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CONRAD SHIPYARD

297'-6" x 54' x 12' INLAND TANK BARGE

VAPOR CONTROL SYSTEM CALCULATIONS

SCALE:	NONE	DATE:	11/19/2012	DWG. NO.
DRAWN BY:	R. ALLUMS	CK'D BY:	R. ALLUMS	C-32
HULL NO.	C1007, C1008	JOB NO.	12-085	REV. 0

VAPOR CONTROL SYSTEM CALCULATIONS - SUMMARY

A. General Description of Vessel:

1.

Builder: CONRAD SHIPYARD Builder's hull numbers: C1007, C1008

Year Built: 2013

 Official Numbers:
 1243651, 1243652

 Owner:
 Canal Barge

 Vessel Names:
 CBC 374, CBC 375

 Vessel Dimensions:
 297'-6" x 54'-0" x 12'-0"

 Service:
 Inland Tank Barge (D/O)

Classification: None

 Max Design Working Pressure of Tanks:
 3.00
 (psig)

 Max Cargo Loading Rate
 5,500
 (bbl/hr)

 Maximum Discharge Rate
 4,300
 (bbl/hr)

VCS Cargoes: See Table 1

Maximum Vapor-Air Mixture Density: 0.35 (Pentane, all isomers) (lbm/ft^3)

Maximum Vapor Growth Rate: 1.54 (Pentane, all isomers) (lbm/ft^3)

B. General Description of Vapor Control System:

[Note: Also see Reference 6 for details of vapor control system.]

1. Pipe:

One (1) 8" diam longitudinal vapor header fitted with a 6" high-velocity PV Valve.

One (1) 8" diam tranverse vapor header with 8" shore connection valves.

One (1) 8" diam branch line off longitudinal header to each cargo tank.

(See Reference 6 for system layout)

2. High Velocity PV Valve:

 Model:
 ERL 6" SUPERAC PV-6

 Pressure Setting:
 1.50
 (psig)

 Vacuum Setting:
 0.5
 (psig)

 PV Valve Flow Capacity:
 See Att. 1
 (bbl/hr)

3. Spill Valve:

Model: None installed

Pressure Setting: N/A

4. Vapor Recovery Hose:

Diameter: 8" (assumed)
Length: 50' (assumed)

5. Cargo Tank P-V Valves: (One central P/V valve only, no individual tank P-V

valves)

Model: See #2 above.

Pressure Setting: 1.50 (psig)
Vacuum Setting: 0.5 (psig)

C. VCS Calculations:

1. Cargo Authority:

The vapor collection system installed on this barge is designed for Grade A and lower petroleum products and Type II/III chemicals. Typical cargoes to be carried by this barge are listed in Table 1. These cargoes are to be listed in the Cargo Authority Attachment (CAA) of the barge's Certificate of Inspection. Note that Table 1 is not intended to be an all-inclusive list and the CAA should therefore not be limited to these cargoes. Other cargoes with less restrictive or equal characteristics shall also be included on the CAA. VCS Categories 1 through 7 are requested.

2. Determining Vapor-Air Mixture Density and Vapor Growth Rate:

Of the cargoes carried, Pentane has the highest vapor-air mixture density. Pentane also has the greatest vapor growth rate. (See Table 1)

3. The Maximum Liquid Transfer Rate as Imposed by the Capacity of the Cargo Tank Venting System: (Ref: 46 CFR 39.20-11)

Tanks #1 P/S are the farthest tanks from the High-Velocity P-V Valve in terms of total equivalent pipe length. Using factors from Reference 4 and 9, the total equivalent length of pipe is calculated for this path. This calculation is shown in Table 2.

Using Darcy's equation, and friction factors selected as appropriate for the pipe size, and the maximum liquid transfer rate, the pressure drop along the VCS piping from tank #1P to the P-V Valve is calculated using the total equivalent length of pipe from Table 2. The pressure drop calculations were done for the maximum loading rate (5,500 BBL/hr) for this barge. This maximum loading rate is based on loading one tank at a time. This calculation is shown in Table 3.

Conclusions:

Using a 5,500 bbl/hr maximum liquid transfer rate (for Pentane and lower cargos), the vapor-air mixture and air-equivalent volumetric flow rates for each cargo are shown in Table 3. The greatest pressure drop in the cargo tank venting system is 0.25 psig for Pentane cargo. At a pressure relief setting of 1.5 psig, the high-velocity P-V valve has an adequate flow capacity (see attachment 1). The greatest total back pressure imposed on the tanks by the cargo tank venting system (2.89 psig) does not exceed the design working pressure of the cargo tanks (3.00 psig). Also, the vacuum relieving capacity of the P-V Valve has been checked against the maximum discharge rate and has been found to have adequate vacuum relieving capacity (see Table 3).

4. The Maximum Liquid Transfer Rate as Imposed by the Relieving Capacity of the Cargo Tank Spill Valves:

No spill valves are installed on this barge.

5. The Maximum Liquid Transfer Rate as Imposed by the Set Point of the Overfill Alarm:

At the maximum cargo loading rate of 5,500 bbl/hr, required overfill alarm set points have been calculated such that the person in charge of the transfer operations has more than 60 seconds from the overfill alarm to stop the transfer operations before the tank overflows. (See attached overfill alarm set point calculation sheets.) The overfill alarms will need to be set at or below these calculated levels to ensure that the VCS complies with 46 CFR 39.20-9. In addition, the overfill alarms must also be set at or below a capacity of 98.5% to comply with 33CFR155.775.

6. The Maximum Liquid Transfer Rate as imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 46 CFR 39.30-1(d)(3):

This requires the sum of the pressure drop along the longest path from the cargo tank to the vessel vapor connection and the back pressure at the facility vapor connection not to exceed 80 percent of the pressure setting of any pressure relief valve in the system. Tanks #1 P/S are the farthest from the facility vapor connection (in terms of total equivalent length of pipe). The total equivalent length from cargo tank #1P to the facility vapor connection is given in Table 4.

Using Darcy's equation, and friction factors selected as appropriate for the pipe size, and the maximum liquid transfer rate, the pressure drop along the VCS piping from tank #1P to the facility vapor connection is calculated using the total equivalent length of pipe from Table 4. These calculations are shown in Table 5.

Conclusions:

Pressure drop at the maximum liquid transfer rate of 5,500 bbl/hr (for Pentane and lower cargoes) along this path for each cargo is given in Table 5. The highest pressure drop (for Pentane) does not exceed 80 percent of the P-V valve pressure setting. If the pressure drop between the facility vapor connection and the shore facility's pressure sensor is known, it should be added to the pressure drop along this path to ensure that the total pressure drop does not exceed 80 percent of the P-V valve pressure setting.

7. Graph as Required by 46 CFR 39.30-1(b)(3): See attached.

Determination of Vapor-Air Mixture Density & Vapor Growth Rate

Table 1

CHRIS Code	Name	Туре	VCS Category	Liquid S.G.	*Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (lb/ft^3)	Vapor Growth Rate	Max. Loading Rate	Vapor Volumetric Flow Rate (bbl/hr)	Air Equivalent Volumetric Flow Rate (bbl/hr)	in VCS (See Table 3) (psig)	Pressure Drop to Facility Connection in VCS (See Table 5) (psig)
1 ACN	Acrylonitrile	111	4	0.81	5.00	1.80							
2 ACT	Acetone	D	1	0.79	10.00	2.00		1.20					
3 ACP	Acetophenone	D	1	1.03	0.60	4.14	0.085		5,500				
4 AND	Adiponitrile	11	1	0.95		3.73							
5 AEC	Amyl acetate (all isomers)	D	1	0.88	0.33	0.10		1.01	5,500 5,500				
6 AAI	Amyl Alcohol (iso-, n-, sec-, primary)	D	1	0.82	0.30	3.04 1.41	0.079	-					
7 ATN	Acetonitrile	m	3	0.78 1.05		3.73		1.00					
8 BAL	Benzyl Alcohol	D III	4	0.88	4.50	2.80		1.25					
9 BNZ	Benzene Benzene, Toluene, Xylene mixtures (10%	iji.	-	0.00	4.00	2.00	0.111	1,24		-			
10 BTX	Benzene or more)	111	1	0.84	7.30	2.80	0.138	1.25	5,500	6875	9252	0.065	0.14
11 BAR	Butyl Acrylate (iso-, n-)	111	2	0.90		4.42	0.086	1.01	5,500	5566	5908		
12 BAX	Butyl Acetate (all isomers)	D	1	0.87	0.60	4.00	0.085	1.01	5,500				
13 IAL	Butyl Alcohol (iso-)	D	1. 1.1	0.81	0.90	2,60		1.02	5,500				
14 BAN	Butyl Alcohol (n-)	D		0.81	0.50	0.10		1.01	5,500				
15 BAS	Butyl Alcohol (sec-)	D	1	0.81	1.30	2.60		1.03					
16 BAT	Butyl Alcohol (tert-)	D	1	0.78		2.60		1.06					
17 BPH	Butyl Benzyl Phthalate	D	1	1.12		10.80	0.077	1.00					
18 BAD	iso-Butyraldehyde	Ш	1	0.80		2.50		1.16	_				
19 BTR	n-Butyraldehyde	III	1	0.80		2.50 5.11	0.131	1.16					
20 BUE	Butyl Toluene	D	1	0.85 1.02	0.10	3.90		1.00					
21 CLS	Caprolactam Solutions	D	1	0.95		3.40	0.077	1.00					-
22 CCH	Cyclohexanone (Anolone)	111	1	0.95		3.40	0.078	1.00	5,500				
23 CHA	Cyclohexylamine	D	1	0.87		2.90	0.116	1.09					
24 CHX 25 CHN	Cyclohexane Cyclohexanol	D	1	0.95				1.00				0.023	0.05
26 CPD	1,3-Cyclopentadiene dimer (molten)	D	2	0.69			0.080	1.01	5,500		5677	0.024	
27 CMP	p-Cymene	D	1	0.86		4.62	0.078	1.00	5,500	5512			
28 CRB	Chlorobenzene	111	1	1.11	0.80	3.88	0.087	1.02	5,500				
29 CRS	Cresols	111	1	1.05	0.08	3.72	0.077	1.00					
30 CUM	Cumene	D	1.	0.86	0.60	4.20	0.085	1.01	5,500				
31 IDA	Decaldehyde (iso-)	D	1	0.83		5,00	0.076	1.00					_
32 DAL	Decaldehyde (n-)	D	1	0.83		5.01	0.076	1.00					
33 DCE	Decene	D	1	0.74		4.80	0.078	1.00					
34 DAX	Decyl Alcohol (all isomers) (Decanol)	D	1	0.83		5.30	0.076	1.00					
35 DBZ	Decylbenzene (n-)	D	- 3	0.86		7.52	0.076	1.00					
36 DAA	Diacetone Alcohol	D	1	0.97	0.10	4.00	0.078	1.00					1
37 DCH	1,1-Dicholoroethane	Ш	1	1.18		3.41 9.59	0.188	1.20					
38 DPA	Dibutyl Phthalate (ortho-)	D	1	1.05 0.87	0.00	4.62	0.078	1.00					
39 DEB	Diethybenzene	D	1	1,12		3.66							
40 DEG	Diethylene Glycol	III	3		1.00	2.50		1.02					-
41 DEN 42 DBL	Diethylamine Diisobulylene	D	1	0.72				1.04					0.0
43 DIK	Diisobutyl Ketone	D	3	0.81	0.16			1.00	5,500	5518	5623	0.024	
44 DIP	Diisopropanolamme	111	1	0.98		4.59		1.00	5,500	5501	5507	0.023	
45 DIX	Diisopropylbenzene (all isomers)	D	1	0.86	0.03	5.60	0.077	1.00					-
46 DTL	Dimethyl Phthalate	D	1	1.19									-
47 DOP	Dioclyl Phthalate	D	1			_					-		
48 DPN	Dipentene	D	1										
49 DIL	Diphenyl	D	1			5.31							
50 DDO	Diphenyl, Diphenyl Ether Mixtures	D	1	1.07									
51 DMF	Dimethylformamide	111	1										
52 DPE	Diphenyl Ether	D	1	1.07	0.01	5.87 4.63							-
53 DPG	Dipropylene Glycol	D	3	1.03									
54 DPX 55 DFF	1,1-, 1,2-, 1,3-Dichloropropane	D	1	0.75						-			
	Distillates Flashed Feed Stocks Distillates Straight Run	D	1	0.73									_
56 DSR 57 DOZ	Distillates Straight Run Dodecene (all isomers)	D	1	0.76			0.077	1.00					0.0
58 DDB	Dodecylbenzene	D	1	0.86				1.25	5,500	6875	12196	0.112	
59 EAC	Ethyl Acrylate	Ш	2	0.93	2.00	3.50	0.100	1.04	5,500	5720	6543	0.032	
60 EAI	2-Ethylhexyl acrylate	m	2		0.02	6.35	0.077	1.00	5,500				
61 EEA	2-Ethoxyethyl acetate	D	1	0.97	0.02	4.70							_
62 ETG	Ethoxy Triglycol (crude)	D	1	1.02									
63 ETA	Ethyl Acetate	D	1										
64 EAA	Ethyl Acetoacetate	D	1										
65 EAL	Ethyl Alcohol (Ethanol)	D	1										
66 ETB	Ethyl Benzene	D	1										
67 EBT	Ethyl Butanol	D	1										
68 EBE	Ethyl tert-butyl ether	D	1										
69 EBR	Ethyl butyrate	D	1										
70 ECY	Ethyl Cyclohexane	D	1										-
71 EDC	Ethylene dichloride	III	1			-							
72 EGL	Ethylene Glycol	III	1							-			
73 EMA	Ethylene Glycol Butyl Ether Acetate	D	1		-								
74 EGY	Ethylene Glycol Diacetate	D	1										
75 EPE 76 EEP	Ethylene Glycol Phenyl Ether Ethyl-3-ethoxypropionate	D	1										-
76 EEP 77 EHX	2-Ethylhexanol (Octanol)	D	1										3 0.0
	E-FINALIOVATION (CONTINUI)	D	1										0.0

	CHRIS Code	Name	Туре	VCS Category	Liquid S.G.	"Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (lb/ft^3)	Vapor Growth Rate	Max. Loading Rate	Vapor Volumetric Flow Rate (bbl/hr)	Air Equivalent Volumetric Flow Rate (bbl/hr)	Pressure Drop to PV Valve in VCS (See Table 3) (psig)	Pressure Drop to Facility Connectin in VCS (S Table 5) (psig)
79	ETE	Ethyl Toluene	D	1	0.88		4.15		1.01	5,500				
		Formamide	D	1	1.13	0.10	1.55		1.00	5,500				
		Formaldehyde Solution	101	1	1.13		1.03		1.00	5,500				
	FAL	Furfuryl Alcohol	D	1	1.13		3.40		1.00	5,500				
33	FFA	Furfural	01	1	1.20		3.31	0,078	1.00	5,500				
	GAK	Gasoline Blending Stocks: Alkylates	D	1	0.75		3.40		1.25	5,500				
	GRF	Gasoline Blending Stocks: Reformates	D	1	0.80	12.50	3.40		1.25	5,500				-
	GAT	Gasolines: Automotive	D	1	0.74	12.50	3.40		1.25	5,500			-	-
	GAV	Gasolines: Aviation	D	1	0.71	12.50 12.50	3.40		1.25	5,500				
	GCS	Gasolines: Casinghead	D	1	0.67		3.40		1.25	5,500				
	GPL	Gasolines: Polymer	D	1	0.75		3.40		1.25	5,500				
	GSR GCR	Gasolines: StraightRun	D	1	1.26	0.00	3.17	0.076	1.00	5,500				3 (
	HMX	Glycerine Heptane (all isomers)	D	1	0.68	2,50	3.45		1.05	5,500				5
	HEP	Heptonic Acid	D	1	0.92		4.49		1.00	5,500		5507	0.023	3
	HTX	Heptanol (all isomers)	D	1	0.82	0.04	4.00		1.00	5,500	5504	5525	0.023	
	HPX	Heptene (all isomers)	D	2	0.70		3.40		1.06	5,500	5819	6958	0.037	
	HXS	Hexane (all isomers)	D	1	0.66		3.00	0.142	1.14	5,500	6270	8561		
	HXO	Hexaonic Acid	D	1	0.93	0.01	4.00	0.076	1.00	5,500				
	HXN	Hexanol	D	1	0.82		3.52		1.02	5,500				
	HEX	Hexene (all isomers)	D	2	0.67	8.00	2.90		1,16					
	HXG	Hexylene Glycol	D	1	0.92		1.10		1.00					
01	PH	Isophorone	D	1	0.93	0.01	4.75		1.00					
02	JPF	Jet Fuels: JP-4	D	1	0.81	3.40	4.00		1.07	5,500				
	JPV	Jet Fuels JP-5 (Kerosene, heavy)	D	1	0.82		4.00		1.00					_
	KRS	Kerosene	D	1	0.81	0.15	4.50 2.60		1.00	5,500				
		Methyl Acetate	D	1	0.92		1.10		1.12					_
		Methyl Alcohol (Methanol)	D	1	0.79		4.97	0.079	1.01	5,500				_
		Methylamyl Acetate	D	1	0.86	0.33	3.52		1.01	5,500				_
	MAA	Methylamyl Alcohol	D	1	0.81		1.00		1.00					
		Methylamyl Keytone	III	2			3.00		1.08					
	MAM MBE	Methyl Acrylate Methyl Tert-Butyl Ether (MTBE)	D	1	0.74		3.10		1.00	5,500				
		Methyl Butyl Ketone	D	1	0.81	0.97	3.50		1.02	5,500			0.027	7
		Methyl Butyrate	D	1	0.90		3.53		1.03	5,500	5639	6168	0.029	
	MEK	Methyl Ethyl Ketone	D	1	0.80		2.50	-	1.09	5,500	5995	7135	0.038	
		Methyl Heptyl Ketone	D	1	0.83	0.06	4.90	0.077	1.00	5,500	5507			
	MIK	Methyl Isobutyl Ketone	D	1	0.80	1.15	3.45	0.089	1.02	5,500	5627			
	MMM	Methyl methacrylate	111	2	0.94	2.02	3.45		1.04	5,500				
	MNA	Methyl Naphthalene	D	1	1.02		4.91	0.076	1.00					
	MNS	Mineral Spirits	D	1	0.75		4.30							
	MPL	Morpholine	111	1	1.00		3.00		1.02					
	MRE	Myrcene	D	1	0.80		4.70		1.00					
	PTN	Naphtha: Petroleum	D	1	0.74		3.50		1.00					-
	NSV	Naphtha: Solvent	D	1	0.87		3.50 4.30		1.00					
	NSS	Naphtha: Stoddard Solvent	D	1	0.78	0.19	4.30		1.00		-			
	NVM	Naphtha: VM&P	D	1	0.77		4.40		1.01	5,500				
	NAX	Nonane (all isomers) Nonene (all isomers)	D	2	0.73	-	4.30	200	1.01	5,500				5
	NON NNS	Nonyl Alcohol (all isomers)	D	1	0.94		5.00							
	NNP	Nonyl Phenol	D	1	0.95		7.60					5512	0.023	3
	NPM	1-, 2-Nitropropane	III	1			3.06		1.02	5,500				
	OAX	Octane (all isomers)	D	1		0.79			1.02					
	OCX	Octanol (all isomers)	D	1			4.48							_
	OTX	Octene (all isomers)	D	2			3.90	-	1.02					
	WTO	Oil, fuel: No. 2	D	1			8.00			5,500				
35	OTD	Oil, fuel: No. 2-D	D	1			3.40		1.01	5,500				
	OFR	Oil, fuel: No. 4	D	1	0.90		3.40						-	
	OFV	Oil, fuel: No. 5	D	1			3.40						-	
	OSX	Oil, fuel: No. 6	D	1	0.95		3.40			-				
	OIL	Oil, misc: Crude	D D	1			3.40			5,500				
	ODS	Oil, Misc: Diesel	D	1	0.90		1.00							_
	OLB	Oil, Misc: Lubricating	D	1			1.00			-				
	ORL OTB	Oil, Misc: Residual Oil, Misc: Turbine	D	1			5.40							
	PTY	Pentane (all isomers)	D	5			2.50		1.54					9
	PTE	Pentane (all isomers)	D	5			2.40	_						
	PIN	Pinene	D	1	0.86		4.70			5,500	-			5
	PLB	Polybutene	D	1		-	1.00						0.023	3
	PGC	Polypropylene Glycol	D	1	1.01		1.00				-			
	IAC	Propyl Acetale (iso-)	D	1	0.89				1.04		5698			
	PAT	Propyl Acetate (150-)	D	1	-				1.04	5,500	5704			-
	IPA	Propyl Alcohol (iso-)	D	1			2.07		1.06					
	PAL	Propyl Alcohol (n-)	D	1			2.07	0.082						
	PBY	Propylbenzene (all isomers)	D	1	0.86	0.20	4.14							
	IPX	iso-Propylcyclohexane	D	1			4.35							
	PPG	Propylene Glycol	D	1			2.62						_	
	PGN	Propylene Glycol Methyl Ether Acetate	D	1		-	3.11							
57	PTT	Propylene Tetramer	D	1			1.00							
58	SFL	Sulfolane	D	1			4.14							
	STY	Styrene	10	2								-		
	TTG	Tetraethylene Glycol	D	1	1.20	0.01	6.70	0.076	1.00	5,500	550	551	0.02	-

	CHRIS Code	Name	Туре	VCS Category	Liquid S.G.	*Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (lb/ft^3)	Vapor Growth Rate	Max. Loading Rate		Volumetric Flow Rate (bbl/hr)	Drop to PV Valve in VCS (See Table 3) (psig)	Connection in VCS (See Table 5) (psig)
161	THN	Tetrahydronaphthalene	D	1	0.97	0.04	4.56							
	TOL	Toluene	D	1	0.87	1.50	3.14	0.091	1.03				0.029	
	TCN	1,2,3-Trichloropropane	11	3	1.39	0.15	5.60					5633		
	TCP	Tricresyl Phosphate (less than 1% of ortho	D	1	1.16	0.01	12.69	0.077	1.00	5,500		5521	0.023	_
	TEB	Triethylbenzene	D	1	0.86	0.02	5.60	0.077	1.00	5,500				
	TEN	Triethylamine	11	3	0.73	2.50	3.49	0.105	1.05	5,500				
	TEG	Triethylene Glycol	D	1	1,12	0.01	5.17	0.076	1.00	5,500		5508		
1.00	TPS	Triethyl Phosphate	D	1	1.07	0.03	6.28	0.077	1.00	5,500	5503			
	TRE	Trimethylbenzene (all isomers)	D	1	0.89	0.14	4.20	0.078	1.00	5,500				
	TRP	Trixylenyl Phosphate	D	1	1.16	0.00	14.20	0.076	1.00	5,500				
-	THE	Tetrahydrofuran	III	1	0.89	8.50	1.35	0.090	1.17	5,500			0.037	0.084
_	UDC	Undecene	D	1	0.75	0.05	5.32	0.077	1.00			100000000000000000000000000000000000000	0.023	
	UND	Undecyl Alcohol	D	1	0.84	0.01	5.94	0.076				5509		0.052
_	VAM	Vinyl Acetate	111	2	0.94	5.80	2.97	0.130	1.12	5,500				
_	XLX	Xylenes (ortho-, meta-, para-)	D	1	0.89	0.51	3.68	0.083	1.01	5,500	5556	5786	0.025	0.058

max = 0.350 1.54 max = 0.249 0.567

1. The above data is sourced from the USCG CHRIS Manual (Ref. 7) & from various manufacturer's MSDS's.

Notes:

Calculation of Maximum Liquid Transfer Rate as Imposed by the Capacity of the Cargo Tank Venting System

Note: Darcy's equation will be used to estimate the pressure drop of the vapor-air mixture through the vent piping from the farthest tank in terms of equivalent pipe length, #1P to the P-V valve. Equivalent length for this path is calculated using Crane's Technical Paper 410 (Ref 4) and Cameron Hydraulic Data handbook (Ref 9).

Calculate equivalent lengths of pipe:

Table 2

a. Pipe run #1

Description:

8" Branch (Exp trunk to vapor stack)

Pipe size, nominal:

8" sch. 40 pipe

Pipe ID (inches):

7.98

Item	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
1	Entrance	8	1	23.3	23.3
2	Straight Pipe	8	1	53.0	53.0
3		8	2	40.0	80.0
4	Tee, flow	8	1	14.0	14.0
5		- =			0.0
6					
	Sum (pipe run #1)				170.3

b. Pipe run #2

Description: 6" branch at P-V valve

Pipe size, nominal: 6" sch. 40 pipe

Pipe ID (inches): 6.07

Item	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
1	Straight Pipe	6	1	3.0	3.0
	Sudden Contraction (8x6)	6	1	8.0	8.0
	Sum (pipe run #2)				11.0

Table 3 Calculation of Maximum Liquid Transfer Rate as Imposed by the Capacity of the Cargo Tank Venting System (Continued)

A. Calculate pressure drop using Darcy's equation:

| Pipe run #1 | 8" Branch (Exp trunk to vapor | Description: stack) | Pipe ID: | Description: 6" branch at P-V valve | Pipe ID: | 6.07 (in) | Pipe ID: | P

							factor:	0.015	5			
CHRIS Code	Name	Vapor-air Mixture Weight Density (from Table 1) (lb/ft^3)	Liquid Transfer Rate (filling) (bbl/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity	Pressure Drop (pipe run #1) (psig)	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ft/s) 46.95	Pressure Drop (pipe run #2) (psig)	Pressure Drop (Total) (psig)	Air Equiv Volumetri Flow Rate (bbl/hr)
	Acrylonitrile	0.095						6600			0.05	3 83
	Acetone Acetophenone	0.085			5566	24.99	0.021	5566	43.19	9 0.006		
	Adiponitrile	0.076	5,500	1.000	5501			5501				
AEC	Amyl acetate (all isomers)	0.075										
AAI	Amyl Alcohol (iso-, n-, sec-, primary)	0.079						5503				23 55
BAL	Acetonitrile Benzyl Alcohol	0.077				24.74	0.018	5511	42.77	7 0.005		
BNZ	Benzene	0.114	5,500	1.250								
BTX	Benzene, Toluene, Xylene mixtures (10% Benze	0.138						6875 5566				
BAR	Butyl Acrylate (iso-, n-)	0.086	5,500									26 58
BAX IAL	Butyl Acetate (all isomers) Butyl Alcohol (iso-)	0.083	5,500				0.020	5599	43.45			
	Butyl Alcohol (n-)	0.074	5,500	1.010								
BAS	Butyl Alcohol (sec-)	0.086						5643 5808				
	Butyl Alcohol (tert-)	0.097	5,500					5501			0.02	23 55
	Butyl Benzyl Phthalate iso-Butyraldehyde	0.131					0.041	6358				
	n-Butyraldehyde	0,131	5,500	1.156				6358				
BUE	Butyl Toluene	0.078										
CLS	Caprolactam Solutions	0.077	5,500									24 56
CCH	Cyclohexanone (Anolone) Cyclohexylamine	0.083	5,500					5568	43.21	0.005	0.02	
CHX	Cyclohexane	0.116			5995			5995				
CHN	Cyclohexanol	0.078										
	1,3-Cyclopentadiene dimer (molten)	0.080						5528 5512				
CMP	p-Cymene Chlorobenzene	0.078						5588	43.36	6 0.006	0.02	27 5
CRS	Cresols	0.077		1.002	5509	24.73	0.018					
CUM	Cumene	0.085	5,500	1.012				5566				
IDA	Decaldehyde (iso-)	0.076						5501 5500				
DAL	Decaldehyde (n-)	0.076	5,500								0.02	24 5
DCE	Decene Decyl Alcohol (all isomers) (Decanol)	0.076				24.70	0.018	5501	42.69	9 0.005	5 0.02	23 5
DBZ	Decylbenzene (n-)	0.076	5,500	1.000		24.70						
DAA	Diacetone Alcohol	0.078	5,500			24.74						
DCH	1,1-Dicholoro ethane	0.188	5,500									
DPA	Dibutyl Phthalate (ortho-)	0.076						5509				
DEB	Diethybenzene Diethylene Glycol	0.076						5501	42,69	9 0.005		
DEN.	Diethylamine	0.083	5,500	1.020	5610			5610				
DBL	Diisobulylene	0.103						5720 5518				
DIK	Diisobutyl Ketone	0.079						5501				
DIP	Diisopropanolamme	0.076	5,500					5503				
DTL	Diisopropylbenzene (all isomers) Dimethyl Phthalate	0.076					0.018	5500				
DOP	Dioclyl Phthalate	0.076	5,500	1,000				5500				
DPN	Dipentene	0.078				24.74		5511 5501				
DIL	Diphenyl	0.076				24.70	0.018	5501				
DDO	Diphenyl, Diphenyl Ether Mixtures Dimethylformamide	0.078						5533	42.94	4 0.005		
DPE	Diphenyl Ether	0.076	5,500	1.000	5501			5501				
DPG	Dipropylene Glycol	0.077	5,500					5508 6193				
DPX	1,1-, 1,2-, 1,3-Dichloropropane	0.162										33 6
DFF	Distillates Flashed Feed Stocks Distillates Straight Run	0.102						5753				
DOZ	Dodecene (all isomers)	0.077	5,500									
DDB	Dodecylbenzene	0.240						6875 5720				
EAC	Ethyl Acrylate	0.100										
EAI EEA	2-Ethylhexyl acrylate 2-Ethoxyethyl acetale	0.077						5503	42.70	0.005	5 0.02	
ETG	Ethoxy Triglycol (crude)	0.076	5,500	1,000								
ETA.	Ethyl Acetate	0.119										
EAA	Ethyl Acetoacetate	0.079									6 0.0	30
EAL	Ethyl Alcohol (Ethanol) Ethyl Benzene	0.083					9 0.020	5566	43.19	9 0.005	5 0.00	
EBT	Ethyl Butanol	0.078						5513			5 0.0	
EBE	Ethyl tert-butyl ether	0.078										
EBR	Ethyl butyrate	0.090										25
ECY	Ethyl Cyclohexane Ethylene dichloride	0.083						5940	46.10	0.009	9 0.0	43
EGL	Ethylene Glycol	0.076	5,500	1.000	5501	24.70	0.018					
EMA	Ethylene Glycol Butyl Ether Acetate	0.077	5,500									
EGY	Ethylene Glycol Diacetale	0.076										
EPE	Ethylene Glycol Phenyl Ether	0.076										23
EEP	Ethyl-3-ethoxypropionate 2-Ethylhexanol (Octanol)	0.076						5502	42.70	0.00	5 0.0	23
EPR	Ethyl Propionate	0.086	5,500	1.070	5885	26.42	2 0.023					
ETE	Ethyl Toluene	0.080	5,500	1.006								
FAM	Formamide	0.076										
FMS	Formaldehyde Solution	0.076								2 0.00	5 0.0	23
FAL	Furfuryl Alcohol Furfural	0.078				24.77	7 0.018	5517	42.8	1 0.00	5 0.0	
GAK	Gasoline Blending Stocks: Alkylates	0.217	5,500	1.250	6875	30.87	7 0.080					
GRF	Gasoline Blending Stocks: Reformates	0.217										
GAT	Gasolines: Automotive	0.217										
GAV	Gasolines: Aviation	0.217										02 1
GCS	Gasolines: Casinghead	0.217							53.3	5 0.02	2 0.1	02
GSR	Gasolines: Polymer Gasolines: StraightRun	0.217	5,500	1,250	6875	30.8	7 0.080	6875				
GCR	Glycerine	0.075	5,500	1.000	5500							
HMX	Heptane (all isomers)	0.105										
HEP	Heptonic Acid	0 076										
HTX	Heptanol (all isomers)	0.07							45.16	6 0.00	8 0.0	137
HPX	Heptene (all isomers) Hexane (all isomers)	0.142			6270	28.15	5 0.043	6270	48.6			
40.00		0.076										
HXO	Hexaonic Acid	0.088		1.020	5610	25.19	9 0.022					

Pipe run #1	Administration	Pipe run #2		
Description:	8" Branch (Exp trunk to vapor stack)	Description:	6" branch at P-V valve	
Pipe ID:	7.98 (in)	Pipe ID:	5.07 (in)	
Equiv. Pipe	744-54	Equiv. Pipe		
Length (table		Length (table		
2a):	170.3 (feet)	2b):	11.0 (feet)	
Darcy friction		Darcy friction		
factor:	0.014	factor:	0.015	

						factor:	0.014		factor:	0.015	1	-	T
	CHRIS Code	Name	Vapor-air Mixture Weight Density (from Table 1) (lb/ft^3)	Liquid Transfer Rate (filling) (bbl/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ft/s)	Pressure Drop (pipe run #1) (psig)	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ft/s)	Pressure Drop (pipe run #2) (psig)	Pressure Drop (Total) (psig)	Air Equiv Volumetr Flow Rat (bbl/hr)
00	IXG	Hexylene Glycol	0.076			5501	24.70		5501	42.69 42.69		0.023	
011		Isophorone	0.076			5501	24.70		5501 5874	42.69			
02		Jet Fuels: JP-4	0,124	5,500		5874	26.37		5511	42.77			
03		Jet Fuels JP-5 (Kerosene, heavy)	0.078			5511	24.74		5517	42.81			
04	KRS	Kerosene	0.079	5,500	1.003	5517 6171	24.77		6171	47.89			
05 1		Methyl Acetate	0.122			6229	27.97		6229	48.34			
06	MAL	Methyl Alcohol (Methanol)	0.082			5536	24.86		5536			0.025	5 5
	MAC	Methylamyl Acetate	0.081	5,500	1.009		24.91		5547	43.05	0.005		5 5
	MAK	Methylamyl Alcohol Methylamyl Keytone	0.076			5506	24.72	0.018	5506	42.72			
	MAM	Methyl Acrylate	0.115			5951	25.72		5951	46.18			
	MBE	Methyl Tert-Butyl Ether (MTBE)	0.077	5,500		5504	24.72		5504				
	ивк	Methyl Butyl Ketone	0.088	5,500		5607	25.17	0.021	5607	43.51			
		Methyl Butyrate	0.091	5,500	1.025	5639	25.32		5639	43.76			
	MEK	Methyl Ethyl Ketone	0.108	5,500		5995	26.92		5995				
	MHK	Methyl Heptyl Ketone	0.077			5507	24.73		5507 5627	42.73			
16	MIK	Methyl Isobutyl Ketone	0.089			5627	25.26		5722	44.4			
	MMM	Methyl methacrylate	0.099			5722			5501	42.69			
	MNA	Methyl Naphthalene	0.076			5501 5522	24.70		5522	42.85			
	MNS	Mineral Spirits	0.079	5,500		5522	25.09		5588				
20		Morpholine	0.084			5519			5519	42.83		0.024	4 !
	MRE	Myrcene	0.079		1.003	5521	24.79		5521	42.84		0.024	
22 F		Naphtha: Petroleum	0.078			5522	24.79		5522	42.85	0.005	0.024	
24 1		Naphtha: Solvent Naphtha: Stoddard Solvent	0.079			5522	24.79	0.019	5522	42.85			
		Naphtha: VM&P	0.079			5521	24.79	0.019	5521	42.84		0.024	
26 1		Nonane (all isomers)	0.080			5530	24.83	0.019	5530	42.91			4
		Nonene (all isomers)	0.082	5,500		5539	24.87		5539	42.98		0.025	
	NNS	Nonyl Alcohol (all isomers)	0.078	5,500		5511	24.74	0.018	5511	42.71			
		Nonyl Phenol	0.076	5,500		5501	24.70		5501	42.69			
	VPM	1-, 2-Nitropropane	0.086			5616		0.021	5616				
31	XAC	Octane (all isomers)	0.087	5,500		5587	25.09		5587 5501	43.36 42.69			
32 0	CX	Octanol (all isomers)	0.076			5501	24.70		5599	43.45			
		Octene (all isomers)	0.088			5599			5562				
		Oil, fuel: No. 2	0,095			5562 5576	24.97 25.04	0,023	5576				
		Oil, fuel: No. 2-D	0.084	5,500		5517	24.77		5517				
		Oil, fuel: No. 4	0.078			5517			5517	42.81			
37 0	OFV	Oil, fuel: No. 5	0.078			5517	24.77	0.018	5517				3
		Oil, fuel: No. 6	0.078			6875	30.87	0.029	6875		0.008	0.036	
39 0		Oil, misc: Crude Oil, Misc: Diesel	0.084			5576	25.04		5576			0.026	6
41 (Oil, Misc: Lubricating	0.076			5517			5517	42.8			
42 0		Oil, Misc: Residual	0.076			5517	24.77		5517				
		Oil, Misc: Turbine	0.082			5533			5533				
44 F		Pentane (all isomers)	0.350		1.540	8470			8470				
	PTE	Pentene (all isomers)	0.310	5,500		8245	37.02		8245	63.98		0.209	
46 F	PIN	Pinene	0.083			5542	24.88		5542	43.0			
47 F	PLB	Polybutene	0.076	5,500		5501	24.70		5501	42.69			
48 F	PGC	Polypropylene Glycol	0,076	5,500		5511	24.74		5511 5698				
19		Propyl Acetate (iso-)	0.097	5,500		5698			5704				
	PAT	Propyl Acetate (n-)	0.098			5704 5830			5830				
1 1		Propyl Alcohol (iso-)	0.091	5,500		5632			5632				
	PAL	Propyl Alcohol (n-)	0.082			5522			5522	42.85	0.005	0.024	4
	PX	Propylbenzene (all isomers) iso-Propylcyclohexane	0.076	5,500		5501	24.70		5501	42.69	0.005	0.023	3
	PPG	Propylene Glycol	0.076	5,500		5501	24.70	0,018	5501	42.65			
	PGN	Propylene Glycol Methyl Ether Acetale	0.083	5,500		5577	25.04		5577	43.2			
		Propylene Tetramer	0.076	5,500	1.000	5502	24.71		5502	42.79			
	SFL	Sulfolane	0.076	5,500		5501	24.70	0.018	5501	42.65			
	STY	Styrene	0.081	5,500		5544	24.89		5544	43.00			
	ITG	Tetraethylene Glycol	0.076	5,500		5501	24.70		5501 5504				
1	THN	Tetrahydronaphthalene	0.077	5,500	1.001	5504	24.72		5665				
	TOL	Toluene	0.091	5,500	1.030	5665			5517				
	TCN	1,2,3-Trichloropropane	0.079	5,500		5517 5501			5501				
	TCP	Tricresyl Phosphate (less than 1% of ortho isome	0.077	5,500		5502			5502				
	TEB	Triethylbenzene	0.077	5,500 5,500	1.000	5775			5775		2 0.007		
	TEN	Triethylamine	0.105	5,500	1.000	5501			5501	42.6	9 0.005	0.02	3
	TEG	Triethylene Glycol	0.076	5,500	1.001	5503			5503				
Ö	TPS	Triethyl Phosphate	0.078	5,500	1.003	5515			5515		0.005		
	TRE	Trimethylbenzene (all isomers)	0.076			5500			5500	42.6	8 0.005		
		Trixylenyl Phosphate	0.090					0.029	6435		4 0.008		
	THF	Tetrahydrofuran Undecene	0.077			5506			5506	42.7	2 0.005		
	UND	Undecyl Alcohol	0.076						5501	42.6	9 0.005		
	VAM	Vinyl Acetate	0.130			6138		0.038	6138				
		Xylenes (ortho-, meta-, para-)	0.083						5556	43.17			
											max =		

High velocity P-V valve pressure setting: Valve setting + pressure drop in piping = Back pressure imposed by P-V valve @ highest flow rate Total back pressure imposed on cargo tank by venting Max design working pressure of tanks;	1.50 (psig) 1.75 (psig) 2.64 (psig) 2.89 (psig) 3.00 (psig)	ок	Conclusion:	At the maximum cargo loading rate, the total back pressure imposed by the tank venting system does not exceed the maximum design working pressure of the tanks.
Check vacuum relieving capacity at maximum discharge rate: Opening vacuum setting for PV Valva: Maximum discharge rate (total):	0.5 (psig) 4300 (bbl/hr)	402 cfm		
Corresponding vacuum at max discharge rate: (see attached PV valve flow capacity curve)	0.49 (psig)			

В.

Table 4

Calculation of the Maximum Liquid Transfer Rate as Imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 46 CFR 39.30-1(d)(3):

Note: Darcy's equation will be used to estimate the pressure drop of the vapor-air mixture through the vent piping from the farthest tank in terms of equivalent pipe length, #1P to the facility connection. Equivalent length for this path is calculated using Crane's Technical Paper 410 (Ref. 4) and Cameron Hydraulic Data handbook (Ref. 9)

Calculate equivalent lengths of pipe:

a. Pipe run #1

Description: 8" Piping
Pipe size, nominal: 8" sch. 40 pipe

Pipe ID (inches): 7.98

ltem	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
1	Entrance	8	1	23.3	23.3
	Straight Pipe	8	1	190.0	190.0
3		8	2	40.0	80.0
4		8	7	14.0	98.0
5	Elbow, 90 deg.	8	0	14.0	0.0
	Elbow, 45 deg.	8	4	11.0	44.0
	Valve, Gate	8	1	8.6	8.6
	Hose	8	1	50.0	50.0
	Sum (pipe run #1)				493.9

Calculation of the Maximum Liquid Transfer Rate as Imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 46 CFR 39.30-1(d)(3) (continued):

Calculate pressure drop using Darcy's equation:

Pipe run #1
Description:
Pipe ID:

8" Piping

7.98 (in)

Equivalent Length of Pipe (from Table 4a):

493.9 (feet)

					Darcy friction factor:	0.014		7		
CHRIS Code	Name	Vapor-air Mixture Weight Density (from Table 1) (lb/ft^3)	Liquid Transfer Rate (filling) (bbl/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity	Pressure Drop (pipe run #1) (psig)	Pressure Drop (Total) (psig)	Air Equivaler Volumetric F Rate (bbl/hr)	
1 ACN	Acrylonitrile	0.095	5,500		6050	27.16	0.079	0.079		
2 ACT	Acetone	0.123	5,500		5566 5566	29.63 24.99		0.060		
	Acetophenone Adiponitrile	0.085 0.076				24.70	0.052	0.052		
	Amyl acetate (all isomers)	0.075		1.007	5536	24.86		0.052	1	
6 AAJ	Amyl Alcohol (iso-, n-, sec-, primary)	0.079	5,500		5533 5503	24.84		0.052	1	
	Acetonitrile	0.076	5,500 5,500			24.74		0.053		
O BNZ	Benzyl Alcohol Benzene	0.114	5,500	1.250	6875	30.87		0.122		
0 BTX	Benzene, Toluene, Xylene mixtures (10% Benzene	0,138		1.250		30.87 24.99		0.147	+	
BAR	Butyl Acrylate (iso-, n-)	0.086 0.085	5,500 5,500			24.99		0.059		
	Butyl Acetate (all isomers) Butyl Alcohol (iso-)	0.083	5,500		5599	25,14	0.059	0.059		
	Butyl Alcohol (n-)	0.074	5,500	1.010		24.94		0.052	+	
5 BAS	Butyl Alcohol (sec-)	0.086	5,500 5,500			25.34 26.08		0.074		
	Butyl Alcohol (tert-)	0.097	5,500			24.70	0.052	0.052	1	
	Butyl Benzyl Phthalate iso-Butyraldehyde	0.131	5,500	1.156	6358	28.55		0.120		
	n-Butyraldehyde	0.131	5,500			28.55		0.120	-	
	Butyl Toluene	0.078	5,500 5,500					0.053		
	Caprolactam Solutions Cyclohexanone (Anolone)	0.078			5522	24.79	0.054	0.054		
	Cyclohexylamine	0.083	5,500	1.012				0.058		
4 CHX	Cyclohexane	0.116						0.054		
	Cyclohexanol	0.078	5,500 5,500			24.82	0.055	0.055		
	1,3-Cyclopentadiene dimer (molten) p-Cymene	0.078	5,500	1.002	5512	24.75	0.054	0.054		
	Chlorobenzene	0.087	5,500	1.016				0.061	1	
9 CRS	Cresols	0.077	5,500 5,500	1.002				0.052		
	Dimethyl Phthalate	0.076 0.076			5500	24.70	0.052	0.052		
	Diocityl Phthalate Dipentene	0.078	5,500	1.002	5511	24.74		0.054	-	
9 DIL	Diphenyl	0.076	5,500			24.70		0.052 0.052	-	
0 DDO	Diphenyl, Diphenyl Ether Mixtures	0.076						0.054		
	Dimethylformamide Diphenyl Ether	0.076				24.70	0.052	0.052		
	Dipropylene Glycol	0.077	5,500	1.001				0.053 0.140		
4 DPX	1,1-, 1,2-, 1,3-Dichloropropane	0,162						0.076	1	
DFF	Distillates Flashed Feed Stocks	0.102						0.076	1	
DSR	Distillates Straight Run Dodecene (all isomers)	0.077					0.052	0.052		
7 DOZ . 8 DDB	Dodecylbenzene	0.240		1.250				0.256 0.074		
9 EAC	Ethyl Acrylate	0.100						0.074		
0 EAI	2-Ethylhexyl acrylate	0.077						0.052		
1 EEA 2 ETG	2-Ethoxyethyl acetate Ethoxy Triglycol (crude)	0.076			5500	24.70	0.052	0.052		
3 ETA	Ethyl Acetale	0.119	5,500	1.09				0.097 0.055		
4 EAA	Ethyl Acetoacetate	0.079						0.067		
5 EAL	Ethyl Alcohol (Ethanol)	0,086					0.058	0.058	1	
6 ETB 7 EBT	Ethyl Benzene Ethyl Butanol	0.078	5,500	1.00				0.053 0.054		
8 EBE	Ethyl tert-butyl ether	0.078						0.064		
9 EBR	Ethyl butyrate	0.090						0.058		
0 ECY 1 EDC	Ethyl Cyclohexane Ethylene dichloride	0.122			5940			0.097		
2 EGL	Ethylene Glycol	0.076	5,500					0.052 0.053	1	
3 EMA	Ethylene Glycol Butyl Ether Acetate	0.077						0.052		
4 EGY 5 EPE	Ethylene Glycol Diacetate Ethylene Glycol Phenyl Ether	0.076				24.7	0.052	0.052		
6 EEP	Ethyl-3-ethoxypropionate	0.076	5,500	1.00		24.7		0.052		
7 EHX	2-Ethylhexanol (Octanol)	0.076	5,500					0.052		
8 EPR	Ethyl Propionate	0.086					0.056	0.056		
9 ETE	Ethyl Toluene Formamide	0.076	5,500	1.00	2 5511	24.7	4 0.052	0.052		
1 FMS	Formaldehyde Solution	0.078	5,500	1.00				0.052	-	
2 FAL	Furfuryl Alcohol	0.07						0.053		
3 FFA	Furfural Gasoline Blending Stocks: Alkylates	0.07		1.25	6875	30.8	7 0.232	0.232		
4 GAK 5 GRF	Gasoline Blending Stocks: Reformates	0.21	5,500	1.25	6875			0.232 0.232		
6 GAT	Gasolines: Automotive	0.21						0.232		
7 GAV	Gasolines: Aviation	0.21					7 0.232	0.232		
8 GCS 9 GPL	Gasolines: Casinghead Gasolines: Polymer	0.21	7 5,500	1.25	6875	30.8		0.232		
0 GSR	Gasolines: StraightRun	0.21	5,500	1.25				0.232 0.052		
II GCR	Glycerine	0.07						0.079		
2 HMX 3 HEP	Heptonic Acid	0.07	5,500	1.00	0 550	24.7	0.052	0.052		
HTX	Heptanol (all isomers)	0.07	7 5,500	1.00				0.053		
95 HPX	Heptene (all isomers)	0.10						0.126		
6 HXS	Hexane (all isomers)	0.14					0.052	0.052		
7 HXO 8 HXN	Hexanol Hexanol	0.08		1.02	0 561	25.1	9 0.063	0.063		
99 HEX	Hexene (all isomers)	0.14	5,50	1.16	0 638			0.136 0.052	-	
00 HXG	Hexylene Glycol	0.07						0.052		
1 IPH	Isophorone	0.07					7 0.097	0.097		
12 JPF 13 JPV	Jet Fuels: JP-4 Jet Fuels JP-5 (Kerosene, heavy)	0.12		1.00	2 551	24.7	4 0.053	0.053		
04 KRS	Kerosene	0.07	9 5,50	1.00				0.054		
D5 MTT	Methyl Acetate	0.12						0.105		
06 MAL	Methyl Alcohol (Methanol)	0.07					6 0.057	0.057		
07 MAC 08 MAA	Methylamyl Acetate Methylamyl Alcohol	0.08		1.00	9 554	7 24.9	1 0.057	0.057		
09 MAK	Methylamyl Keytone	0.07	5,50	1.00	1 550			0.052		
10 MAM	Methyl Acrylate	0.11	5,50	1.08	2 595	1 26.7	2 0.092	0.092		

Pipe run #1	
Description:	8" Piping
Pipe ID:	7.98 (in)
Equivalent Length of	
Pipe (from Table 4a):	493.9 (feet)

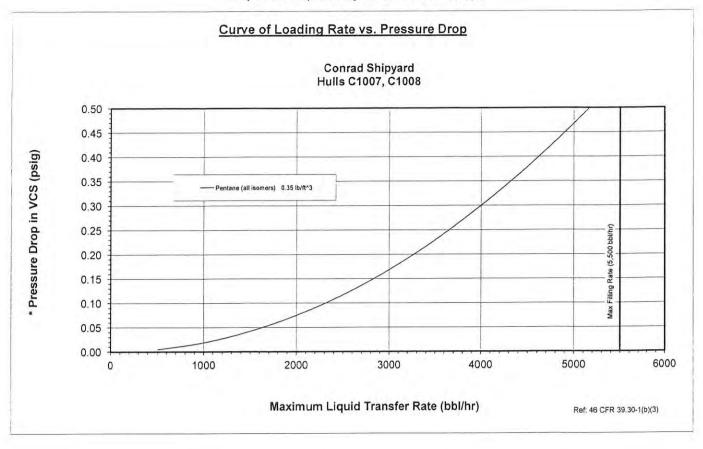
					arcy friction factor:	0.014	0.052	0.052	55
11 MBE	Methyl Tert-Butyl Ether (MTBE)	0.077	5,500	1.001	5504 5607	24.72 25.17	0.062	0.062	50
12 MBK	Methyl Butyl Ketone	0.088	5,500	1.019	5639	25.32	0.065	0.065	61
	Methyl Butyrate	0.091	5,500	1.025	5995	26.92	0.088	0.088	7
	Methyl Ethyl Ketone	0.108	5,500	1.001	5507	24.73	0.053	0.053	5
	Methyl Heptyl Ketone	0.077	5,500		5627	25.26	0.064	0.064	6
16 MIK	Methyl Isobutyl Ketone	0.089	5,500	1.023	5722	25.69	0.074	0.074	
	Methyl methacrylate	0.099	5,500			24.70	0.052	0.052	- 5
18 MNA	Methyl Naphthalene	0.076	5,500	1.000	5501	24.79	0.055	0.055	-
19 MNS	Mineral Spirits	0.079	5,500	1.004	5522 5588	25.09	0.059	0.059	5
20 MPL	Morpholine	0.084	5,500	1.016	5519	24.78	0.054	0.054	- 6
21 MRE	Myrcene	0.079	5,500	1.003		24.79	0.054	0.054	
22 PTN	Naphtha: Petroleum	0.078	5,500	1.004	5521 5522	24.79	0.054	0.054	
23 NSV	Naphtha: Solvent	0.078	5,500	1.004		24.79	0.055	0.055	
24 NSS	Naphtha: Stoddard Solvent	0.079	5,500	1.004	5522 5521	24.79	0.054	0.054	
	Naphtha: VM&P	0.079	5,500	1.004			0.056	0.056	
26 NAX	Nonane (all isomers)	0.080	5,500	1.005	5530	24.83	0.057	0.057	
27 NON	Nonene (all isomers)	0.082	5,500	1.007	5539	24.87		0.054	
28 NNS	Nonyl Alcohol (all isomers)	0.078	5,500	1.002	5511	24.74	0.054		
29 NNP	Nonyl Phenol	0.076	5,500	1.000	5501	24.70	0.052	0.052	
30 NPM	1-, 2-Nitropropane	0.086	5,500	1.021	5616	25.21	0.062	0.062	
31 OAX	Octane (all isomers)	0.087	5,500	1.016	5587	25.09	0.061	0.061	
32 OCX	Octanol (all isomers)	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Octene (all isomers)	0.088	5,500	1.018	5599	25.14	0.063	0.063	
	Oil, fuel: No. 2	0.095	5,500	1.011	5562	24.97	0.066	0.066	
35 OTD	Oil, fuel: No. 2-D	0.084	5,500	1.014	5576	25.04	0.059	0.059	
36 OFR	Oil, fuel: No. 4	0.078	5,500	1.003	5517	24.77	0.054	0.054	
	Oil, fuel: No. 5	0.078	5,500	1.003	5517	24.77	0.054	0.054	
	Oil, fuel: No. 6	0.078	5,500	1.003	5517	24.77	0.054	0.054	
	Oil, misc: Crude	0.078	5,500	1.250	6875	30.87	0.083	0.083	
	Oil, Misc: Diesel	0.084	5,500	1.014	5576	25.04	0.059	0.059	
	Oil, Misc: Lubricating	0.076	5,500	1.003	5517	24.77	0.052	0.052	
	Oil, Misc: Residual	0.076	5,500	1.003	5517	24.77	0.052	0.052	
	Oil. Misc: Turbine	0.082	5,500	1.006	5533	24.84	0.057	0.057	
	Pentane (all isomers)	0.350	5,500	1.540	8470	38.03	0.567	0.567	1
	Pentene (all isomers)	0.310	5,500	1.499	8245	37.02	0.477	0.477	1
46 PIN	Pinene	0.083	5,500	1.008	5542	24.88	0.057	0.057	
47 PLB	Polybutene	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Polypropylene Glycol	0.076	5,500	1.002	5511	24.74	0.052	0.052	
	Propyl Acetate (iso-)	0.097	5,500	1.036	5698	25.58	0.072	0.072	
	Propyl Acetate (n-)	0.098	5,500	1.037	5704	25.61	0.072	0.072	
	Propyl Alcohol (iso-)	0.091	5,500	1.060	5830	26.18	0.070	0.070	
	Propyl Alcohol (n-)	0.082	5,500	1.024	5632	25.29	0.059	0.059	
	Propylbenzene (all isomers)	0.079	5,500	1.004	5522	24.79	0.055	0.055	
	iso-Propylogical (all isomers)	0.076	5,500	1.000	5501	24.70	0.052	0.052	
		0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Propylene Glycol	0.083	5,500	1.014	5577	25.04	0.058	0.058	
	Propylene Glycol Methyl Ether Acetate	0.076	5,500	1.000	5502	24.71	0.052	0.052	
	Propylene Tetramer	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Sulfolane	0.076	5,500	1.008	5544	24.89	0.056	0.056	
	Styrene		5,500	1.000	5501	24.70	0.052	0.052	
	Tetraethylene Glycol	0.076	5,500	1.001	5504	24.72	0.053	0.053	
	Tetrahydronaphthalene			1.030	5665	25,44	0.066	0.066	
62 TOL	Toluene	0.091	5,500	1.003	5517	24.77	0.055	0.055	
63 TCN	1,2,3-Trichloropropane	0.079	5,500		5501	24.70	0.052	0.052	
64 TCP	Tricresyl Phosphate (less than 1% of ortho isomer)	0.077	5,500	1,000		24.71	0.052	0.052	
	Triethylbenzene	0.077	5,500	1.000	5502 5775	25,93	0.032	0.079	
	Triethylamine	0.105	5,500	1.050		24.70	0.052	0.052	
	Triethylene Glycol	0.076	5,500	1.000	5501	24.70	0.052	0.053	
	Triethyl Phosphate	0.077	5,500	1.001	5503			0.054	
	Trimethylbenzene (all isomers)	0.078	5,500	1.003	5515	24.76	0.054		
70 TRP	Trixylenyl Phosphate	0.076	5,500	1.000	5500	24.70	0.052	0.052	
71 THF	Tetrahydrofuran	0.090	5,500	1.170	6435	28.89	0.084	0.084	
	Undecene	0.077	5,500	1.001	5506	24.72	0.053	0.053	
	Undecyl Alcohol	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Vinyl Acetate	0.130	5,500	1.116	6138	27.56	0.111	0.111	
	Xylenes (ortho-, meta-, para-)	0.083	5,500	1.010	5556	24.95	0.058	0.058	

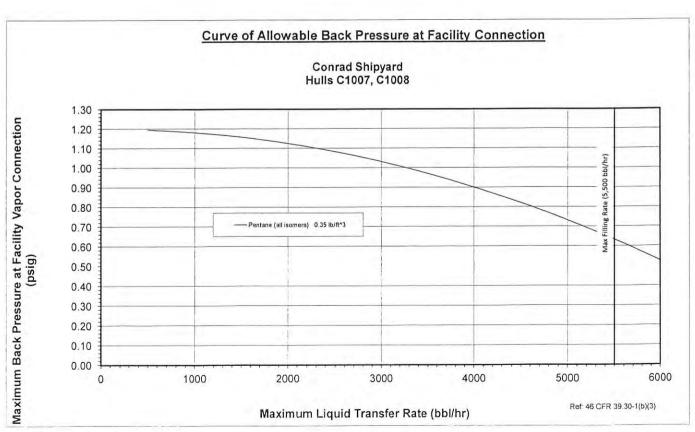
Compare pressure drop to P-V valve pressure settings:
 High-velocity P-V Valve pressure setting:
 Cargo tank P-V Valve pressure setting:
 30% of lowest P-V Valve Pressure Setting:
 Highest Pressure Drop from Tank to Facility Connection:
 Max Allowable Back Pressure at Facility Connection:

1.50 (psig) 1.50 (psig) 1.20 (psig) 0.57 (psig) 0.63 (psig)

Pentane (all isomers)

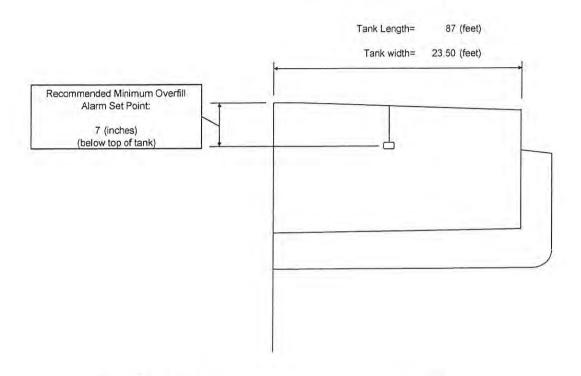
Conclusion:
For the cargo with the highest pressure drop (Pentane), the pressure drop is 0.57 psig. This, when added to the back pressure at the facility vapor connection must not exceed 80% of the pressure setting of any P-V valve in the cargo tank venting system. Therefore, the maximum allowable back pressure at the shore facility must not exceed 0.63 psig when loading with Pentane at the maximum liquid transfer rate (5,500 bbl/hr).





CONRAD SHIPYARD C1007, C1008

Calculation of Overfill Alarm Set Point (Cargo Tank No. 1 P/S)

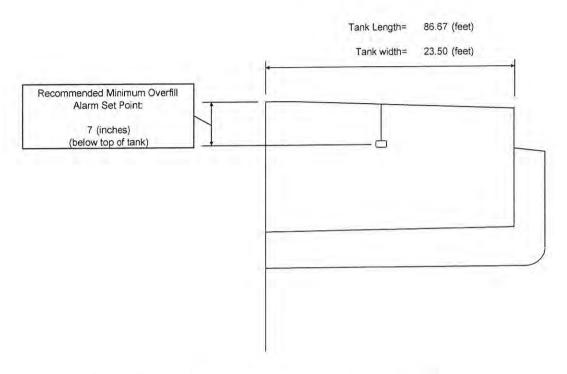


Maximum (per tank) Cargo	=	5,500 (bbl/hr)	
Loading Rate	=	91.67 (bbl/min)	
Minimum allowable time from			
alarm to overflow		60 (sec)	
Required volume above overfill			
alarm set point	=	91.7 (bbl)	
Capacity to deck at CL (17'-8" ABL) =		5315 BBL	
Capacity to 7" below dk at CL (17'-1" ABL) =		5203 BBL	
Volume above alarm =	1	112.2 BBL	RESULT OK
**Recommended set point of	=	7 (inches)	[Appx. 98% full tank]

**Note: Or 98.5%, whichever is lower (to d	comply with 33CFR155.775)
Capacity at 98.5% =	5235 BBL
Dist from TT at CL =	0.49 ft.

CONRAD SHIPYARD C1007, C1008

Calculation of Overfill Alarm Set Point (Cargo Tank No. 2 P/S)

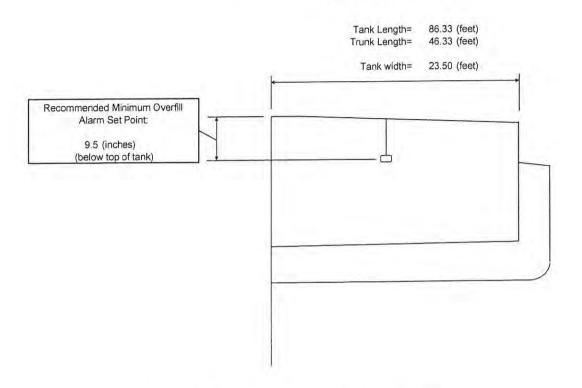


Maximum (per tank) Cargo	=	5,500 (bbl/hr)	
Loading Rate	=	91.67 (bbl/min)	
Minimum allowable time from			
alarm to overflow	=	60 (sec)	
Required volume above overfill			
alarm set point	=	91.7 (bbl)	
Capacity to deck at CL (17'-8" ABL) =		5295 BBL	
Capacity to 7" below dk at CL (17'-1" ABL) =		5183 BBL	
Volume above alarm =		111.8 BBL	RESULT OK
**Recommended set point of	=	7 (inches)	[Appx. 98% full tank]
	Loading Rate Minimum allowable time from alarm to overflow Required volume above overfill alarm set point Capacity to deck at CL (17'-8" ABL) = Capacity to 7" below dk at CL (17'-1" ABL) = Volume above alarm =	Loading Rate = Minimum allowable time from alarm to overflow = Required volume above overfill alarm set point = Capacity to deck at CL (17'-8" ABL) = Capacity to 7" below dk at CL (17'-1" ABL) = Volume above alarm =	Loading Rate = 91.67 (bbl/min) Minimum allowable time from alarm to overflow = 60 (sec) Required volume above overfill alarm set point = 91.7 (bbl) Capacity to deck at CL (17'-8" ABL) = 5295 BBL Capacity to 7" below dk at CL (17'-1" ABL) = 5183 BBL Volume above alarm = 111.8 BBL

**Note: Or 98.5%, whichever is lower (to c	comply with 33CFR155.775)
Capacity at 98.5% =	5215 BBL
Dist from TT at CL =	0.49 ft.

CONRAD SHIPYARD C1007, C1008

Calculation of Overfill Alarm Set Point (Cargo Tank No. 3 P/S)



Maximum (per tank) Cargo	=	5,500 (bbl/hr)	
Loading Rate	=	91.67 (bbl/min)	
Minimum allowable time from			
alarm to overflow	=	60 (sec)	
Required volume above overfill			
alarm set point	=	91.7 (bbl)	
Capacity to deck at CL (17'-8" ABL) =		4427 BBL	
Capacity to 9.5" below dk at CL (16'-10.5" ABL) =		4328 BBL	
Volume above alarm =		99.5 BBL	RESULT OK
**Recommended set point of	=	9.5 (inches)	[Appx. 98% full tank]

**Note: Or 98.5%, whichever is lower (to comply with 33CFR155.775)

Capacity at 98.5% = 4361 BBL

Dist from TT at CL = 0.62 ft.

Vapor Recovery Calculations

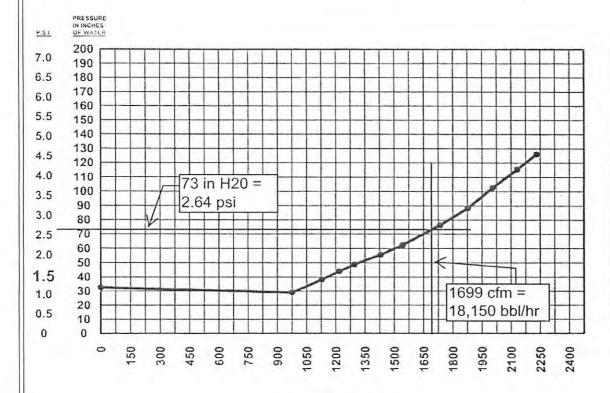
REFERENCES

- 1. 46 CFR 32.55-25, Venting of cargo tanks of tank barges constructed on or after July 1, 1951 -
- 2. 46 CFR 39.20-11, Vapor overpressure and vacuum protection TB/ALL
- 3. 46 CFR 39.30-1, Operational Requirements TB/ALL
- 4. Flow of Fluids Through Valves, Fittings, and Pipe; Crane Technical Paper No. 410
- USCG Guidelines for Determining the Maximum Liquid Transfer Rate for a Tank Vessel Transferring a Flammable or Combustible Cargo Using a Vapor Control System
- 6. Conrad Dwg. P3 Vapor Control Piping
- 7. USCG CHRIS (Chemical Hazards Response Information System) Manual.
- 8. 46 CFR 39.20-9, Tank Barge Liquid Overfill Protection B/ALL
- 9. Cameron Hydraulic Data, 15th edition

LIST OF ATTACHMENTS

- 1. Flow Capacity Curves for High-Velocity P-V Valve
- 2. Vacuum flow diagram for High-Velocity P-V Valve
- 3. USCG Approval Certificate for High-Velocity P-V Valve

CONRAD C1007, C1008

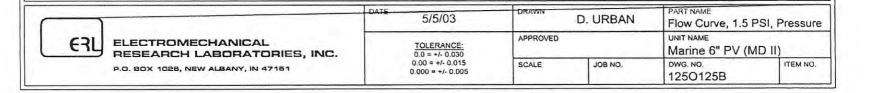


BARRELS	FLOW	PRESSURE
PER	FT.'/	IN. OF
HOUR	MIN.	Hz0

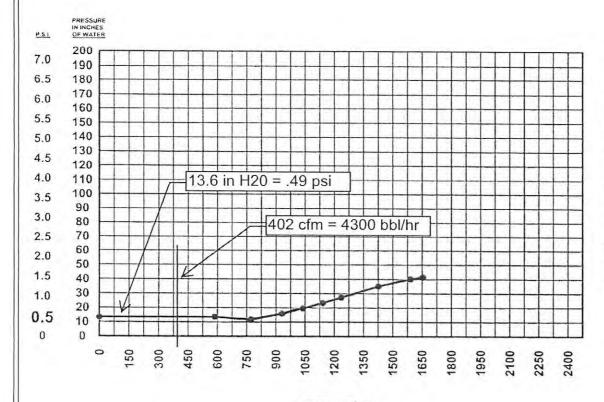
10418	974	29.2
12054	1127	38.6
13017	1217	44.2
13862	1296	49.0
15295	1430	55.8
16493	1542	62.6
18547	1734	76.6
20066	1876	88.5
21435	2004	102,8
22783	2130	115.8
23852	2230	126.3

Curve for Pressure Side 6" PV Valve - 1.5 PSI data based on air flow

FLOW IN FT.3/MIN.



CONRAD C1007, C1008

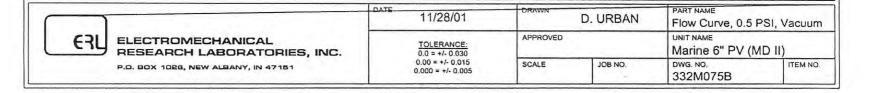


BARRELS	FLOW	PRESSURE
PER	FT.'/	IN. OF
HOUR	MIN.	H ₂ 0

6260	585	13.6
8256	772	11.8
9958	931	16.0
11100	1038	19.9
12197	1141	23.7
13207	1235	27.5
15252	1426	35.5
17003	1590	40.4
17674	1653	41.7

Curve for Vacuum Side
6" PV Valve - 0.5 PSI
data based on air flow

FLOW IN FT.3/MIN.





U. S. Department of Homeland Security United States Coast Guard Certificate of Approval

Coast Guard Approval Number: 162.017/167/4

Expires: 05 April 2016

PRESSURE-VACUUM RELIEF VALVES FOR TANK VESSELS

ELECTROMECHANICAL RESEARCH LABORATORIES INC. 2560 Charlestown Road NEW ALBANY IN 471510

ERL SUPERAC Model II, 6-inch High Velocity Pressure/Vacuum Relief Valve.

High-velocity weight-loaded pressure/vacuum relief valve, constructed of 300 series stainless steel.

Identifying Data: ERL Drawing No. 050M147B dated June 6, 2001. Flow data located in CEESI Test Reports dated December 12, 2001 (initial testing), November 8, 2004 (5.5 psi pressure setting), December 13, 2005 (10.0 psi pressure setting), and January 30, 2006 (3.0 psi vacuum setting), February 14, 2011 (5.0 psi vacuum setting).

Approved for relief settings of: 1.0 - 10.0 psig pressure, and 0.5 - 5.0 psig vacuum.

ERL SUPERAC (TM) Model II 6" P/V Valve has been tested in accordance with API 2000, and is approved for use in vapor control systems.

This certificate supersedes approval no. 162.017/0167/3 dated May 12, 2006, to expand range of vacuum settings up to 5.0 psi.

*** END ***

THIS IS TO CERTIFY THAT the above named manufacturer has submitted to the undersigned satisfactory evidence that the item specified herein complies with the applicable laws and regulations as outlined on the reverse side of this Certificate, and approval is hereby given. This approval shall be in effect until the expiration date hereon unless sooner canceled or suspended by proper authority.



GIVEN UNDER MY HAND THIS 5th DAY OF APRIL 2011, AT WASHINGTON D.C.

C. R. O'NEIL

Assistant Chief, Tank Vessel and Offshore Division

U.S. Coast Guard Marine Safety Center



Marine Safety Center Vapor Control System (VCS) Plan Review Information Sheet (PRIS)



Vessel Name	CBC 377 - 379, 381 - 383, 385	Shipyard	Conrad Industries
Official Number	O.N. 1243653 - 1243659	Hull Number	C-1011 through C-1017
Control Systems. CG Ins	s critical VCS parameters for MSC pectors should verify the vessel's vapor control endorsement on the variet the vessel's design the CG Ir	√CS design is consistent with ∕essel's Certificate of Inspect	n the information listed in boxes 2, 6, 7 tion. For cases where the information in
2. Tank Maximum Desi		3.00 psig	Raised Trunk X Flush Deck
3. Authorized Maximum Cargo Transfer Rate(s)		5,500 bbl/hr loadi	ing (max 2 tanks simultaneously) harging
4. Authorized Maximum Vapor-Air Mixture Density		0.347 lbm/ft ³	
5. Authorized VCS Categories 1 through 7			
a. Ca		PENTANE PENTANE	
CG Approval Required Venting Required Venting Required Venting Required Venting Required Protect	ng Capacity of Pressure-Side of ng Capacity of Vacuum-Side of tion System (check appropriate be	P/V valve 14673 P/V valve 5500 ox or boxes)	ngitudinal Header (inches) 8 ansverse Header (Inches) 8 bbl/hr (air) bbl/hr (air)
a. High Level/Tank Ovb. Overfill Control Shuc. Spill Valved. Rupture Disk	rerfill Alarm 🔲 Type	Beran Gaurd 07324TWIN-2A OCMI to Verify N/A	Setting in psi Meets ASTM F1271 N/A
10. Closed Gauging	Verify the vessel has closed gau	uging that satisfies 46 CFR 3	9.20-3 and 151.15-10(c).
In accordance with 46 plans approved by Mar No. C1-1300533 dated annotated with "Yes" in When the vessel is car ensuring the provision: 11b. The MSC approvision of the closed.	ne Marine Safety Center's recomm CFR Part 39, excluding part 39.40 rine Safety Center letter Serial No. I February 19, 2013, and has been the the vessel's Cargo Authority rrying cargoes containing greater to sof 46 US Code of Federal Regulated at the value at the value.	, this vessel's vapor collectic C1-1205080 dated December found acceptable for the contract that the contract of the contract	re applied. designed in a way it is "clearly" open or
11d. Previous applica	ble approval letters:	SC Letter C1-1205080 dtd D	December 19, 2012
VCS Approval Letter	MSC Letter C1-1300533 dtd Fe	ebruary 19, 2013 MSC F	Plan Reviewer LT Joseph P. Burge