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GUARINO & COX, LLC

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CONRAD SHIPYARD

297'-6" x 54' x 12' INLAND TANK BARGE

VAPOR CONTROL SYSTEM CALCULATIONS

SCALE:	NONE	DATE:	11/19/2012	DWG. NO.
DRAWN BY:	R. ALLUMS	CK'D BY:	R. ALLUMS	C-32
HULL NO.	C1007, C1008	JOB NO.	12-085	REV. 0

VAPOR CONTROL SYSTEM CALCULATIONS - SUMMARY

A. General Description of Vessel:

1.

Builder: CONRAD SHIPYARD Builder's hull numbers: C1007, C1008

Year Built: 2013

 Official Numbers:
 1243651, 1243652

 Owner:
 Canal Barge

 Vessel Names:
 CBC 374, CBC 375

 Vessel Dimensions:
 297'-6" x 54'-0" x 12'-0"

 Service:
 Inland Tank Barge (D/O)

Classification: None

 Max Design Working Pressure of Tanks:
 3.00
 (psig)

 Max Cargo Loading Rate
 5,500
 (bbl/hr)

 Maximum Discharge Rate
 4,300
 (bbl/hr)

VCS Cargoes: See Table 1

Maximum Vapor-Air Mixture Density: 0.35 (Pentane, all isomers) (lbm/ft^3)

Maximum Vapor Growth Rate: 1.54 (Pentane, all isomers) (lbm/ft^3)

B. General Description of Vapor Control System:

[Note: Also see Reference 6 for details of vapor control system.]

1. Pipe:

One (1) 8" diam longitudinal vapor header fitted with a 6" high-velocity PV Valve.

One (1) 8" diam tranverse vapor header with 8" shore connection valves.

One (1) 8" diam branch line off longitudinal header to each cargo tank.

(See Reference 6 for system layout)

2. High Velocity PV Valve:

 Model:
 ERL 6" SUPERAC PV-6

 Pressure Setting:
 1.50
 (psig)

 Vacuum Setting:
 0.5
 (psig)

 PV Valve Flow Capacity:
 See Att. 1
 (bbl/hr)

3. Spill Valve:

Model: None installed

Pressure Setting: N/A

4. Vapor Recovery Hose:

Diameter: 8" (assumed)
Length: 50' (assumed)

5. Cargo Tank P-V Valves: (One central P/V valve only, no individual tank P-V

valves)

Model: See #2 above.

Pressure Setting: 1.50 (psig)
Vacuum Setting: 0.5 (psig)

C. VCS Calculations:

1. Cargo Authority:

The vapor collection system installed on this barge is designed for Grade A and lower petroleum products and Type II/III chemicals. Typical cargoes to be carried by this barge are listed in Table 1. These cargoes are to be listed in the Cargo Authority Attachment (CAA) of the barge's Certificate of Inspection. Note that Table 1 is not intended to be an all-inclusive list and the CAA should therefore not be limited to these cargoes. Other cargoes with less restrictive or equal characteristics shall also be included on the CAA. VCS Categories 1 through 7 are requested.

2. Determining Vapor-Air Mixture Density and Vapor Growth Rate:

Of the cargoes carried, Pentane has the highest vapor-air mixture density. Pentane also has the greatest vapor growth rate. (See Table 1)

3. The Maximum Liquid Transfer Rate as Imposed by the Capacity of the Cargo Tank Venting System: (Ref: 46 CFR 39.20-11)

Tanks #1 P/S are the farthest tanks from the High-Velocity P-V Valve in terms of total equivalent pipe length. Using factors from Reference 4 and 9, the total equivalent length of pipe is calculated for this path. This calculation is shown in Table 2.

Using Darcy's equation, and friction factors selected as appropriate for the pipe size, and the maximum liquid transfer rate, the pressure drop along the VCS piping from tank #1P to the P-V Valve is calculated using the total equivalent length of pipe from Table 2. The pressure drop calculations were done for the maximum loading rate (5,500 BBL/hr) for this barge. This maximum loading rate is based on loading one tank at a time. This calculation is shown in Table 3.

Conclusions:

Using a 5,500 bbl/hr maximum liquid transfer rate (for Pentane and lower cargos), the vapor-air mixture and air-equivalent volumetric flow rates for each cargo are shown in Table 3. The greatest pressure drop in the cargo tank venting system is 0.25 psig for Pentane cargo. At a pressure relief setting of 1.5 psig, the high-velocity P-V valve has an adequate flow capacity (see attachment 1). The greatest total back pressure imposed on the tanks by the cargo tank venting system (2.89 psig) does not exceed the design working pressure of the cargo tanks (3.00 psig). Also, the vacuum relieving capacity of the P-V Valve has been checked against the maximum discharge rate and has been found to have adequate vacuum relieving capacity (see Table 3).

4. The Maximum Liquid Transfer Rate as Imposed by the Relieving Capacity of the Cargo Tank Spill Valves:

No spill valves are installed on this barge.

5. The Maximum Liquid Transfer Rate as Imposed by the Set Point of the Overfill Alarm:

At the maximum cargo loading rate of 5,500 bbl/hr, required overfill alarm set points have been calculated such that the person in charge of the transfer operations has more than 60 seconds from the overfill alarm to stop the transfer operations before the tank overflows. (See attached overfill alarm set point calculation sheets.) The overfill alarms will need to be set at or below these calculated levels to ensure that the VCS complies with 46 CFR 39.20-9. In addition, the overfill alarms must also be set at or below a capacity of 98.5% to comply with 33CFR155.775.

6. The Maximum Liquid Transfer Rate as imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 46 CFR 39.30-1(d)(3):

This requires the sum of the pressure drop along the longest path from the cargo tank to the vessel vapor connection and the back pressure at the facility vapor connection not to exceed 80 percent of the pressure setting of any pressure relief valve in the system. Tanks #1 P/S are the farthest from the facility vapor connection (in terms of total equivalent length of pipe). The total equivalent length from cargo tank #1P to the facility vapor connection is given in Table 4.

Using Darcy's equation, and friction factors selected as appropriate for the pipe size, and the maximum liquid transfer rate, the pressure drop along the VCS piping from tank #1P to the facility vapor connection is calculated using the total equivalent length of pipe from Table 4. These calculations are shown in Table 5.

Conclusions:

Pressure drop at the maximum liquid transfer rate of 5,500 bbl/hr (for Pentane and lower cargoes) along this path for each cargo is given in Table 5. The highest pressure drop (for Pentane) does not exceed 80 percent of the P-V valve pressure setting. If the pressure drop between the facility vapor connection and the shore facility's pressure sensor is known, it should be added to the pressure drop along this path to ensure that the total pressure drop does not exceed 80 percent of the P-V valve pressure setting.

7. Graph as Required by 46 CFR 39.30-1(b)(3): See attached.

Determination of Vapor-Air Mixture Density & Vapor Growth Rate

Table 1

CHRIS Code	Name	Туре	VCS Category	Liquid S.G.	*Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (lb/ft^3)	Vapor Growth Rate	Max. Loading Rate	Vapor Volumetric Flow Rate (bbl/hr)	Air Equivalent Volumetric Flow Rate (bbl/hr)	in VCS (See Table 3) (psig)	Pressure Drop to Facility Connection in VCS (See Table 5) (psig)
1 ACN	Acrylonitrile	111	4	0.81	5.00	1.80							
	Acetone	D	1	0.79	10.00	2.00		1.20					
	Acetophenone	D	1	1.03	0.60	4.14	0.085		5,500				
	tell and the	11	1	0.95		3.73							
	and a section (and the section)	D	1	0.88	0.33	0.10		1.01	5,500 5,500				
	7.00	D	1	0.82	0.30	3.04 1.41	0.079	-					
		111	3	0.78 1.05		3.73		1.00					
	Dolla, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1,	D III	1	0.88	4.50	2.80		1.25					
	Benzene Benzene, Toluene, Xylene mixtures (10%	na .		0.00	7.50	2.00	0.714	1.20	0,000				
		111	1	0.84	7.30	2.80	0.138	1.25	5,500	6875	9252	0.065	0.14
		111	2	0.90		4.42	0.086	1.01	5,500	5566	5908		
		D	1	0.87	0.60	4.00	0.085	1.01	5,500				
		D	1. 1.1	0.81	0.90	2,60		1.02	5,500				
		D		0.81	0.50	0.10		1.01	5,500				
	Butyl Alcohol (sec-)	D	1	0.81	1.30	2.60		1.03					
16 BAT	Daty () Moderna () Land	D	1	0.78		2.60		1.06					
	Daty Consty Constant	D	1	1.12		10.80	0.077	1.00					
	19.5 (6.11)	Ш	1	0.80		2.50		1.16					
		III	1	0.80		2.50 5.11	0.131	1.16					
		D	1	0.85 1.02	0.10	3.90		1.00					
	2 4F1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 -	D III	1	0.95		3.40	0.077	1.00					-
	a) eletterialization (contract)	111	1	0.87		3.42	0.083	1.01	5,500				
	S) significant	D	1	0.78		2.90	0.116	1.09					0.09
		D	1	0.95		3.45		1.00			5579	0.023	
	S) GIOTIONALIOI	D	2	0.69		4.55	0.080	1.01	5,500	5528			
		D	1	0.86	0.11	4.62	0.078	1.00	5,500				
		111	1	1.11	0.80	3.88	0.087	1.02					
		111	1	1.05		3.72	0.077	1.00					
		D	1	0.86		4.20	0.085	1.01	5,500				
31 IDA		D	1	0.83		5,00	0.076	1.00					_
	Described (i.)	D	1	0.83		5.01	0.076	1.00					-
	0000110	D	11	0.74		4.80	0.078	1.00					
	Boolin decire (an insurance)	D	1	0.83		5.30	0.076	1.00					
	Decylbenzene (n-)	D	- 1	0.86		7.52	0.076	1.00					
	Diddotollo i dadile.	D	1	0.97	9.90	4.00 3.41	0.078	1.20					1
	THE PROPERTY OF THE PROPERTY O	III D	1	1.05		9.59							
	Dibutyl Phthalate (ortho-)	D	1	0.87	0.08	4.62	0.078	1.00					
	Diethybenzene Diethylene Glycol	D	1	1.12		3.66						0.023	0.0
	Diethylamine	111	3	0.71	1.00	2.50		1.02			5864	0.026	
	Diisobulylene	D	1	0.72		3.86		1.04	5,500	5720	6654		
		D	1	0.81	0.16	4.90	0.079	1.00					
	Diisopropanolamme	00	1	0.98		4.59							
45 DIX		D	1	0.86		5.60		1.00					-
	- miles iji i i i i i i i i i i i i i i i i i	D	1	1.19		6.69							
	Diodiji i ittidiata	D	1	0.98							-		
	- F	D	1	0.84		4.90							
	Diphenyl	D	1	0.99		5.31 5.86							
	Diphenyl, Diphenyl Ether Mixtures	111	1	0.95					-				
		D	1	1.07	0.01	5.87							0.0
	Diphenyl Ether Dipropylene Glycol	D	1	1.03		4.63							0.0
		111	3	1.16						6193	9034		
	Distillates Flashed Feed Stocks	D	1	0.75		3.40	0.102	1.05	5,500	5753			
	Distillates Straight Run	D	1	0.73	2.30	3.40	0.102						
	Dodecene (all isomers)	D	1	0.76	0.02	5.81	0.077	1.00					
	Dodecylbenzene	D	1	0.86									
	Ethyl Acrylate	Ш	2	0.93									
60 EAI	2-Ethylhexyl acrylate	Ш	2	0.89				1.00					
	2-Ethoxyethyl acetate	D	1	0.97		4.70							
	Ethoxy Triglycol (crude)	D	1	1.02									1000
	Ethyl Acetate	D	1	0.90									
	Ethyl Acetoacetate	D	1	1.03						_		_	
	Ethyl Alcohol (Ethanol)	D	1	0.79									
	Ethyl Benzene	D	1	0.87									
	Ethyl Butanol	D D	1										_
	Ethyl tert-butyl ether	D	1										
	Ethyl butyrate	D	1	0.79									
	Ethyl Cyclohexane Ethylene dichloride	III	1										-
	Ethylene Glycol	III	1	1.19		2.21							3 0.0
	Ethylene Glycol Butyl Ether Acetate	D	1	0.94						-			3 0.
	Ethylene Glycol Diacetate	D	1	1.10	-	5.03							
	Ethylene Glycol Phenyl Ether	D	1			4.80					5508		
76 EEP	Ethyl-3-ethoxypropionate	D	1	0.95	0.01	5.00	0.076	1.00					
	2-Ethylhexanol (Octanol)	D	1	0.84									
	The state of the s	D	1	0.89	3.50	1.60	0.086	1.07	5,500	5885	6255	0.030	0.0

- 1	CHRIS Code	Name	Туре	VCS Category	Liquid S.G.	"Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (lb/ft^3)	Vapor Growth Rate	Max. Loading Rate	Vapor Volumetric Flow Rate (bbl/hr)	Air Equivalent Volumetric Flow Rate (bbl/hr)	Pressure Drop to PV Valve in VCS (See Table 3) (psig)	Pressure Drop to Facility Connection in VCS (S Table 5) (psig)
79	ETE	Ethyl Toluene	D	1	0.88		4.15		1.01	5,500				
		Formamide	D	1	1.13	0.10	1.55			5,500				
		Formaldehyde Solution	111	1	1.13		1.03		1.00					
	FAL	Furfuryl Alcohol	D	1	1.13		3.40		1.00					
33	FFA	Furfural	01	1	1.20		3.31	0.078						
	GAK	Gasoline Blending Stocks: Alkylates	D	1	0.75		3.40		1.25					
	GRF	Gasoline Blending Stocks: Reformates	D	1	0.80	12.50	3.40		1.25					-
	GAT	Gasolines: Automotive	D	1	0.74	12.50	3.40		1.25					-
	GAV	Gasolines: Aviation	D	1	0.71	12.50 12.50	3.40		1.25	5,500				
	GCS	Gasolines: Casinghead	D	1	0.67		3.40		1.25					
	GPL	Gasolines: Polymer	D	1	0.75		3.40		1.25	5,500				
	GSR GCR	Gasolines: StraightRun Glycerine	D	1	1.26	0.00	3.17	0.076	1.00					
	HMX	Heptane (all isomers)	D	1	0.68	2,50	3.45		1.05			6779	0.035	
	HEP	Heptonic Acid	D	1	0.92		4.49		1.00	5,500	5501	5507	0.023	(
	HTX	Heptanol (all isomers)	D	1	0.82	0.04	4.00	0.077	1.00	5,500	5504			
	HPX	Heptene (all isomers)	D	2	0.70		3.40		1.06	5,500	5819	6958		
	HXS	Hexane (all isomers)	D	1	0.66	7.00	3.00	0.142	1.14	5,500	6270			
	HXO	Hexaonic Acid	D	1	0.93	0.01	4.00	0.076	1.00	5,500				
	HXN	Hexanol	D	1	0.82		3.52		1.02					
	HEX	Hexene (all isomers)	D	2	0.67	8.00	2.90		1.16					
	HXG	Hexylene Glycol	D	1	0.92		1.10		1.00					
01	IPH	Isophorone	D	1	0.93	0.01	4.75		1.00					
02	JPF	Jet Fuels: JP-4	D	1	0.81	3.40	4.00		1.07					
	JPV	Jet Fuels JP-5 (Kerosene, heavy)	D	1	0.82		4.00		1.00					-
	KRS	Kerosene	D	1	0.81	0.15	4.50		1.00					
		Methyl Acetate	D	1	0.92		2.60		1.12					
		Methyl Alcohol (Methanol)	D	1	0.79		1.10 4.97	0.079	1.01	5,500				_
		Methylamyl Acetate	D	1	0.86	0.33	3.52		1.01	5,500				
	MAA	Methylamyl Alcohol	D	1	0.81		1.00		1.00					
		Methylamyl Keytone	III	2			3.00		1.08					
	MAM MBE	Methyl Acrylate Methyl Tert-Butyl Ether (MTBE)	D	1	0.74		3.10		1.00				0.023	3
		Methyl Butyl Ketone	D	1	0.81	0.97	3.50		1.02				0.027	(
		Methyl Butyrate	D	1	0.90		3.53		1.03	5,500	5639	6168	0.029	
	MEK	Methyl Ethyl Ketone	D	1	0.80		2.50		1.09	5,500	5995	7135	0.038	
		Methyl Heptyl Ketone	D	1	0.83	0.06	4.90	0.077	1.00	5,500	5507			
	MIK	Methyl Isobutyl Ketone	D	1	0.80	1.15	3.45	0.089	1.02	5,500	5627			
	MMM	Methyl methacrylate	111	2	0.94	2.02	3.45		1.04					
	MNA	Methyl Naphthalene	D	1	1.02		4.91	0.076	1.00					
	MNS	Mineral Spirits	D	1	0.75		4.30							
	MPL	Morpholine	111	1	1.00		3.00		1.02					
	MRE	Myrcene	D	1	0.80		4.70		1.00					_
	PTN	Naphtha: Petroleum	D	1	0.74		3.50							
	NSV	Naphtha: Solvent	D	1	0.87		3.50 4.30							
	NSS	Naphtha: Stoddard Solvent	D	1	0.78	0.19	4.30							
	NVM	Naphtha: VM&P	D	1	0.77		4.40			5,500				-
	NAX	Nonane (all isomers)	D	2	0.72	-	_	200	1 1-1					
	NON NNS	Nonene (all isomers) Nonyl Alcohol (all isomers)	D	1	0.94									
	NNP	Nonyl Phenol	D	1	0.95		7.60					5512	0.023	
	NPM	1-, 2-Nitropropane	III	1	0.99	1.05	3.06	0.086	1.02	5,500	5616	5979		
	OAX	Octane (all isomers)	D	1				0.087						
	OCX	Octanol (all isomers)	D	1	0.83	0.01	4.48	0.076						-
	OTX	Octene (all isomers)	D	2				-						
	OTW	Oil, fuel: No. 2	D	1										
35	OTD	Oil, fuel: No. 2-D	D	1										
	OFR	Oil, fuel: No. 4	D	1	0.90									_
	OFV	Oil, fuel: No. 5	D	1										-
	osx	Oil, fuel: No. 6	D	1						-			_	
	OIL	Oil, misc: Crude	0	1	0.95									
	ODS	Oil, Misc: Diesel	D	1	0.90		_							
	OLB	Oil, Misc: Lubricating	D	1						-				-
	ORL	Oil, Misc: Residual	D	1										_
	OTB	Oil, Misc: Turbine	D	5					_					-
	PTY	Pentane (all isomers) Pentene (all isomers)	D	5									-	
	PIN	Pinene	D	1	0.86				-		-		1010	-
	PLB	Polybutene	D	1		-	1.00				_			_
	PGC	Polypropylene Glycol	D	1	1.01		_				-			3
	IAC	Propyl Acetale (iso-)	D	1	0.89									1
	PAT	Propyl Acetale (Iso-)	D	1	-								0.032	1
	IPA	Propyl Alcohol (iso-)	D	1								6382		
	PAL	Propyl Alcohol (n-)	D	1				-			5632			
	PBY	Propylbenzene (all isomers)	D	1							5522			-
	IPX	iso-Propylcyclohexane	D	1			4.35							
	PPG	Propylene Glycol	D	1		-	2.62	0.076						
	PGN	Propylene Glycol Methyl Ether Acetate	D	1	0.92									-
	PTT	Propylene Tetramer	D	1	0,29									
	SFL	Sulfolane	D	1										
	STY	Styrene	10	2								-		
	TTG	Tetraethylene Glycol	D	1		0.01	6.70	0.076	1.00	5,500	550	1 551	0.023	31

	CHRIS Code	Name	Туре	VCS Category	Liquid S.G.	*Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (lb/ft^3)	Vapor Growth Rate	Max. Loading Rate		Volumetric Flow Rate (bbl/hr)	Drop to PV Valve in VCS (See Table 3) (psig)	Connection in VCS (See Table 5) (psig)
161	THN	Tetrahydronaphthalene	D	1	0.97	0.04	4.56		1.00					
	TOL	Toluene	D	1	0.87	1.50	3.14	0.091	1.03				0.029	
	TCN	1,2,3-Trichloropropane	11	3	1.39	0.15	5.60		1.00			5633	0.024	
	TCP	Tricresyl Phosphate (less than 1% of ortho	D	1	1.16	0.01	12.69	0.077	1.00	5,500		5521	0.023	_
	TEB	Triethylbenzene	D	1	0.86	0.02	5.60	0.077	1.00	5,500				
	TEN	Triethylamine	11.	3	0.73	2.50	3.49	0.105	1.05	5,500			0.035	
	TEG	Triethylene Glycol	D	1	1.12	0.01	5.17	0.076	1.00			5508	0.023	
168	TPS	Triethyl Phosphate	D	1	1.07	0.03	6.28	0.077	1.00				0.023	
	TRE	Trimethylbenzene (all isomers)	D	1	0.89	0.14	4.20	0.078	1.00	5,500			0.024	
	TRP	Trixylenyl Phosphate	D	1	1.16	0.00	14.20	0.076	1.00	5,500			0.023	
171	THE	Tetrahydrofuran	III	1	0.89	8.50	1.35		1.17	5,500			0,037	0.084
_	UDC	Undecene	D	1	0.75	0.05	5.32	0.077	1.00			100000000000000000000000000000000000000	0.023	
173	UND	Undecyl Alcohol	D	1	0.84	0.01	5.94					5509	0.023	0.052
_	VAM	Vinyl Acetate	III	2	0.94	5.80	2.97	0.130						
_	XLX	Xylenes (ortho-, meta-, para-)	D	1	0.89	0.51	3.68	0.083	1.01	5,500	5556	5786	0.025	0.058

max = 0.350 1.54 max = 0.249 0.567

1. The above data is sourced from the USCG CHRIS Manual (Ref. 7) & from various manufacturer's MSDS's.

Notes:

Calculation of Maximum Liquid Transfer Rate as Imposed by the Capacity of the Cargo Tank Venting System

Note: Darcy's equation will be used to estimate the pressure drop of the vapor-air mixture through the vent piping from the farthest tank in terms of equivalent pipe length, #1P to the P-V valve. Equivalent length for this path is calculated using Crane's Technical Paper 410 (Ref 4) and Cameron Hydraulic Data handbook (Ref 9).

Calculate equivalent lengths of pipe:

Table 2

a. Pipe run #1

Description:

8" Branch (Exp trunk to vapor stack)

Pipe size, nominal:

8" sch. 40 pipe

Pipe ID (inches):

7.98

Item	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
1	Entrance	8	1	23.3	23.3
2	Straight Pipe	8	1	53.0	53.0
3		8	2	40.0	80.0
4	Tee, flow	8	1	14.0	14.0
5		- 1			0.0
6					1
	Sum (pipe run #1)				170.3

b. Pipe run #2

Description: 6" branch at P-V valve

Pipe size, nominal: 6" sch. 40 pipe

Pipe ID (inches): 6.07

Item	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
1	Straight Pipe	6	1	3.0	3.0
	Sudden Contraction (8x6)	6	1	8.0	8.0
	Sum (pipe run #2)				11.0

Table 3 Calculation of Maximum Liquid Transfer Rate as Imposed by the Capacity of the Cargo Tank Venting System (Continued)

A. Calculate pressure drop using Darcy's equation:

| Pipe run #1 | 8" Branch (Exp trunk to vapor | Description: stack) | Pipe ID: | Description: 6" branch at P-V valve | Pipe ID: | 6.07 (in) | Pipe ID: | P

							factor:	0.015	5			
CHRIS Code	Name	Vapor-air Mixture Weight Density (from Table 1) (lb/ft^3)	Liquid Transfer Rate (filling) (bbl/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ft/s)	Pressure Drop (pipe run #1) (psig)	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ft/s)	Pressure Orop (pipe run #2) (psig)	Pressure Drop (Total) (psig)	Air Equiv. Volumetri Flow Rate (bbl/hr)
	Acrylonitrile	0.095						6050 6600				3 83
	Acetone Acetophenone	0.085			5566	24.99	0.021	5566	43.19	0.006		
AND	Adiponitrile	0.076				24.70		5501 5536				
AEC AAI	Amyl Alcohol (iso-, n-, sec-, primary)	0.075						5533		4 0.005	0.02	24 56
	Acetonitrile	0.076	5,500	1.001	5503	24.7	0.018	5503				
BAL	Benzyl Alcohol	0.077				24.74 30.87		5511 6875				
BNZ	Benzene Benzene, Toluene, Xylene mixtures (10% Benze	0.114 0.138						6875	53.35	0.014	0.06	55 92
BAR	Butyl Acrylate (iso-, n-)	0.086	5,500	1.012				5566				
	Butyl Acetate (all isomers)	0.085	5,500 5,500					5566 5599				
BAN	Butyl Alcohol (iso-) Butyl Alcohol (n-)	0.074						5555	43.11	0.005	0.02	23 54
	Butyl Alcohol (sec-)	0.086	5,500	1.026	5643			5643				
	Butyl Alcohol (tert-)	0.097	5,500			26.08		5808 5501				
	Butyl Benzyl Phthalate iso-Butyraldehyde	0.077						6358	49.34	4 0.011	0.05	
	n-Butyraldehyde	0,131	5,500	1.156	6358			6358				
BUE	Butyl Toluene	0.078				24.74		5511 5506				
CLS	Caprolactam Solutions Cyclohexanone (Anolone)	0.077	5,500			24.79		5522	42.85	0.005	0.02	24 56
CHA	Cyclohexylamine	0.083	5,500	1,012	5568	25.00		5568				
CHX	Cyclohexane	0.116				26.92 24.77		5995 5517				
CHN	Cyclohexanol 1,3-Cyclopentadiene dimer (molten)	0.078				24.82	0.019	5528	42.90	0.005	0.02	24 56
	p-Cymene	0.078	5,500	1.002	5512	24.75	0.018	5512				
CRB	Chlorobenzene	0.087						5588 5509				
CRS	Cresols Cumene	0.077						5566	43.19	0.006	0.02	26 51
IDA	Decaldehyde (iso-)	0.076	5,500	1.000	5501	24.70	0.018	5501				
DAL	Decaldehyde (n-)	0.076				24.70		5500 5513				
DCE	Decene Deced Alcohol (all isomers) (Decanol)	0.078	5,500			24.70		5501	42.69	9 0.005	0.02	23 5
DAX	Decyl Alcohol (all isomers) (Decanol) Decylbenzene (n-)	0.076	5,500	1.000	5501	24.70	0.018	5501	42.69			
DAA	Diacetone Alcohol	0.078	5,500			24.74		5511 6589				
DCH	1,1-Dicholoroethane	0.188	5,500			29.59		5500				23 5
DPA	Dibutyl Phthalate (ortho-) Diethybenzene	0.078				24.73	0.018	5509	42.75	5 0.005		
DEG	Diethylene Glycol	0.076				24.70		5501 5610				
DEN	Diethylamine	0.083	5,500					5720				
DBL	Diisobulylene Diisobutyl Ketone	0.103						5518	42.82	2 0.005	5 0.02	
DIP	Diisopropanolamme	0.076	5,500	1.000	5501	24.70		5501				
DIX	Diisopropylbenzene (all isomers)	0.077	5,500			24.7		5503 5500				
DOP	Dimethyl Phthalate Dioclyl Phthalate	0.076						5500	42.68	0.005	0,02	
DPN	Dipentene	0.078				24.7		5511				
DIL	Diphenyl	0.076				24.70	0.018	5501 5501				
DDO	Diphenyl, Diphenyl Ether Mixtures Dimethylformamide	0.078				24.84		5533	42,94	4 0.005	0.02	24 5
DPE	Diphenyl Ether	0.076				24.70		5501 5508				
DPG	Dipropylene Glycol	0.077	5,500		5508			6193				62 9
DFF	1,1-, 1,2-, 1,3-Dichloropropane Distillates Flashed Feed Stocks	0.102				25.83	3 0.026	5753				
DSR	Distillates Straight Run	0.102						5753 5502				
DOZ	Dodecene (all isomers)	0.077	5,500					6875				
DDB	Dodecylbenzene Ethyl Acrylate	0.100					8 0.025	5720				
EAL	2-Ethylhexyl acrylate	0.077						5502 5503				
EEA	2-Ethoxyethyl acetale	0.077						5500				23 5
ETG	Ethoxy Triglycol (crude) Ethyl Acetate	0.119			5995	26.93	2 0.033	5995				
EAA	Ethyl Acetoacetate	0.079						5522 5885				
EAL	Ethyl Alcohol (Ethanol)	0.086						5566			5 0.00	26
EBT	Ethyl Benzene Ethyl Butanol	0.078									5 0.0	
EBE	Ethyl tert-butyl ether	0.078									-	
EBR	Ethyl butyrate	0.090						5555	43.11	1 0.005	5 0.0	25
EDC	Ethyl Cyclohexane Ethylene dichloride	0,122	5,500	1.080	5940	26.6	7 0.033	5940	46.10			
EGL	Ethylene Glycol	0.076	5,500									
EMA	Ethylene Glycol Butyl Ether Acetate Ethylene Glycol Diacetate	0.077			5506				42.69	9 0.009	5 0.0	23
EGY	Ethylene Glycol Phanyl Ether	0.076	5,500	1.000	5501	24.7	0.018	5501				
EEP	Ethyl-3-ethoxypropionate	0.076	5,500	1.000								
EHX	2-Ethylhexanol (Octanol)	0.076									6 0.0	30
EPR	Ethyl Propionate Ethyl Toluene	0.080	5,500	1.006	5531	24.8	3 0.019	5531	42.92	2 0.00	5 0.0	24
FAM	Formamide	0.076	5,500	1.002								
FMS	Formaldehyde Solution	0.076									5 0.0	23
FAL	Furfuryl Alcohol Furfural	0.078			5517	24.7	7 0.018	5517	42.81	1 0.00	5 0.0	23
GAK	Gasoline Blending Stocks: Alkylates	0.217	5,500	1.250	6875	30.8						
GRF	Gasoline Blending Stocks: Reformates	0.217										
GAT	Gasolines: Automotive Gasolines: Aviation	0.217						6875	.53.35	5 0.02	2 0.1	02 1
GAV GCS	Gasolines: Casinghead	0.217	5,500	1,250	6875	30.8	7 0.080	6875				
GPL	Gasolines: Polymer	0.217	5,500	1.250								
GSR	Gasolines: StraightRun	0.217									5 0.0	23
GCR 2 HMX	Glycerine Heptane (all isomers)	0.105			5775	25.9	3 0.02	5775	44.82	2 0.00	7 0.0	
HEP	Heptonic Acid	0 076	5,500	1.000	5501							
4 HTX	Heptanol (all isomers)	0.077										
5 HPX 5 HXS	Heptene (all isomers) Hexane (all isomers)	0.109						6270	48.66	6 0.01	2 0.0	155
TIMO	Hexaonic Acid	0.076	5,500	1.000	5501	24.7	0 0.011					
HXO		0.088	5,500	1.020	5610	25.1	9 0.023	5610	43.54	4 0.00	6 0.0	127

Pipe run #1	Administration	Pipe run #2		
Description:	8" Branch (Exp trunk to vapor stack)	Description:	6" branch at P.V valve	
Pipe ID:	7.98 (in)	Pipe ID:	5.07 (in)	
Equiv. Pipe	7.5.4.4	Equiv. Pipe		
Length (table		Length (table		
2a):	170.3 (feet)	2b):	11.0 (feet)	
Darcy friction		Darcy friction		
factor:	0.014	factor:	0.015	

						factor:	0.014		factor:	0.015	1	-	T
	CHRIS Code	Name	Vapor-air Mixture Weight Density (from Table 1) (lb/ft^3)	Liquid Transfer Rate (filling) (bbl/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ft/s)	Pressure Drop (pipe run #1) (psig)	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ft/s)	Pressure Drop (pipe run #2) (psig)	Pressure Drop (Total) (psig)	Air Equiv Volumet Flow Rai (bbl/hr)
00	IXG	Hexylene Glycol	0.076			5501	24.70		5501	42.69 42.69		0.023	
01		Isophorone	0.076			5501	24.70		5501 5874	45.58			
02		Jet Fuels: JP-4	0.124			5874	26.37		5511	42.77			
03		Jet Fuels JP-5 (Kerosene, heavy)	0.078			5511	24.74		5517	42.81			
04	KRS	Kerosene	0.079	5,500	1.003	5517 6171	24.77 27.71		6171	47.89			
05		Methyl Acetate	0.122			6229	27.97		6229	48.34			
06	MAL	Methyl Alcohol (Methanol)	0.079			5536	24.86		5536			0.025	5 5
	MAC	Methylamyl Acetate	0.081	5,500	1.009	5547	24.91		5547	43.05	0.005		5 5
	MAA MAK	Methylamyl Alcohol Methylamyl Keytone	0.076			5506	24.72	0.018	5506	42.72			
	MAM	Methyl Acrylate	0.115			5951	26.72	0.032	5951	46.18			
	MBE	Methyl Tert-Butyl Ether (MTBE)	0.077	5,500		5504	24.72		5504				
	ивк	Methyl Butyl Ketone	0.088			5607	25.17	0.021	5607	43.51			
		Methyl Butyrate	0.091		1.025	5639	25.32		5639	43.76			
	MEK	Methyl Ethyl Ketone	0.108			5995	26.92		5995				
	MHK	Methyl Heptyl Ketone	0.077			5507	24.73		5507 5627	42.73			
16	MIK	Methyl Isobutyl Ketone	0.089			5627	25.26		5722	44.4			
	MMM	Methyl methacrylate	0.099			5722	25.69		5501	42.69			
	MNA	Methyl Naphthalene	0.076			5501 5522	24.70 24.79		5522	42.85			
	MNS	Mineral Spirits	0.079			5522	25.09		5588				
20		Morpholine	0.084			5519	24.78		5519	42.83		0.024	4 !
	MRE	Myrcene	0.079		1.003	5521	24.79		5521	42.84		0.024	
22		Naphtha: Petroleum	0.078			5522	24.79		5522	42.85	0.005	0.024	
24 1		Naphtha: Solvent Naphtha: Stoddard Solvent	0.079			5522	24.79	0.019	5522	42.85			
		Naphtha: VM&P	0.079			5521	24.79	0.019	5521	42.84		0.024	
26		Nonane (all isomers)	.0.080			5530	24.83	0.019	5530	42.91			4
		Nonene (all isomers)	0.082	5,500		5539	24.87		5539	42.98		0.025	
	NNS	Nonyl Alcohol (all isomers)	0.078	5,500		5511	24.74	0.018	5511	42.71			
		Nonyl Phenol	0.076	5,500		5501	24.70		5501	42.69			
	VPM	1-, 2-Nitropropane	0.086			5616	25.21	0.021	5616				
31		Octane (all isomers)	0.087			5587	25.09		5587 5501	43.36 42.69			
32 (CX	Octanol (all isomers)	0.076			5501	24.70		5599	43.45			
		Octene (all isomers)	0.088			5599	25.14		5562				
		Oil, fuel: No. 2	0.095			5562 5576	24.97 25.04	0,023	5576				
		Oil, fuel: No. 2-D	0.084	5,500		5517	24.77		5517				
		Oil, fuel: No. 4	0.078			5517	24.77		5517	42.81			
37 (OFV	Oil, fuel: No. 5	0.078			5517	24.77	0.018	5517				3
		Oil, fuel: No. 6	0.078			6875	30.87	0.029	6875		0.008	0.036	
39 0		Oil, misc: Crude Oil, Misc: Diesel	0.084			5576	25.04		5576			0.026	6
		Oil, Misc: Lubricating	0.076			5517	24.77		5517	42.8			
42 (Oil, Misc: Residual	0.076			5517	24.77		5517				
		Oil, Misc: Turbine	0.082			5533	24.84		5533				
	PTY	Pentane (all isomers)	0.350		1.540	8470	38.03		8470				
	PTE	Pentene (all isomers)	0.310	5,500		8245	37.02		8245	63.98		0.209	
46	PIN	Pinene	0.083			5542	24.88		5542	43.0			
47	PLB	Polybutene	0.076			5501	24.70		5501	42.69			
48	PGC	Polypropylene Glycol	0,076			5511	24.74		5511 5698				
	AC	Propyl Acetate (iso-)	0.097			5698	25.58		5704				
	PAT	Propyl Acetate (n-)	0.098			5704 5830	25.61 26.18		5830				
1 1		Propyl Alcohol (iso-)	0.091	5,500		5632	25.29		5632				
	PAL	Propyl Alcohol (n-)	0.082			5522	24.79		5522	42.85	0.005	0.024	4
	PX	Propylbenzene (all isomers) iso-Propylcyclohexane	0.076			5501	24.70		5501	42.69	0.005	0.023	3
	PPG	Propylene Glycol	0.076			5501	24.70	0,018	5501	42.65			
	PGN	Propylene Glycol Methyl Ether Acetale	0.083			5577	25.04		5577	43.2			
		Propylene Tetramer	0.076	5,500	1.000	5502	24.71		5502	42.79			
	SFL	Sulfolane	0.076	5,500		5501	24.70	0.018	5501	42.65			
	STY	Styrene	0.081	5,500		5544	24.89		5544	43.00			
	ITG	Tetraethylene Glycol	0.076	5,500		5501	24.70		5501 5504				
	THN	Tetrahydronaphthalene	0.077	5,500	1.001	5504	24.72		5665				
	TOL	Toluene	0.091	5,500	1.030	5665	25.44 24.77		5517				
	TCN	1,2,3-Trichloropropane	0.079			5517 5501	24.70		5501				
	TCP	Tricresyl Phosphate (less than 1% of ortho isome	r 0.077			5502			5502				
	TEB	Triethylbenzene	0.077		1.050	5775	25.93		5775		2 0.007		
	TEN	Triethylamine	0.105	5,500	1.000	5501	24.70		5501	42.6	9 0.005		
	TEG	Triethylene Glycol	0.077		1.001	5503	24.71		5503		1 0.005	0.02	23
0	TPS	Triethyl Phosphate Trimethylbenzene (all isomers)	0.078	5,500	1.003	5515			5515	42.81	0.005		
	TRP	Trixylenyl Phosphate	0.076			5500	24.70		5500				
	THE	Tetrahydrofuran	0.090			6435	28.89	0.029	6435	49.9			
	UDC	Undecene	0.077			5506	24.72		5506		2 0.005		
	UND	Undecyl Alcohol	0.076			5501	24.70	0.018	5501				
	VAM	Vinyl Acetate	0.130			6138	27.56	0.038	6138				
		Xylenes (ortho-, meta-, para-)	0.083			5556	24.95	0,020	5556	43.1			
											max ≃		

High velocity P-V valve pressure setting: Valve setting + pressure drop in piping = Back pressure imposed by P-V valve @ highest flow rate Total back pressure imposed on cargo tank by venting Max design working pressure of tanks;	1.50 (psig) 1.75 (psig) 2.64 (psig) 2.89 (psig) 3.00 (psig)	ок	Conclusion:	At the maximum carga loading rate, the total back pressure imposed by the tank venting system does not exceed the maximum design working pressure of the tanks.
Check vacuum relieving capacity at maximum discharge rate: Opening vacuum setting for PV Valve: Maximum discharge rate (total):	0.5 (psig) 4300 (bbl/hr)	402 cfm		
Corresponding vacuum at max discharge rate: (see attached PV valve flow capacity curve)	0.49 (psig)			

В.

Table 4

Calculation of the Maximum Liquid Transfer Rate as Imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 46 CFR 39.30-1(d)(3):

Note: Darcy's equation will be used to estimate the pressure drop of the vapor-air mixture through the vent piping from the farthest tank in terms of equivalent pipe length, #1P to the facility connection. Equivalent length for this path is calculated using Crane's Technical Paper 410 (Ref. 4) and Cameron Hydraulic Data handbook (Ref. 9)

Calculate equivalent lengths of pipe:

a. Pipe run #1

Description: 8" Piping
Pipe size, nominal: 8" sch. 40 pipe

Pipe ID (inches): 7.98

ltem	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
1	Entrance	8	1	23.3	23.3
	Straight Pipe	8	1	190.0	190.0
3		8	2	40.0	80.0
4		8	7	14.0	98.0
5	Elbow, 90 deg.	8	0	14.0	0.0
	Elbow, 45 deg.	8	4	11.0	44.0
	Valve, Gate	8	1	8.6	8.6
	Hose	8	1	50.0	50.0
	Sum (pipe run #1)				493.9

Calculation of the Maximum Liquid Transfer Rate as Imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 46 CFR 39.30-1(d)(3) (continued):

Calculate pressure drop using Darcy's equation:

Pipe run #1
Description:
Pipe ID:

8" Piping

7.98 (in)

Equivalent Length of Pipe (from Table 4a):

493.9 (feet)

					Darcy friction factor:	0.014		7	1
CHRIS Code	Name	Vapor-air Mixture Weight Density (from Table 1) (lb/ft^3)	Liquid Transfer Rate (filling) (bbl/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity	Pressure Drop (pipe run #1) (psig)	Pressure Drop (Total) (psig)	Air Equivaler Volumetric F Rate (bbl/hr)
1 ACN	Acrylonitrile	0.095	5,500		6050	27.16	0.079	0.079	
2 ACT	Acetone	0.123	5,500		5566 5566	29.63 24.99		0.060	
	Acetophenone	0.085 0.076				24.70	0.052	0.052	
4 AND 5 AEC	Adiponitrile Amyl acetate (all isomers)	0.075		1.007	5536	24.86		0.052	
6 AAJ	Amyl Alcohol (iso-, n-, sec-, primary)	0.079	5,500			24.84		0.055 0.052	-
	Acetonitrile	0.076	5,500		5503 5511	24.71		0.053	+
8 BAL	Benzyl Alcohol	0.077	5,500 5,500			30.87		0.122	
9 BNZ	Benzene Benzene, Toluene, Xylene mixtures (10% Benzene	0,138		1.250		30.87	0.147	0.147	- 1
0 BTX 1 BAR	Butyl Acrylate (iso-, n-)	0.086		1.012	5566	24.99		0.060	
	Butyl Acetate (all isomers)	0.085	5,500			24.99 25.14		0.059	1
3 IAL	Butyl Alcohol (iso-)	0.083	5,500			24.94		0.052	1
	Butyl Alcohol (n-)	0.074 0.086	5,500 5,500					0.062	
5 BAS 6 BAT	Butyl Alcohol (sec-) Butyl Alcohol (tert-)	0.097	5,500			26,08	0.074	0.074	
7 BPH	Butyl Benzyl Phthalate	0.077	5,500	1.000		24.70		0.052 0.120	+
8 BAD	iso-Butyraldehyde	0.131	5,500			28.55 28.55		0.120	1
9 BTR	n-Butyraldehyde	0.131	5,500 5,500			24.74		0.054	
0 BUE	Butyl Toluene	0.078	5,500				0.053	0.053	
1 CLS 2 CCH	Caprolactam Solutions Cyclohexanone (Anolone)	0.078			5522	24.79		0.054	
3 CHA	Cyclohexylamine	0.083	5,500					0.058 0.094	-
4 CHX	Cyclohexane	0.116						0.054	-
CHN	Cyclohexanol	0.078	5,500 5,500			24.82		0.055	
CPD	1,3-Cyclopentadiene dimer (molten)	0.078			5512	24.75	0.054	0.054	
7 CMP 8 CRB	p-Cymene Chlorobenzene	0.087	5,500	1.016	5588	25.09		0.061	-
CRS	Cresols	0.077	5,500	1.002				0.053 0.052	-
DTL	Dimethyl Phthalate	0.076		1.000				0.052	
7 DOP	Dioclyl Phthalate	0.076				24.74		0.054	
B DPN B DIL	Dipentene Diphenyl	0.076			5501	24.70	0.052	0.052	4
0 DDO	Diphenyl Diphenyl Ether Mixtures	0.076		1.000		24.70		0.052	
1 DMF	Dimethylformamide	0.078				24.84		0.054 0.052	-
2 DPE	Diphenyl Ether	0.076						0.053	
3 DPG	Dipropylene Glycol	0.077						0.140	
4 DPX	1,1-, 1,2-, 1,3-Dichloropropane Distillates Flashed Feed Stocks	0.102				25.83	0.076	0.076	
5 DFF 6 DSR	Distillates Straight Run	0.102		1.046				0.076	
DOZ .	Dodecene (all isomers)	0.077						0.052 0.256	
8 DDB	Dodecylbenzene	0.240						0.074	
9 EAC	Ethyl Acrylate	0.100						0.052	
0 EAI 1 EEA	2-Ethylhexyl acrylate 2-Ethoxyethyl acetate	0.077			5503	24.7	0.052	0.052	
ETG	Ethoxy Triglycol (crude)	0.076		1.000				0.052 0.097	
3 ETA	Ethyl Acetate	0.119						0.055	
4 EAA	Ethyl Acetoacetate	0.079						0.067	
5 EAL	Ethyl Alcohol (Ethanol)	0,086						0.058	11
6 ETB 7 EBT	Ethyl Benzene Ethyl Butanol	0.078		1.00	5513			0.053	
8 EBE	Ethyl tert-butyl ether	0.078						0.054 0.064	
9 EBR	Ethyl butyrate	0.090						0.058	+
0 ECY	Ethyl Cyclohexane	0.083						0.097	
1 EDC	Ethylene dichloride Ethylene Glycol	0.076				24.7		0.052	1
2 EGL 3 EMA	Ethylene Glycol Butyl Ether Acetate	0.077	5,500	1.00				0.053	_
4 EGY	Ethylene Glycol Diacetate	0.076						0.052 0.052	
5 EPE	Ethylene Glycol Phenyl Ether	0.076						0.052	
6 EEP	Ethyl-3-ethoxypropionate	0.076	5,500					0.052	
7 EHX 8 EPR	2-Ethylhexanol (Octanol) Ethyl Propionate	0.076			5885	26.4	2 0.067	0.067	
9 ETE	Ethyl Toluene	0.080	5,500	1.00	5531			0.056	
0 FAM	Formamide	0.076						0.052 0.052	
1 FMS	Formaldehyde Solution	0.078						0.053	
2 FAL	Furfuryl Alcohol	0.07						0.053	
4 GAK	Gasoline Blending Stocks; Alkylates	0.21	5,500	1.25	6875			0.232	
5 GRF	Gasoline Blending Stocks: Reformates	0.21	5,500	1.25				0.232 0.232	
6 GAT	Gasolines: Automotive	0.21						0.232	
7 GAV	Gasolines: Aviation	0.21						0.232	
8 GCS 9 GPL	Gasolines: Casinghead Gasolines: Polymer	0.21			6875	30.8	7 0.232	0.232	
0 GSR	Gasolines: StraightRun	0.21	5,500	1.25	0 687			0.232 0.052	
1 GCR	Glycerine	0.07	5,500					0.052	
2 HMX	Heptane (all isomers)	0.10						0.052	
3 HEP	Heptonic Acid	0.07					2 0.053	0.053	
4 HTX 5 HPX	Heptene (all isomers) Heptene (all isomers)	0.10		1.05	8 581	26.1	3 0.083	0.083	
6 HXS	Hexane (all isomers)	0.14	2 5,500	1.14	0 627			0.126	-1-
7 HXO	Hexaonic Acid	0.07						0.052 0.063	
8 HXN	Hexanol	0.08						0.003	
99 HEX	Hexene (all isomers)	0.14						0.052	
00 HXG	Hexylene Glycol Isophorone	0.07			0 550	24.7	0 0.052	0.052	
12 JPF	Jet Fuels: JP-4	0.12	4 5,50	1,06	8 587			0.097	
33 JPV	Jet Fuels JP-5 (Kerosene, heavy)	0.07	5,50	1.00				0.053 0.054	
04 KRS	Kerosene	0.07						0.105	1
5 MTT	Methyl Acetate	0.12						0.070	
06 MAL 07 MAC	Methyl Alcohol (Methanol) Methylamyl Acetate	0.07		1.00	7 553	5 24.8	6 0.057	0.057	
08 MAA	Methylamyl Alcohol	0.08	1 5,50	1.00	9 554			0.057	
09 MAK	Methylamyl Keytone	0.07						0.052	
10 MAM	Methyl Acrylate	0.11	5,50	1.08	2 595	1 26.7	u.092	0.032	1

Pipe run #1	
Description:	8" Piping
Pipe ID:	7.98 (in)
Equivalent Length of	
Pipe (from Table 4a):	493.9 (feet)

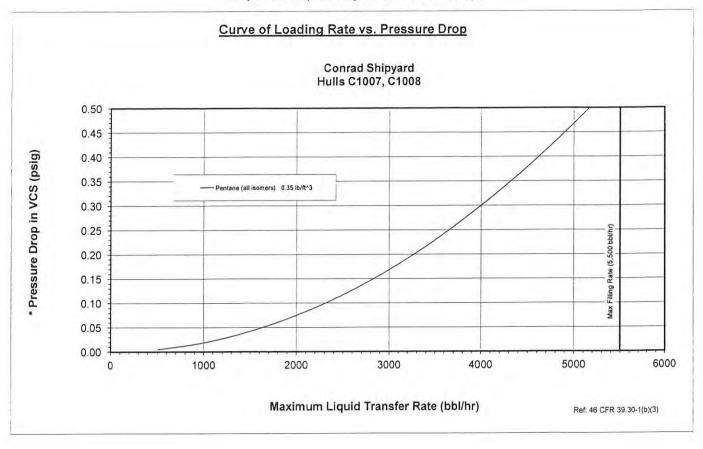
					friction factor:	0.014	0.052	0.052	55
11 MBE	Methyl Tert-Butyl Ether (MTBE)	0.077	5,500	1.001	5504 5607	24.72 25.17	0.062	0.062	60
12 MBK	Methyl Butyl Ketone	0.088	5,500	1.019	5639	25.32	0.065	0.065	6
13 MBU	Methyl Butyrate	0.091	5,500	1.025	5995	26.92	0.088	0.088	7
14 MEK	Methyl Ethyl Ketone	0.108	5,500	1.001	5507	24.73	0.053	0.053	5
15 MHK	Methyl Heptyl Ketone	0.077	5,500		5627	25.26	0.064	0.064	6
16 MIK	Methyl Isobutyl Ketone	0.089	5,500	1.023	5722	25.69	0.074	0.074	6
17 MMM	Methyl methacrylate	0.099	5,500			24.70	0.052	0.052	- 5
18 MNA	Methyl Naphthalene	0.076	5,500	1.000	5501 5522	24.79	0.055	0.055	5
19 MNS	Mineral Spirits	0.079	5,500	1.004	5588	25.09	0.059	0.059	- 5
20 MPL	Morpholine	0.084	5,500	1.016	5519	24.78	0.054	0.054	5
21 MRE	Myrcene	0.079	5,500	1.003		24.79	0.054	0.054	5
22 PTN	Naphtha: Petroleum	0.078	5,500	1.004	5521 5522	24.79	0.054	0.054	5
23 NSV	Naphtha: Solvent	0.078	5,500	1.004		24.79	0.055	0.055	
24 NSS	Naphtha: Stoddard Solvent	0.079	5,500	1.004	5522 5521	24.79	0.054	0.054	
25 NVM	Naphtha: VM&P	0.079	5,500	1.004			0.056	0.056	
26 NAX	Nonane (all isomers)	0.080	5,500	1.005	5530	24.83	0.057	0.057	
27 NON	Nonene (all isomers)	0.082	5,500	1.007	5539	24.87	0.054	0.054	
28 NNS	Nonyl Alcohol (all isomers)	0.078	5,500	1.002	5511	24.74			
29 NNP	Nonyl Phenol	0.076	5,500	1.000	5501	24.70	0.052	0.052	
30 NPM	1-, 2-Nitropropane	0.086	5,500	1.021	5616	25.21	0.062	0.062	
31 OAX	Octane (all isomers)	0.087	5,500	1.016	5587	25.09	0.061	0.061	
32 OCX	Octanol (all isomers)	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Octene (all isomers)	880.0	5,500	1.018	5599	25.14	0.063	0.063	
34 OTW	Oil, fuel: No. 2	0.095	5,500	1.011	5562	24.97	0.066	0.066	
35 OTD	Oil, fuel: No. 2-D	0.084	5,500	1.014	5576	25.04	0.059	0.059	
36 OFR	Oil, fuel: No. 4	0.078	5,500	1.003	5517	24.77	0.054	0.054	
37 OFV	Oil, fuel: No. 5	0.078	5,500	1.003	5517	24.77	0.054	0.054	
38 OSX	Oil, fuel: No. 6	0.078	5,500	1.003	5517	24.77	0.054	0.054	
39 OIL	Oil, misc: Crude	0.078	5,500	1.250	6875	30.87	0.083	0.083	
40 ODS	Oil, Misc; Diesel	0.084	5,500	1.014	5576	25.04	0.059	0.059	
41 OLB	Oil, Misc: Lubricating	0.076	5,500	1.003	5517	24.77	0.052	0.052	
42 ORL	Oil, Misc: Residual	0.076	5,500	1.003	5517	24.77	0.052	0.052	
43 OTB	Oil, Misc: Turbine	0.082	5,500	1.006	5533	24.84	0.057	0.057	
44 PTY	Pentane (all isomers)	0.350	5,500	1.540	8470	38.03	0.567	0.567	1
45 PTE	Pentene (all isomers)	0.310	5,500	1.499	8245	37.02	0.477	0.477	
46 PIN	Pinene	0.083	5,500	1.008	5542	24.88	0.057	0.057	
47 PLB	Polybutene	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Polypropylene Glycol	0.076	5,500	1.002	5511	24.74	0.052	0.052	
	Propyl Acetate (iso-)	0.097	5,500	1.036	5698	25.58	0.072	0.072	
	Propyl Acetate (n-)	0.098	5,500	1.037	5704	25.61	0.072	0.072	
	Propyl Alcohol (iso-)	0.091	5,500	1.060	5830	26.18	0.070	0.070	
	Propyl Alcohol (n-)	0.082	5,500	1.024	5632	25.29	0.059	0.059	
	Propylbenzene (all isomers)	0.079	5,500	1.004	5522	24.79	0.055	0.055	
54 IPX	iso-Propylcyclohexane	0.076	5,500	1.000	5501	24.70	0.052	0.052	
55 PPG	Propylene Glycol	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Propylene Glycol Methyl Ether Acetate	0.083	5,500	1.014	5577	25.04	0.058	0.058	_
	Propylene Tetramer	0.076	5,500	1.000	5502	24.71	0.052	0.052	_
	Suifolane	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Styrene	0.081	5,500	1.008	5544	24.89	0.056	0.056	
	Tetraethylene Glycol	0.076	5,500	1.000	5501	24.70	0.052	0.052	
61 THN	Tetrahydronaphthalene	0.077	5,500	1.001	5504	24.72	0.053	0.053	
62 TOL	Toluene	0.091	5,500	1.030	5665	25.44	0.066	0.066	
63 TCN	1,2,3-Trichloropropane	0.079	5,500	1.003	5517	24.77	0.055	0.055	
54 TCP	Tricresyl Phosphate (less than 1% of ortho isomer)	0.077	5,500	1,000	5501	24.70	0.052	0.052	
	Triethylbenzene	0.077	5,500	1.000	5502	24.71	0.052	0.052	
	Triethylamine	0.105	5,500	1.050	5775	25.93	0.079	0.079	
67 TEG	Triethylene Glycol	0.076	5,500	1.000	5501	24.70	0.052	0.052	
	Triethyl Phosphate	0.077	5,500	1.001	5503	24.71	0.053	0.053	
69 TRE	Trimethylbenzene (all isomers)	0.078	5,500	1.003	5515	24.76	0.054	0.054	
70 TRP	Trixylenyl Phosphate	0.076	5,500	1.000	5500	24.70	0.052	0.052	
71 THF	Tetrahydrofuran	0.090	5,500	1,170	6435	28.89	0.084	0.084	
	Undecene	0.077	5,500	1.001	5506	24.72	0.053	0.053	
	Undecene Undecyl Alcohol	0.076	5,500	1.000	5501	24.70	0.052	0.052	
72 ILIAID		0.070						0 2.11	
73 UND 74 VAM	Vinyl Acetate	0.130	5,500	1.116	6138	27.56	0.111	0.111	

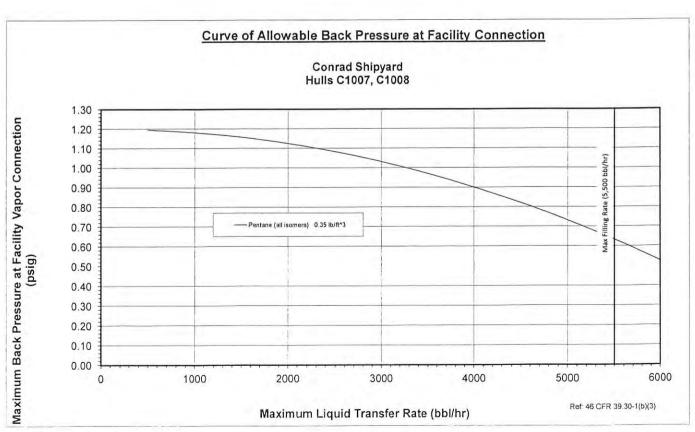
Compare pressure drop to P-V valve pressure settings:
 High-velocity P-V Valve pressure setting:
 Cargo tank P-V Valve pressure setting:
 30% of lowest P-V Valve Pressure Setting:
 Highest Pressure Drop from Tank to Facility Connection:
 Max Allowable Back Pressure at Facility Connection:

1.50 (psig) 1.50 (psig) 1.20 (psig) 0.57 (psig) 0.63 (psig)

Pentane (all isomers)

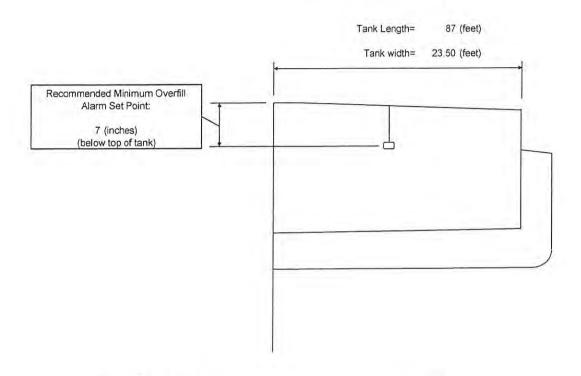
Conclusion:
For the cargo with the highest pressure drop (Pentane), the pressure drop is 0.57 psig. This, when added to the back pressure at the facility vapor connection must not exceed 80% of the pressure setting of any P-V valve in the cargo tank venting system. Therefore, the maximum allowable back pressure at the shore facility must not exceed 0.63 psig when loading with Pentane at the maximum liquid transfer rate (5,500 bbl/hr).





CONRAD SHIPYARD C1007, C1008

Calculation of Overfill Alarm Set Point (Cargo Tank No. 1 P/S)

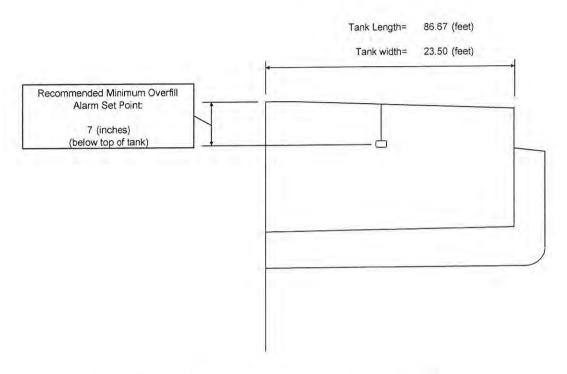


Maximum (per tank) Cargo	=	5,500 (bbl/hr)	
Loading Rate	=	91.67 (bbl/min)	
Minimum allowable time from			
alarm to overflow		60 (sec)	
Required volume above overfill			
alarm set point	=	91.7 (bbl)	
Capacity to deck at CL (17'-8" ABL) =		5315 BBL	
Capacity to 7" below dk at CL (17'-1" ABL) =		5203 BBL	
Volume above alarm =	1	112.2 BBL	RESULT OK
**Recommended set point of	=	7 (inches)	[Appx. 98% full tank]

**Note: Or 98.5%, whichever is lower (to d	comply with 33CFR155.775)
Capacity at 98.5% =	5235 BBL
Dist from TT at CL =	0.49 ft.

CONRAD SHIPYARD C1007, C1008

Calculation of Overfill Alarm Set Point (Cargo Tank No. 2 P/S)

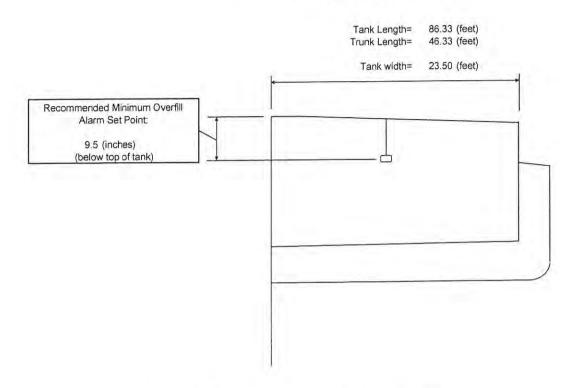


Maximum (per tank) Cargo	2	5,500 (bbl/hr)	
Loading Rate	=	91.67 (bbl/min)	
Minimum allowable time from			
alarm to overflow	(2)	60 (sec)	
Required volume above overfill			
alarm set point	=	91.7 (bbl)	
Capacity to deck at CL (17'-8" ABL) =		5295 BBL	
Capacity to 7" below dk at CL (17'-1" ABL) =		5183 BBL	
Volume above alarm =		111.8 BBL	RESULT OK
**Recommended set point of	=	7 (inches)	[Appx. 98% full tank]
	Loading Rate Minimum allowable time from alarm to overflow Required volume above overfill alarm set point Capacity to deck at CL (17'-8" ABL) = Capacity to 7" below dk at CL (17'-1" ABL) = Volume above alarm =	Loading Rate = Minimum allowable time from alarm to overflow = Required volume above overfill alarm set point = Capacity to deck at CL (17'-8" ABL) = Capacity to 7" below dk at CL (17'-1" ABL) = Volume above alarm =	Loading Rate = 91.67 (bbl/min) Minimum allowable time from alarm to overflow = 60 (sec) Required volume above overfill alarm set point = 91.7 (bbl) Capacity to deck at CL (17'-8" ABL) = 5295 BBL 5183 BBL Volume above alarm = 111.8 BBL

**Note: Or 98.5%, whichever is lower (to c	comply with 33CFR155.775)
Capacity at 98.5% =	5215 BBL
Dist from TT at CL =	0.49 ft.

CONRAD SHIPYARD C1007, C1008

Calculation of Overfill Alarm Set Point (Cargo Tank No. 3 P/S)



Maximum (per tank) Cargo	=	5,500 (bbl/hr)	
Loading Rate	=	91.67 (bbl/min)	
Minimum allowable time from			
alarm to overflow	=	60 (sec)	
Required volume above overfill			
alarm set point	=	91.7 (bbl)	
Capacity to deck at CL (17'-8" ABL) =		4427 BBL	
Capacity to 9.5" below dk at CL (16'-10.5" ABL) =		4328 BBL	
Volume above alarm =		99.5 BBL	RESULT OK
**Recommended set point of	=	9.5 (inches)	[Appx. 98% full tank]

**Note: Or 98.5%, whichever is lower (to comply with 33CFR155.775)

Capacity at 98.5% = 4361 BBL

Dist from TT at CL = 0.62 ft.

Vapor Recovery Calculations

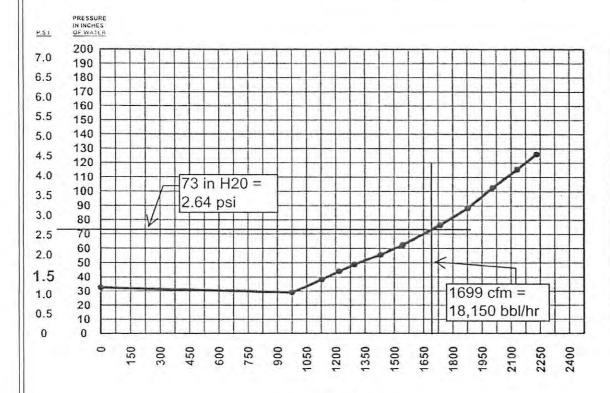
REFERENCES

- 1. 46 CFR 32.55-25, Venting of cargo tanks of tank barges constructed on or after July 1, 1951 -
- 2. 46 CFR 39.20-11, Vapor overpressure and vacuum protection TB/ALL
- 3. 46 CFR 39.30-1, Operational Requirements TB/ALL
- 4. Flow of Fluids Through Valves, Fittings, and Pipe; Crane Technical Paper No. 410
- USCG Guidelines for Determining the Maximum Liquid Transfer Rate for a Tank Vessel Transferring a Flammable or Combustible Cargo Using a Vapor Control System
- 6. Conrad Dwg. P3 Vapor Control Piping
- 7. USCG CHRIS (Chemical Hazards Response Information System) Manual.
- 8. 46 CFR 39.20-9, Tank Barge Liquid Overfill Protection B/ALL
- 9. Cameron Hydraulic Data, 15th edition

LIST OF ATTACHMENTS

- 1. Flow Capacity Curves for High-Velocity P-V Valve
- 2. Vacuum flow diagram for High-Velocity P-V Valve
- 3. USCG Approval Certificate for High-Velocity P-V Valve

CONRAD C1007, C1008

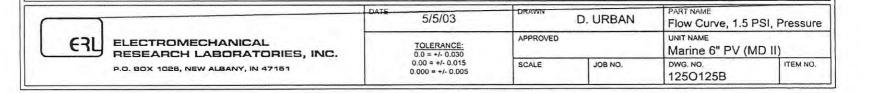


BARRELS	FLOW	PRESSURE
PER	FT.'/	IN. OF
HOUR	MIN.	Hz0

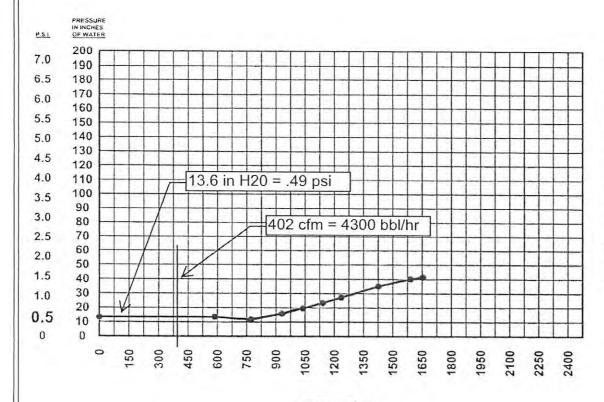
10418	974	29.2
12054	1127	38.6
13017	1217	44.2
13862	1296	49.0
15295	1430	55.8
16493	1542	62.6
18547	1734	76.6
20066	1876	88.5
21435	2004	102,8
22783	2130	115.8
23852	2230	126.3

Curve for Pressure Side 6" PV Valve - 1.5 PSI data based on air flow

FLOW IN FT.3/MIN.



CONRAD C1007, C1008

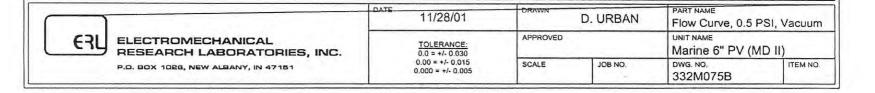


BARRELS	FLOW	PRESSURE
PER	FT.'/	IN. OF
HOUR	MIN.	H ₂ 0

6260	585	13.6
8256	772	11.8
9958	931	16.0
11100	1038	19.9
12197	1141	23.7
13207	1235	27.5
15252	1426	35.5
17003	1590	40.4
17674	1653	41.7

Curve for Vacuum Side
6" PV Valve - 0.5 PSI
data based on air flow

FLOW IN FT.3/MIN.





U. S. Department of Homeland Security United States Coast Guard Certificate of Approval

Coast Guard Approval Number: 162.017/167/4

Expires: 05 April 2016

PRESSURE-VACUUM RELIEF VALVES FOR TANK VESSELS

ELECTROMECHANICAL RESEARCH LABORATORIES INC. 2560 Charlestown Road NEW ALBANY IN 471510

ERL SUPERAC Model II, 6-inch High Velocity Pressure/Vacuum Relief Valve.

High-velocity weight-loaded pressure/vacuum relief valve, constructed of 300 series stainless steel.

Identifying Data: ERL Drawing No. 050M147B dated June 6, 2001. Flow data located in CEESI Test Reports dated December 12, 2001 (initial testing), November 8, 2004 (5.5 psi pressure setting), December 13, 2005 (10.0 psi pressure setting), and January 30, 2006 (3.0 psi vacuum setting), February 14, 2011 (5.0 psi vacuum setting).

Approved for relief settings of: 1.0 - 10.0 psig pressure, and 0.5 - 5.0 psig vacuum.

ERL SUPERAC (TM) Model II 6" P/V Valve has been tested in accordance with API 2000, and is approved for use in vapor control systems.

This certificate supersedes approval no. 162.017/0167/3 dated May 12, 2006, to expand range of vacuum settings up to 5.0 psi.

*** END ***

THIS IS TO CERTIFY THAT the above named manufacturer has submitted to the undersigned satisfactory evidence that the item specified herein complies with the applicable laws and regulations as outlined on the reverse side of this Certificate, and approval is hereby given. This approval shall be in effect until the expiration date hereon unless sooner canceled or suspended by proper authority.



GIVEN UNDER MY HAND THIS 5th DAY OF APRIL 2011, AT WASHINGTON D.C.

C. R. O'NEIL

Assistant Chief, Tank Vessel and Offshore Division

U.S. Coast Guard Marine Safety Center



Marine Safety Center Vapor Control System (VCS) Plan Review Information Sheet (PRIS)



Vessel Name	CBC 374, 375, 380, 384, 386	Shipyard	Conrad and Orange
Official Number	various	Hull Number	C-1007, C-1008, H-451 through H-453
Control Systems. CG In: 6 8 prior to updating the	es critical VCS parameters for MSC Sta spectors should verify the vessel's VCS vapor control endorsement on the vess reflect the vessel's design the CG Inspe	design is consistent well's Certificate of Inspe	ith the information listed in boxes 2, 6, 7 ction. For cases where the information
. Tank Maximum Des	ign Working Pressure	3.00 psig	Raised Trunk X Flush Deck
. Authorized Maximur	m Cargo Transfer Rate(s)	5,500 bbl/hr load 4,300 bbl/hr disc	ling (max 2 tanks simultaneously) charging
. Authorized Maximu	n Vapor-Air Mixture Density	0.347 lbm/ft ³	
i. Authorized VCS Cat	egories 1	through 7	
a. C	hest vapor density and/or pressure of argo Name ISO-PEN	ITANE	
CG Approval Required Venti	ERL Settings in JPERAC II PV-6 Pressure	-side 1.5 Lo -side 0.5 Tr	8. VCS Pipe Sizes: Approx. Inside Diameter Ingitudinal Header (inches) ansverse Header (Inches) bbl/hr (air) bbl/hr (air)
	tion System (check appropriate box or verfill Alarm	boxes) ran Gaurd 07324TWIN-2A OCMI to Verify N/A N/A	Setting in psi Meets ASTM F1271 N/A
1. Instructions/Guideli 11a. The following is the In accordance with 46 plans approved by Maracceptable for the colle Attachment's VCS columber the vessel is carensuring the provisions 11b. The MSC approv	ines for the OCMI: ne Marine Safety Center's recommende CFR Part 39, excluding part 39.40, this rine Safety Center letter Serial No. C1- ection of bulk liquid cargo vapors annota mn. rying cargoes containing greater than 0 s of 46 US Code of Federal Regulations al letter/s must be available at the OCM	d COI endorsement: vessel's vapor collectio 205189 dated January ated with "Yes" in the th .5% benzene, the perso Part 197, Subpart C an	n system has been inspected to the 4, 2013, and has been found e vessel's Cargo Authority