - Grade
  - Pore Size
  - Media Size
- Separate impurities from fluid





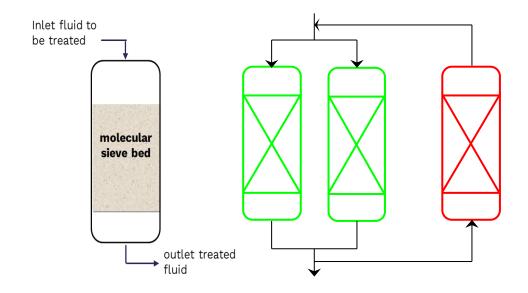






## **Industrial Adsorption**

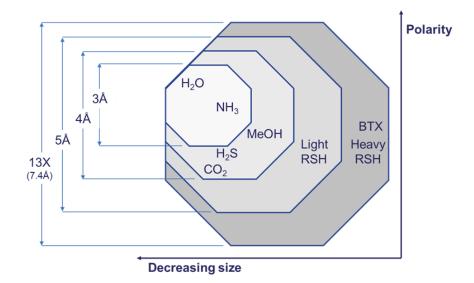
- MS Beads/Pellets loaded into fixed beds (2+)
- Adsorption
  - Capacity equilibrium and dynamic capacity
  - Fixed or BT cycles
- Regeneration (desorption)
  - Slip stream/alternate gas
  - High temperature
  - Cooling step

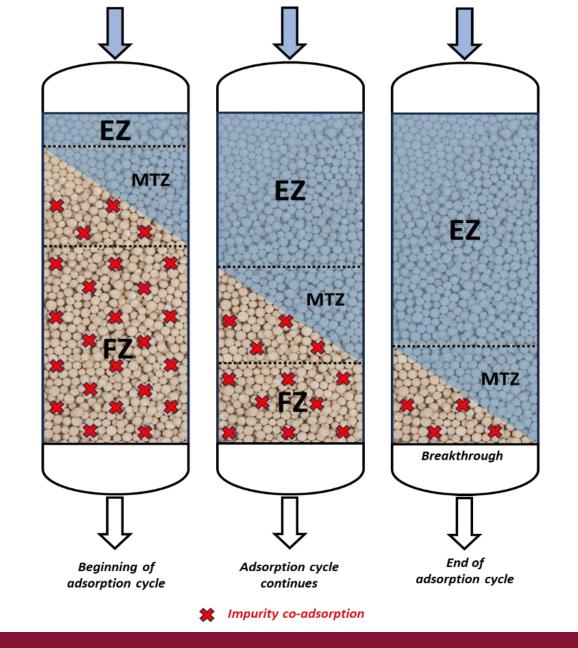




## **Adsorption Zones**

- Adsorption Zones
  - Equilibrium (EZ) saturated with impurities
  - Mass Transfer (MTZ) concentration gradient
  - Fresh (FZ) unused portion of bed
- Zone Evolution
- Water smallest, most polar









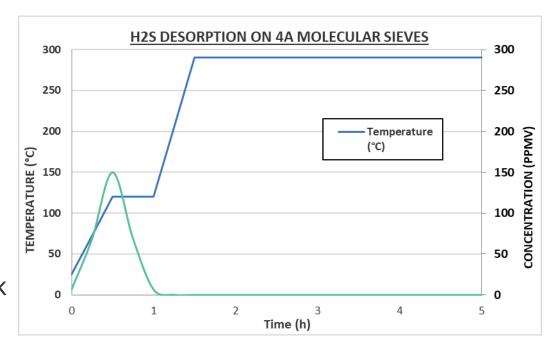
## **H2S Desorption Peak**

#### Use of 4A molecular sieves

- Efficiency (capacity and regeneration)
- H2S can co-adsorb in the MTZ & FZ

#### Desorption Peak

- H<sub>2</sub>S desorbs more easily than water
- Peak Occurs around 80 120°C (176 248°F)
- 5 -10 ppmv H2S in feed  $\rightarrow$  100 150 ppmv peak





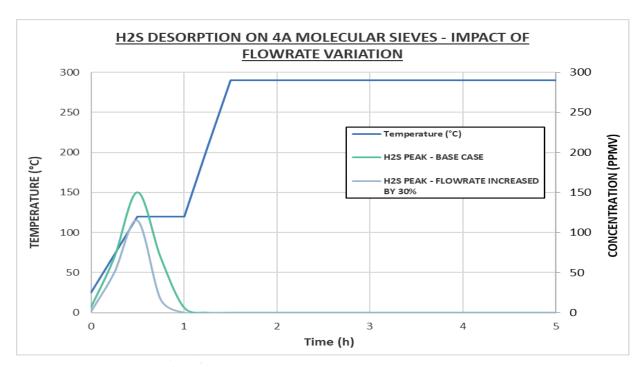


# H2S Spike Mitigation in Operation

## Regeneration Modifications

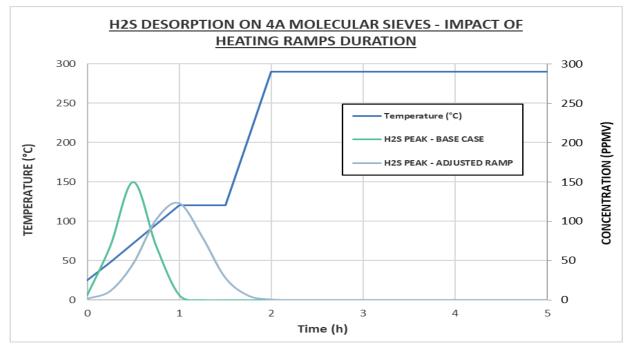
#### Increased regeneration flow

- Increased Regen Gas Consumption (~30%)
- Dilutes H<sub>2</sub>S peak from 150 to 115 ppmv



#### Slower temperature ramp

- Reduce temperature ramp from 90 to 120 min
- Gradually desorbs H<sub>2</sub>S reducing peak from 150 to 123 ppmv

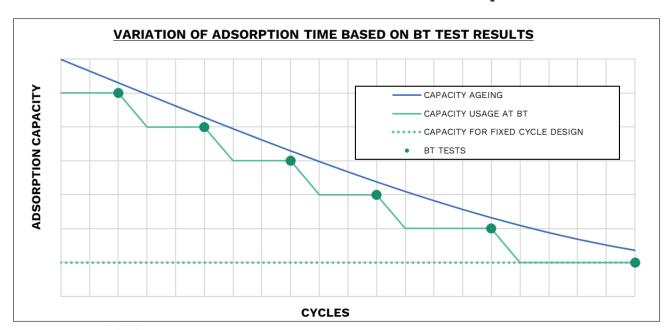


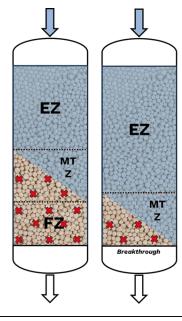


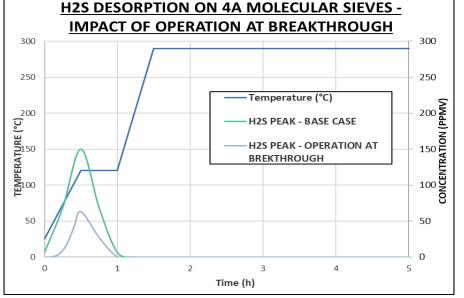


# **Operation to Breakthrough**

- Adsorption time varies based on water loading + aging
  - Adsorption stopped when moisture is detected at the bed outlet
  - Or based on BT testing, the adsorption time can be periodically adjusted
- FZ eliminated → reduced H2S spikes → 150 ppmv to ~60 ppmv







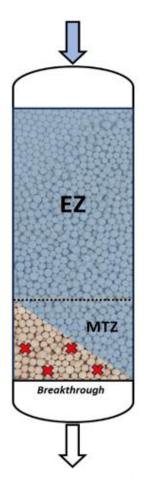


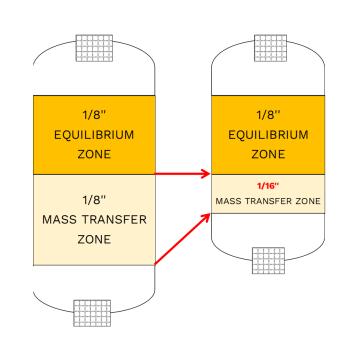


# H2S Spike Mitigation in Design

### **MTZ Reduction**

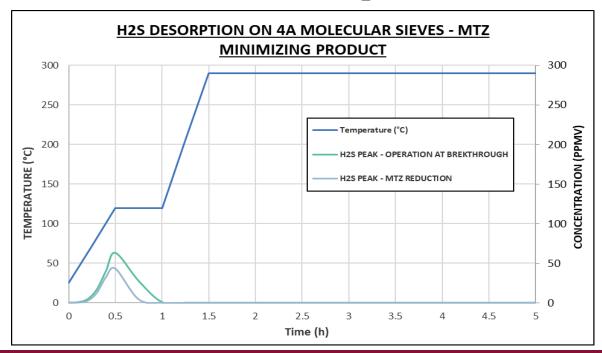
#### Molecular Sieves Size – large vs small





#### **Optimized Product/Specialty Grade**

- Selection of correct clay binder
- Optimized/Controlled manufacturing → improved adsorption kinetics
- MTZ reduced by 30%  $\rightarrow$  H<sub>2</sub>S peak of 44 ppmv

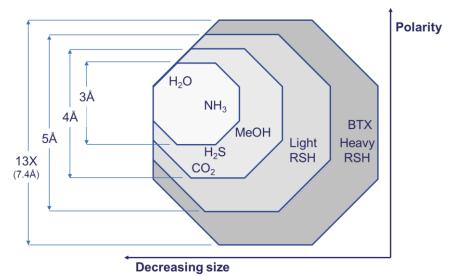




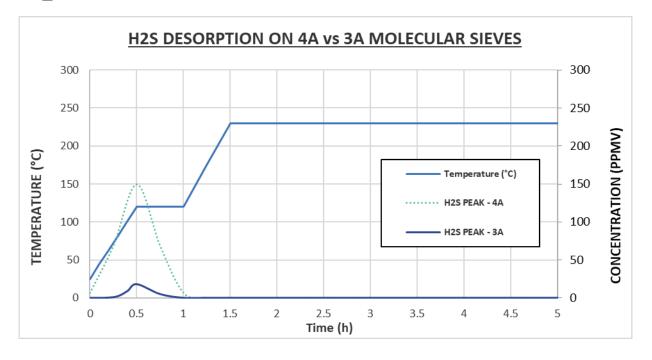


## **3A Molecular Sieves**

- Selective adsorption minimizing co-adsorption of H<sub>2</sub>S
- Standard or advanced grades with tightly controlled pore size
- Significant peak reduction vs 4A → H<sub>2</sub>S Peak of 18 ppmv
- Reduced capacity vs 4A sieves



**IN ANY CASE: WATER FIRST!** 

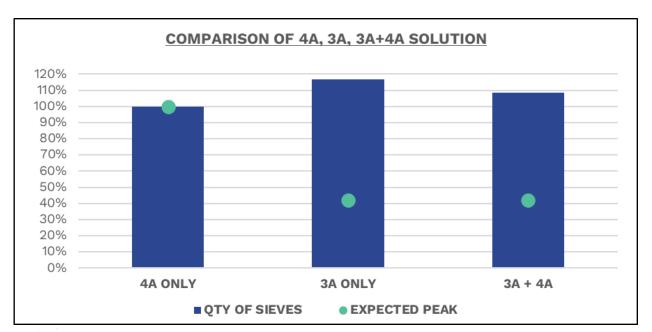


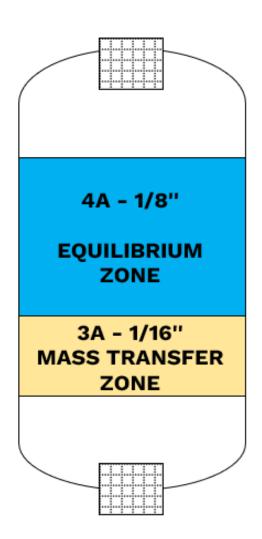




## **Optimized Design Solution**

- Improved 4A + 3A
- Maximizes adsorption capacity while minimizing H<sub>2</sub>S peak
- Design EZ with 4A and MTZ with 3A
- Results in 10% less MS needed than in the 3A solution



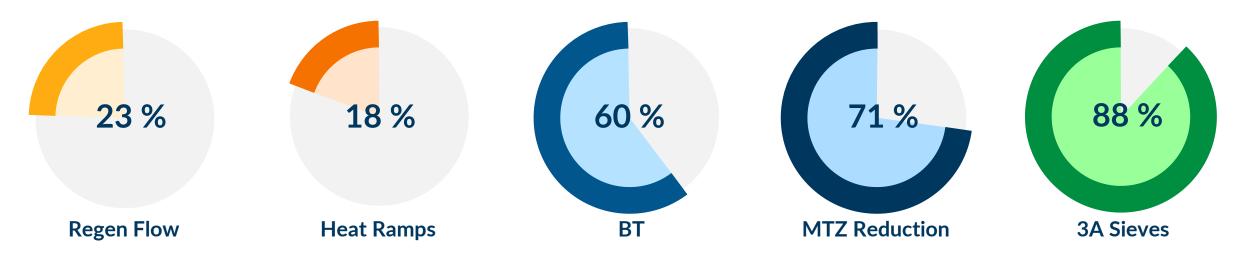






## Conclusion

- H<sub>2</sub>S peaks pose risks/issues for plants if not managed
- H<sub>2</sub>S peaks can be managed in the operational and design phase
- Improvements in H<sub>2</sub>S peaks observed in the Case Study







# Thank you!