U.S. Department of Homeland Security

United States Coast Guard Commanding Officer United States Coast Guard Marine Safety Center 2100 2nd Street, S.W. Stop 7102 Washington, DC 20593-7102 Staff Symbol: MSC-3 Phone: (202) 475-3403 Fax: (202) 475-3920 Email:msc@uscg.mil

16710/P018276 Serial: C1-1302141 June 28, 2013

Conrad Industries, Inc. Attn: Mr. Richard L. Soudelier PO Box 790 Morgan City, LA 70381 Email: rlsoudelier@conradindustries.com

Subj: New Construction, CG1239547, Conrad Shipyard Hull Number C-1039 New Construction, CG1239548, Conrad Shipyard Hull Number C-1043 297'-6" x 54' x 12' Unmanned Double Hull Type II/III Tank Barges (D/O) Grade A (max. 25 psia Reid) and Lower Grades Flammable or Combustible Liquids Identified in 46 CFR Table 30.25-1 or 46 CFR 153 Table 2 as Pollution Category I or III and Specified Hazardous Cargoes Design Density 8.7 lbs/gal; Maximum Density (slack load) 15 lbs/gal Rivers; Lakes, Bays, and Sounds; Limited Coastwise on unmanned fair weather voyages only, not more than 12 miles offshore between St. Marks and Carrabelle, Florida Plan Approval Extension, Vapor Collection System, and List of Authorized Cargoes

Dear Mr. Soudelier:

We have reviewed the information submitted with your email dated May 31, 2013, (MSC Document No. 1313789) wherein you have requested that plans previously approved under project P014938, Conrad Shipyard Hulls C-994 through C-997, be used for the construction of the subject vessels. While we have no objection to you using the plans that were previously approved plans, please be advised that the cognizant Officer in Charge, Marine Inspection (OCMI) has the final authority for these issues.

Enclosure (1) includes details regarding MSC approval letters for previously approved plans you wish to use for the construction of the subject vessels. By copy of this letter, we recommend the OCMI extend approval of all drawings and calculations addressed in enclosure (1) to the subject vessels. This extension of plan approval is based on our understanding that:

- a. The subject vessel will be built to the same plans as those specified in enclosure (1),
- b. The regulations used for the original plan approval have not changed since the original plan approval,
- c. The owner of the original plans specifically authorizes the use of the plans for new construction,
- d. There are no modifications to subject vessel or any of the installed systems which would require additional review, and
- e. All comments provided in the original approval letters, accompanying the approved plans, still apply.

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# Subj: New Construction, CG1239547, Conrad Shipyard Hull Number C-1039 New Construction, CG1239548, Conrad Shipyard Hull Number C-1043 Plan Approval Extension, Vapor Collection System, and List of Authorized Cargoes

You must provide the OCMI a copy of each item listed in enclosure (1) with its corresponding MSC approval letter. Plans that do not conform to any part of (a) through (e) above shall be submitted to our office for approval. The installation, workmanship, and testing shall be to the satisfaction of the OCMI. Any vessel system, arrangement, structure, or other item that requires plan approval but is not covered by an extension must be either submitted to the MSC for review or reviewed by the OCMI.

The Vapor Control System (VCS) PRIS for the subject vessels is included as enclosure (2). In addition, we have updated each vessel's cargo and vapor control authority. The 46 CFR 151 Cargo List and VCS List of Cargoes are included as enclosures (3) and (4).

At the time of this review, the vessels' official numbers were not available. Once you provide the vessel names and official numbers to this office, the updated Cargo Authority Attachments (CAAs), containing the cargoes found in enclosure (3) and vapor control authority for the cargoes found in enclosure (4), will be made available for issuance by the OCMI.

Please note that only the local OCMI can issue a vessel's CAA as part of the Certificate of Inspection (COI). The OCMI will verify the carriage authority and vapor control tank group characteristics we used as a basis for creating enclosures (3) and (4) are consistent with the vessel's actual design. For the OCMI's convenience, we have included the following recommended COI endorsement:

Only those hazardous cargoes named in the vessel's Cargo Authority Attachment, Serial No. C1-1302141 dated June 20, 2013, may be carried and then only in the tanks indicated.

When the vessel is carrying cargoes containing greater than 0.5% benzene, the person in charge is responsible for ensuring the provisions of 46 US Code of Federal Regulations Part 197, Subpart C are applied.

In accordance with 46 CFR Part 39, excluding part 39.40, this vessel's vapor control system has been inspected to the plans approved by Marine Safety Center letters Serial No. C1-1204161 dated September 25, 2012 and extended by C1-1302141 dated June 20, 2013, and found acceptable for collection of bulk liquid cargo vapors annotated with "Yes" in the CAA's VCS column.

Our Project Number for these vessels is <u>P018276</u>. Please ensure that future correspondence includes the Project Number, and either the Coast Guard (CG) number that appears in the subject line or the Official Number of each barge once assigned. To avoid confusion, the owners are

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 Plan Approval Extension, Vapor Collection System, and List of Authorized Cargoes

encouraged to provide the National Vessel Documentation Center with the vessel CG numbers when applying for documentation.

If you have any questions concerning our review, please contact Lieutenant Ryan Mowbray at the number listed above.

Sincerely,

M. J. SEXTON Lieutenant, U. S. Coast Guard Assistant Chief, Tank Vessel and Offshore Division By direction

- Encl: (1) Plan Approval Extension Form
  - (2) VCS PRIS, Conrad Shipyard Hulls C-1039 and C-1043, dated June 20, 2013
  - (3) 46 CFR Part 151 Cargo List, Conrad Shipyard Hulls C-1039 and C-1043, dated June 20, 2013
  - (4) VCS List of Cargoes, Conrad Shipyard Hulls C-1039 and C-1043, dated June 20, 2013

Copy: Commander, Coast Guard Sector Morgan City

U.S. Department of Homeland Security

United States Coast Guard Ő,

Commanding Officer United States Coast Guard Marine Safety Center 2100 2<sup>nd</sup> Street, S.W. Stop 7102 Washington, DC 20593-7102 Staff Symbol: MSC-3 Phone: (202) 475-3403 Fax: (202) 475-3920 Email: msc@uscg.mil

16710/P014938 Serial: C1-1204161 September 25, 2012

Conrad Industries, Inc. Attn: Mr. Richard L. Soudelier PO Box 790 Morgan City, LA 70381 Email: rlsoudelier@conradindustries.com

Subj: JARED JOSEPH, O.N. 1242310, Conrad Shipyard Hull No. C-994 NICHOLAS RAY, O.N. 1213431, Conrad Shipyard Hull No. C-995 ALLISON JANE, O.N. 1213432, Conrad Shipyard Hull No. C-996 MACI BRYAN, O.N. 1242740, Conrad Shipyard Hull No. C-997 297'-6" x 54' x 12' Unmanned Double Hull Type II/III Tank Barges (D/O) Grade A (max. 25 psia Reid) and Lower Grades Flammable or Combustible Liquids Identified in 46 CFR Table 30.25-1 or 46 CFR 153 Table 2 as Pollution Category I or III and Specified Hazardous Cargoes Design Density 8.7 lbs/gal; Maximum Density (slack load) 15 lbs/gal Rivers; Lakes, Bays, and Sounds; Limited Coastwise on unmanned fair weather voyages only, not more than 12 miles offshore between St. Marks and Carrabelle, Florida Vapor Collection System and List of Authorized Cargoes

- Ref: (a) Document No. 1216407, Conrad Shipyard, "Vapor Control Piping," Dwg. No. P-03, Sheets 1 and 2, Rev. 2, dated May 3, 2012
  - (b) Document No. 1216410, Guarino & Cox, LLC, "Vapor Control System Calculations," Dwg. No. C-32, Rev. 1, dated September 25, 2012
  - (c) Coast Guard Marine Safety Center's "Industry Guidelines for Determining the Maximum Liquid Transfer Rate for a Tank Vessel Transferring a Flammable or Combustible Cargo Using a Vapor Control System" dated July 15, 2001

Dear Mr. Richard L. Soudelier:

In response to your electronic submissions dated September 14, 2012, September 24 2012, and September 25, 2012 we have reviewed the vapor collection system (VCS) piping plan and the vapor control pressure drop calculations for compliance with 46 CFR Part 39, excluding Subpart 39.40. The VCS piping plan, reference (a), is marked "**Approved**." The installation, workmanship and testing shall be to the satisfaction of the cognizant Officer in Charge, Marine Inspection (OCMI). The pressure drop calculations, reference (b) are "**Examined**." Calculations and plans such as these are not normally marked approved, but are used to verify that the system meets the applicable regulations. The following comments apply:

16710/P014938 Serial: C1-1204161 September 25, 2012

Subj: Conrad Shipyard Hull C-994 through C-997; Vapor Collection System and List of Authorized Cargoes

1. Based on your calculations, this VCS is capable of recovering vapors of the cargoes listed in enclosure (1) at a maximum vapor-air mixture density of  $0.35 \text{ lbm/ft}^3$ , at a maximum liquid load rate of 5,500 bbl/hr, and at a maximum liquid discharge rate of 4,300 bbl/hr.

2. In accordance with reference (b), the set-point of the overfill shutdown system shall be no higher than **7 inches** below the tank top of cargo tank 1 P/S and 2 P/S, and set no higher than **9.5 inches** below the tank top of cargo tank 3 P/S.

3. The oil transfer procedures shall include a table or graph showing the liquid transfer rate versus the pressure drop, as required by 46 CFR 39.30-1(b)(3), to the satisfaction of the cognizant OCMI. This information must be taken from the calculations, tables, and graphs contained within reference (b). However, the table or graph added to the oil transfer procedures should exclude unauthorized cargoes, and shall not reflect transfer rates exceeding the maximum liquid load rate approved in paragraph 1.

4. The tanks share a common vent header, which would allow mixing of various vapors and liquid cargoes. Note this configuration restricts the types of cargoes that can be carried simultaneously.

5. Enclosure (3) contains VCS Category 2 and 4. Polymerization and residue build-up of these cargoes can adversely affect the operation of the vapor collection system. The barge's owner must develop a method for internal visual inspection to verify that fouling of VCS components is not occurring, to the satisfaction of the cognizant OCMI.

6. In conjunction with this review, we have generated the subject vessel's cargo authority based on the Tank Group Characteristics Loading Form submitted with your email dated September 14, 2012. The 46 CFR 151 Cargo List is attached as enclosure (2).

7. The Cargo Authority Attachment (CAA) for each vessel is now available in the Coast Guard's Marine Information for Safety and Law Enforcement (MISLE). The CAA will contain the cargoes found in enclosures (1) and (2). Please note that only the cognizant OCMI can issue a vessel's CAA, which is valid only when referenced by and attached to a valid Certificate of Inspection (COI). The OCMI will verify the carriage authority and vapor control tank group characteristics we used to create enclosures (1) and (2) are consistent with the vessel's actual construction. Enclosure (3) contains the VCS tank group characteristics and our recommended COI endorsement.

As a condition of your participation in MSC's electronic commerce program, you must provide a copy of the approved drawings to the OCMI, along with a copy of the corresponding MSC approval letter.

Our Project Number for this vessel is **P014938**. Please ensure that future correspondence includes the Project Number and Official Number that appears in the subject line for each barge.

16710/P014938 Serial: C1-1204161 September 25, 2012

Subj: Conrad Shipyard Hull C-994 through C-997; Vapor Collection System and List of Authorized Cargoes

If you have any questions concerning our review, please contact Lieutenant Rachel Beckmann at the number listed above.

Sincerely,

J. B. Wheeler Lieutenant, U. S. Coast Guard Assistant Chief, Tank Vessel and Offshore Division By direction

- Encl: (1) Vapor Collection System List of Cargoes; Conrad Shipyard Hull Nos. C-994 through C-997; dated September 25, 2012
  - (2) 46 CFR Part 151 Cargo List, Conrad Shipyard Hull Nos. C-994 through C-997; dated September 25, 2012
  - (3) VCS PRIS; Conrad Shipyard Hull Nos. C-994 through C-997; dated September 25, 2012

Copy: Commander, Coast Guard Sector Morgan City, w/ enclosures

		REVISION	S		
REV	DES	SCRIPTION		DATE	BY
1	A. Changed HVPV valve from ERL to T	anktech per ov	ner request.	9-25-12	RA
	B. Modified calculations to suit.				
	C. Added hull C 794 THRU C-99	7			
				1 1	
	GUA	RINO & CO	DX, LLC		
		9 Helenbirg Rd.			
	XX	Covington, La. 7			
		(985) 871-99	97		
			ITS CONTENTS, IN ANY FASHION		
			N WITHOUT THE PREVIOUS WRITT 'IS STRICTLY PROHIBITED,	EN	
	Con	rad Industi	ries, Inc		
	297'-6" x 54'	x 12' INLAN	D TANK BARGE		· · · · · · ·
	VAPOR CONTR	IOL SYSTE	M CALCULATIONS		
SCALE	: NONE	DATE:	9-25-12	DWG	. NO
DRAW		CK'D BY:	R. ALLUMS	<u> </u>	52
HULL	NO. C-994 THRU C-997	JOB NO,	10-002	REV.	1

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## VAPOR CONTROL SYSTEM CALCULATIONS - SUMMARY

# A. General Description of Vessel:

۱.

Builder:	CONRAD INDUSTRIES, INC	
Builder's hull numbers:	Conrad C-994 THRU C-997	
Year Built:	2012/2013	
Official Numbers:		
Owner:		
Vessel Names:		
Vessel Dimensions:	297'-6" x 54'-0" x 12'-0"	
Service:	Inland Tank Barge (D/O)	
Classification:	None	
Max Design Working Pressure of Tanks:	3.00	(psig)
Max Cargo Loading Rate	5,500	(bbl/hr)
Maximum Discharge Rate	4,300	(bbl/hr)
VCS Cargoes:	See Table 1	
Maximum Vapor-Air Mixture Density:	0.35 (Pentane, all isomers)	(lbm/ft^3)
Maximum Vapor Growth Rate:	1.54 (Pentane, all isomers)	(lbm/ft^3)

## B. General Description of Vapor Control System:

[Note: Also see Reference 6 for details of vapor control system.]

### 1. Pipe:

One (1) 8" diam longitudinal vapor header fitted with a 6" high-velocity PV Valve. One (1) 8" diam tranverse vapor header with 8" shore connection valves. One (1) 8" diam branch line off longitudinal header to each cargo tank. (See Reference 6 for system layout)

2. High Velocity PV Valve:		
Model:	Tanktech/Bergan KLPH-6	
Pressure Setting:	1,50	(psig)
Vacuum Setting:	0.5	(psig)
PV Valve Flow Capacity:	See Att. 1	(bbl/hr)
3. Spill Valve:		
Model:	None installed	
Pressure Setting:	N/A	
4. Vapor Recovery Hose:		
Diameter:	8" (assumed)	
Length:	50' (assumed)	
5. Cargo Tank P-V Valves:	(One central P/V valve only, no individual tank P-V valves)	
Model:	See #2 above.	
Pressure Setting:	1,50	(psig)
Vacuum Setting:	0.5	(psig)

#### C. VCS Calculations:

### 1. Cargo Authority:

The vapor collection system installed on this barge is designed for Grade A and lower petroleum products and chemicals. Typical cargoes to be carried by this barge are listed in Table 1. These cargoes are to be listed in the Cargo Authority Attachment (CAA) of the barge's Certificate of Inspection. Note that Table 1 is not intended to be an all-inclusive list and the CAA should therefore not be limited to these cargoes. Other cargoes with less restrictive or equal characteristics shall also be included on the CAA.

#### 2. Determining Vapor-Air Mixture Density and Vapor Growth Rate:

Of the cargoes carried, Pentane has the highest vapor-air mixture density. Pentane also has the greatest vapor growth rate. (See Table 1)

# 3. The Maximum Liquid Transfer Rate as Imposed by the Capacity of the Cargo Tank Venting System: (Ref: 46 CFR 39.20-11)

Tanks #1 P/S are the farthest tanks from the High-Velocity P-V Valve in terms of total equivalent pipe length. Using factors from Reference 4 and 9, the total equivalent length of pipe is calculated for this path. This calculation is shown in Table 2.

Using Darcy's equation, and friction factors selected as appropriate for the pipe size, and the maximum liquid transfer rate, the pressure drop along the VCS piping from tank #1P to the P-V Valve is calculated using the total equivalent length of pipe from Table 2. The pressure drop calculations were done for the maximum loading rate (5,500 BBL/hr) for this barge. This maximum loading rate is based on loading one tank at a time. This calculation is shown in Table 3.

#### Conclusions:

Using a 5,500 bbl/hr maximum liquid transfer rate (for Pentane and lower cargos), the vapor-air mixture and air-equivalent volumetric flow rates for each cargo are shown in Table 3. The greatest pressure drop in the cargo tank venting system is 0.24 psig for Pentane cargo. At a pressure relief setting of 1.5 psig, the high-velocity P-V valve has an adequate flow capacity (see attachment 1). The greatest total back pressure imposed on the tanks by the cargo tank venting system (1.03 psig) does not exceeed the design working pressure of the cargo tanks (3.00 psig). Also, the vacuum relieving capacity of the P-V Valve has been checked against the maximum discharge rate and has been found to have adequate vacuum relieving capacity (see Table 3).

4. The Maximum Liquid Transfer Rate as Imposed by the Relieving Capacity of the Cargo Tank Spill Valves:

No spill valves are installed on this barge.

#### 5. The Maximum Liquid Transfer Rate as Imposed by the Set Point of the Overfill Alarm:

At the maximum cargo loading rate of 5,500 bbl/hr, required overfill alarm set points have been calculated such that the person in charge of the transfer operations has more than 60 seconds from the overfill alarm to stop the transfer operations before the tank overflows. (See attached overfill alarm set point calculation sheets.) The overfill alarms will need to be set at or below these calculated levels to ensure that the VCS complies with 46 CFR 39.20-9. In addition, the overfill alarms must also be set at or below a capacity of 98.5% to comply with 33CFR155.775.

6. The Maximum Liquid Transfer Rate as imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 46 CFR 39.30-1(d)(3):

This requires the sum of the pressure drop along the longest path from the cargo tank to the vessel vapor connection and the back pressure at the facility vapor connection not to exceed 80 percent of the pressure setting of any pressure relief valve in the system. Tanks #1 P/S are the farthest from the facility vapor connection (in terms of total equivalent length of pipe). The total equivalent length from cargo tank #1P to the facility vapor connection is given in Table 4.

Using Darcy's equation, and friction factors selected as appropriate for the pipe size, and the maximum liquid transfer rate, the pressure drop along the VCS piping from tank #1P to the facility vapor connection is calculated using the total equivalent length of pipe from Table 4. These calculations are shown in Table 5.

#### Conclusions:

Pressure drop at the maximum liquid transfer rate of 5,500 bbl/hr (for Pentane and lower cargoes) along this path for each cargo is given in Table 5. The highest pressure drop (for Pentane) does not exceed 80 percent of the P-V valve pressure setting. If the pressure drop between the facility vapor connection and the shore facility's pressure sensor is known, it should be added to the pressure drop along this path to ensure that the total pressure drop does not exceed 80 percent of the P-V valve pressure setting.

7. Graph as Required by 46 CFR 39.30-1(b)(3): See attached.

#### Table 1 Determination of Vapor-Air Mixture Density & Vapor Growth Rate

	CHRIS Code	Name	VCS Category	Liquid S.G.	*Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (Ib/ft^3)	Vapor Growth Rate	Max. Loading Rate	Vapor Volumetric Flow Rate (bbl/hr)	Air Equivalent Votumetric Flow Rate (bbl/hr)	Pressure Drop to PV Valve in VCS (See Table 3) (psig)	Pressure Drop to Facility Connection in VCS (See Table 5) (psig)
1	ACN	Acrylonitrile	4	0,81	5.00	1.80		1.10	5,500				
		Acetone	1	0.79	10.00	2.00	0,123						
		Acetophenone	1	1.03	0,60	4.14	0.085		5,500				
		Adiponitrile	1	0,95	0.01	3,73	0,076	1.00	5,500	5501	5506	0.022	
		Amyl acetate (all isomers)	1	0.88	0,33	0,10			5,500	5536	5485	0.022	0.044
		Amyl Alcohol (iso-, n-, sec-, primary)	1	0.82	0,30	3.04	0.079		5,500				
		Acetonitrile	3		0.03	1.41	0.076						1
		Benzyl Alcohol Benzene	1		0.10	3,73 2,80	0.077					- <u> </u> -	
		Benzene, Toluene, Xylene mixtures (10%	1	0.00	4.50	2.00		1.20	0,000	0075	0420	0.052	0.103
10		Benzene or more)	1	0.84	7,30	2,80	0,138	1.25	5,500	6875	9252	0.063	0.124
		Butyl Acrylate (iso-, n-)	2		0,60		0.086		5,500				
		Butyl Acetate (all isomers)	1	0,87	0,60	4.00	0.085	1.01	5,500	5566	5867	0.025	0.050
	IAL	Butyl Alcohol (iso-)	1		0.90								
	BAN BAS	Butyl Alcohol (n-)	1		0,50								
	BAS	Butyl Alcohol (sec-) Butyl Alcohol (tert-)	1	0,81	1.30			1.03					
		Butyl Benzyl Phthalate	1										
		iso-Butyraldehyde	1				0.077	1.16				_	
19	BTR	n-Butyraldehyde	1			-		1.16					
		Butyl Toluene	1				0.078					0.023	3 0.045
		Caprolactam Solutions	1	1.02	0.05		0.077						
		Cyclohexanone	1		0.20								
	CHA CHX	Cyclohexylamine Cyclohexane	1		0,62		0,083	-	· · ·				
		Cyclohexanol	1	0.78					· · ·				
	CPD	1,3-Cyclopentadiene dimer (molten)	2										
	CMP	p-Cymene	1	0.86		4,62		1		-			
	CRB	Chlorobenzene	1	1.11	0.80	3,88			+ · · · · · · · · · · · · ·				
	CRS	Cresols	1		0.08								
	CUM	Cumene	1		0.60							-	
	IDA DAL	Decaldehyde (iso-) Decaldehyde (n-)	1	0.83	0.01	5.00			-l				
	DCE	Decene	1	0.83	0.00				· · ·				
	DAX	Decyl Aicohol (all isomers) (Decanol)	1	0.83		5.30							
	DBZ	Decylbenzene (n-)	1	0,86	0.01	7.52	0.076	5 1,00			5512		
	DAA	Diacetone Alcohol	1	0.97	0.10								
	DCH DPA	1,1-Dicholoroethane	1	1.18									
	DEB	Dibutyl Phthalate (ortho-) Diethybenzene	1	1.05									
	DEG	Diethylene Glycol	1			3.66							
41		Diethylamine	3										
	DBL	Diisobulylene	1		2.00	3.86	0,103	3 1.04	5,500	5720	6654		
	DIK	Diisobutyl Ketone	1					-					-
	DIP	Diisopropanolamme	1	· · · · · ·									
		Disopropylbenzene (all isomers) Dimethyl Phthalate	1										
	DOP	Dioclyl Phthalate									-		
48	DPN	Dipentene	1	0,84					5,500	D 551			
	DIL	Diphenyl	1						· ·		5500	3 0.02	2 0.044
	DDO	Diphenyl, Diphenyl Ether Mixtures	1										
	DMF DPE	Dimethylformamide Diphenyl Ether	1										
		Dipropylene Glycol	1										
	DPX	1,1-, 1,2-, 1,3-Dichloropropane	3										
	DFF	Distillates Flashed Feed Stocks	1										
56	DSR	Distillates Straight Run	1	0.73	2,30	3.40	0.102	2 1.05	5 5,500	575	3 666		
	DOZ	Dodecene (all isomers)	1										
	DDB	Dodecylbenzene	1										
	EAC	Ethyl Acrylate 2-Ethylhexyl acrylate	2									-	
		2-Ethymexyl acrylate 2-Ethoxyethyl acetate											
	2 ETG	Ethoxy Triglycol (crude)	1										
63	BETA	Ethyl Acetate	1										
64	I EAA	Ethyl Acetoacetate	1	1.03	0,20	4.48	0,079	9 1.00	5,500	552	2 563		
	5 EAL	Ethyl Alcohol (Ethanol)	1			_						5 0.02	9 0.057
	BETB	Ethyl Benzene	1						+				
	7 EBT B EBE	Ethyl Butanol Ethyl tert-butyl ether	1										

#### Vapor Recovery Calculations

	- 1	CHRIS Code	Name	VCS Category	Liquid S.G.	*Vapor Press. @ 115 F (psia)	Vapor S.G.	Vapor-air Mixture Weight Density (lb/ft^3)	Vapor Growth Rate	Max. Loading Rate	Vapor Volumetric Flow Rate (bbl/hr)	Air Equivalent Volumetric Flow Rate (bbl/hr)	Pressure Drop to PV Valve In VCS (See Table 3) (psig)	Pressure Drop to Facility Connection In VCS (See Table 5) (psig)
			Ethyl butyrate	1	0.88	1.00	4.00	0.090	1.02	5,500				0,054
			Ethyl Cyclohexane	1	0.79		3.87	0.083	1.01	5,500				0.049
			Ethylene dichloride	1			3.42	0.122						0.082
	72		Ethylene Glycol Ethylene Glycol Butyl Ether Acetate	1	1.19 0.94	0.01	2.21 5.52	0.076	1.00	· · ·		5503 5544		
			Ethylene Glycol Diacetate	1		0.03	5.02	0.077				5508		0.045
			Ethylene Glycol Phenyl Ether	1	1.10		4.80	0,076				5508		
	76		Ethyl-3-ethoxypropionate	1	0.95	0.01	5.00				5501	5510		0,044
			2-Ethylhexanol	1		0.02			-	· ·	5502			0.044
			Ethyl Propionate	1	0.89									
		FAM	Formamide	1										0.047
		FMS	Formaldehyde Solution	1										0.044
	82	FAL	Furfuryl Alcohol	1	1.13	0.05								0.044
		FFA	Furfural	1										
		GAK	Gasoline Blending Stocks: Alkylates	1										
		GRF GAT	Gasoline Blending Stocks: Reformates Gasolines: Automotive	1										
		GAV	Gasolines: Automotive	1										
	88	GCS	Gasolines: Casinghead	1	0.67									
	89	GPL	Gasolines: Polymer	1	0.75	12.50	3.40	0.217	1.25	5,500	6875	11610	0.099	0.196
ļ		GSR	Gasolines: StraightRun	1										
		GCR HMX	Glycerine Heptane (all isomers)	1	1									
		HEP	Heptonic Acid	1	0.88		1							
		HTX	Heptanol (all isomers)	1										
		HPX	Heptene (all isomers)	2						5,500	5819	6958	0.038	0.070
		HXS	Hexane (all isomers)	1									-	
		HXO	Hexaonic Acid	1										
	90	HXN HEX	Hexanol Hexene (all isomers)	2										
· ·		HXG	Hexylene Glycol	1										
	101	IPH	Isophorone	1						· · ·				
	102		Jet Fuels: JP-4	1										0.082
		JPV	Jet Fuels JP-5 (Kerosene, heavy)	1										
		KRS MTT	Kerosene Methyl Acetate	1										
		MAL	Methyl Alcohol (Methanol)	1						- <u> </u>				
		MAC	Methylamyl Acetate	1								6 5756		
		MAA	Methylamyl Alcohol	1	4101		-	-						
		MAK MAM	Methylamyl Keytone Methyl Acrylate	1										
		MBE	Methyl Tert-Butyl Ether (MTBE)	1										
		MBK	Methyl Butyl Ketone	1										
	113	MBU	Methyl Butyrate	1	0,90	1.26	3.53	3 0.091	l 1.0:	3 5,500	5639	616	8 0.028	3 0.055
		MEK	Methyl Ethyl Ketone	1										
		MHK MIK	Methyl Heptyl Ketone Methyl Isobutyl Ketone	1										
		MMM	Methyl methacrylate	2										
	118	MNA	Methyl Naphthalene	1	1.02	2 0.01	4.91	0.076	6 1.00	5,500	) 550 <sup>-</sup>	1 550	8 0.02	2 0,044
		MNS	Mineral Spirits	1										
		MPL MRE	Morpholine Marcene	1										
		MRE PTN	Myrcene Naphtha: Petroleum	1										
		NSV	Naphtha: Solvent	1										
	124	NSS	Naphtha: Stoddard Solvent	1	0.78	3 0.20	4,30	0,079	1.0	5,500	) 5522	2 563	3 0.02	B D.046
		NVM	Naphtha: VM&P	1										3 0.046
		NAX NON	Nonane (all isomers) Nonene (all isomers)	1		-								
		NNS	Nonene (all isomers)											
		NNP	Nonyl Phenol	1										
	130	NPM	1-, 2-Nitropropane	1	0,99	1.05	5 3,06	3 0.086	5 1.0	2 5,500	561	6 597	9 0.02	6 0.052
		OAX	Octane (all isomers)	11										
		OCX OTX	Octanol (all isomers) Octene (all isomers)	1										
		OTW	Oil, fuel: No. 2	1			-							
	135	OTD	Oil, fuel: No. 2-D	1										
		OFR	Oil, fuel: No. 4	1			5 3.40	0.078	3 1.0	0 5,500	551	7 557	7 0.02	3 0.045
		OFV	Oil, fuel: No. 5	1										
		OSX OIL	Oil, fuel: No. 6 Oil, misc: Crude	1		1								
		ODS	Oil, Misc: Diesel	1										
		OLB	Oil, Misc: Lubricating		0.90									

#### Vapor Recovery Calculations

	CHRIS Code	Name	VCS Category	Liquid S.G.	*Vapor Press. @ 115 F		Weight Density		Max. Loading Rate	Flow Rate	Air Equivalent Volumetric Flow Rate	in VCS (See Table 3)	Pressure Drop to Facility Connection in VCS (See Table 5)
4.45				1.00	(psla)		(lb/ft^3)	1.4.7		(bbl/hr)	(bbi/hr)	(psig)	(psig)
	ORL OTB	Oil, Misc: Residual Oil, Misc: Turbine	1	1.02	0.15	1.00	0.076		5,500		5517	0.022	
			1	0.87	0.30	5.40	0.082	1.01	5,500		5754	0.024	0.04
	PTY	Pentane (all isomers)	5			2.50	0.350	1.54	5,500				0.47
	PTE	Pentene (all isomers)	5			2.40	0.310	1.50		8245			0.40
146		Pinene	1	0,00		4.70	0.083	1.01	5,500	5542		0.024	0.04
	PLB	Polybutene	1		0.01	1.00	0.076	1.00			55 <u>01</u>		0.04
	PGC	Polypropylene Glycol	1	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	0,10	1.00	0.076	1.00					0.04
149		Propyl Acetate (iso-)	1			3.52	0.097	1.04	5,500				0.06
	PAT	Propyl Acetate (n-)	1			3.52	0,098	1.04	5,500				0.06
151		Propyl Alcohol (iso-)	1	0.79		2,07	0.091	1.06					0.05
	PAL	Propyl Alcohol (n-)	1	0.80	1.20	2.07	0.082	1.02	5,500			0,025	
	PBY	Propylbenzene (all isomers)	1	0.86		4.14	0.079	1.00				0.023	0.04
154		iso-Propylcyclohexane	1	0,80	0.01	4.35	0.076	1.00			5507	0.022	0.04
	PPG	Propylene Glycol	1		0.01	2.62	0,076	1.00			5504		0.04
	PGN	Propylene Glycol Methyl Ether Acetate	1	0.92	0.70	3.11	0.083	1.01	5,500				0,04
	PTT	Propylene Tetramer	1			1.00	0.076	1.00	5,500	5502	5502	0.022	0.04
	SFL	Sulfolane	1		0.01	4.14	0.076	1.00	5,500	5501	5506	0.022	0.04
	STY	Styrene	2	0.92	0.40	3.60	0.081	1.01	5,500	5544	5719	0.024	0,04
	TTG	Tetraethylene Glycol	1	1.20	0.01	6.70	0.076	1.00	5,500	5501	5511	0.022	0.04
	THN	Tetrahydronaphthalene	1	0,97	0.04	4.56	0.077	1.00	5,500	5504	5529	0.022	0.04
	TOL	Toluene	1	0,87	1.50	3.14	0.091	1.03			6201	0.028	0.05
163	TCN	1,2,3-Trichloropropane	3	1.39	0.15	5.60	0.079	1.00	5,500	5517	5633	0,023	0.0
164	TCP	Tricresyl Phosphate (less than 1% of ortho	1	1.16	0.01	12,69	0.077	1.00	5,500	5501	5521	0.022	0.0
165	TEB	Triethylbenzene	1	0.86	0.02	5,60	0.077	1.00	5,500	5502	5518	0.022	0.0
166	TEN	Triethylamine	3	0,73	2,50	3,49	0.105	1.05	5,500	5775	6795	0.034	0.0
167	TEG	Triethylene Glycol	1	1.12	0.01	5.17	0.076	1.00	5,500	5501	5508	0.022	0.0
168	TPS	Triethyl Phosphate	1	1.07	0.03	6.28	0,077	1.00	5,500	5503	5530	0.022	0.0
169	TRE	Trimethylbenzene (all isomers)	1	0.89	0.14	4.20	0,078	1.00	5,500	5515	5588		0.04
	TRP	Trixylenyl Phosphate	1	1.16	0,00	14.20	0.076	1.00	5,500	5500	5500	0,022	
171	THE	Tetrahydrofuran	1	0,89	8.50								
172	UDC	Undecene	1	0.75		5.32		1.00					
	UND	Undecyl Alcohol	1	0.84		5.94							
174	VAM	Vinyl Acetate	2			2,97	0,130						
	XLX	Xylenes (ortho-, meta-, para-)	1			3.68							

Notes:

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1. The above data is sourced from the USCG CHRIS Manual (Ref. 7) & from various manufacturer's MSDS's.

# Calculation of Maximum Liquid Transfer Rate as Imposed by the Capacity of theTable 2Cargo Tank Venting System

Note: Darcy's equation will be used to estimate the pressure drop of the vapor-air mixture through the vent piping from the farthest tank in terms of equivalent pipe length (#1P) to the P-V valve. Equivalent length for this path is calculated using Crane's Technical Paper 410 (Ref 4) and Cameron Hydraulic Data handbook (Ref 9).

Calculate equivalent lengths of pipe:

a. <u>Pipe run #1</u>

Description:

Pipe size, nominal: Pipe ID (inches): 8" Branch (Exp trunk to vapor stack) 8" sch. 40 pipe 7.98

ltem	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
	Entropy of		1		00.0
<u> </u>	Entrance	8	1	23.3	23.3
2	Straight Pipe	8	1	54.0	54.0
3	Tee, branch	8	2	39.9	79.8
4	Tee, flow	8	1	13.3	13.3
5					
6					
	Sum (pipe run #1)				170.4

<u>Pipe run #2</u> Description: Pipe size, nominal: Pipe ID (inches):

b.

6" branch at P-V valve 6" sch. 40 pipe 6.07

Item	Description	Size (in)	Qty	Unit Equivalent Length (ft)	Total Equivalent Length (ft)
1	Straight Pipe	6	1	3.0	3.0
2	Reducer (8x6)	6	1	6.4	6.4
	Sum (pipe run #2)				9.4

#### Vapor Recovery Calculations

### Table 3 Calculation of Maximum Liquid Transfer Rate as imposed by the Capacity of the Cargo Tank Venting System (Continued)

A. :	Calculate	pressure drop using Darcy's equation:				Pipe run #1		····-	Pipe run #2	<u> </u>		ı	
						Description:	8" Branch (Exp in stack)	unk to vapor		6" branch at P-V	(uoluo		
						Pipe ID:	7,98	(in)	Pipe ID:	6.07			
						Equiv, Pipe Length (table			Equiv, Pipe Length (table				
						2a):	170.4	(feet)	2b):	9.4	(feei)		
						Darcy friction factor:	0.014		Darcy friction factor;	0.015	j		
			Vapor-air Mixture Weight	Liquid		Vapor			Vapor			Pressure	Air Eaultr
	CHRIS		Density (from	Transfer	Vapor Growth	Volumetric Flow		Pressure Drop	Volumetric Flow		Pressure Drop	Drop	Volumetric
	Code	Name	Table 1) (b/@^3)	Rate (filling) (bbl/hr)	Rate	Rate (bbl/hr)	Mean Velocity (ft/s)	(pipe run #1) (psig)	Rate (bbl/hr)	Mean Velocity (ft/s)	(pipe run #2) (psig)	(Total) (psig)	Flow Rate (bbl/hr)
	AGN AGT	Acrylonitrile	0.095	5,500		6050	27.16	0,027	6050	46.95	0,006	0.0	33 6756
3	ACP	Acetophenone	0.123	5,500	1,012	6600 6600 5566		0,042	e 6600 5566			0.0	
	AND AEC	Adiponitrile Amyl acetate (all isomers)	0.076									0.0	22 6506
6	AAI	Amyl Alconol (iso-, n-, sec-, primary)	0,079	5,500	1.006	5533	24.84	0.019	5533	42,94	0.004	0,0	23 5637
	ATN BAL	Acetonitrile Benzyl Alcohol	0.076						5503 5511				
	BNZ BTX	Benzene Benzene, Toluene, Xylene mixtures (10% Benzen	0.114				30.87	0.042		53.35	0.010	0.0	52 8420
11	BAR	Butyl Acrylate (iso-, n-)	0.086	5,500	1.012	2 5566	24.99	0.021	5566	43,19	0.005	0.0	26 5908
	BAX	Butyl Acetate (all Isomers) Butyl Alcohol (iso-)	0,085		1.012								
	BAN BAS	Butyl Alcohol (n-) Butyl Alcohol (sec-)	0.074	5,500	1.010	5555	24,94	0.018	3 5556	43.11	0.004	0.0	22 5477
16	BAT	Butyl Alcohol (tert-)	0.097	5,500	1.056	5808	26.08		5643 5 5808			0.0	
	BPH BAD	Butyl Benzyl Phthalate	0.077		0 1,000				5501 6358			0.0	22 5516
19	BTR	n-Butyraidehyde	0,131	1 5,500	1.156	5 6358	28,65	0.041	6358	49.34	4 0.010	0.0	51 8344
21	BUE	Butyl Toluene Caprolactam Solutions	0.078	7 5,500	1.001	5506						0.0	22 5530
	CCH CHA	Cyclohexanone Cyclohexylamine	0.078	5,500	) 1.004	1 5522	24,79	0.019	5522	2 42,85	5 0.004	0.0	23 5603
24	снх	Cyclonexane	0.116	6,500	1,090	5995	26.92	0,033	3 5995	6 46.52	2 0.008	0.0	140 7410
26	CHN CPD	Cyclohexanol 1,3-Cyclopentadiene dimer (molten)	0.078		0 1.003							0.0	23 5579
27	CMP CRB	p-Cymene	0,078	3 5,500	1.002	2 5512	2 24.75	0.018	5512	42.78	B 0.004	0,0	23 5579
29	CRS	Chlorobenzene Cresols	0.087	7 5,500	1,002	2 5509	24.73	0,018		42.75	5 0.004	0,0	
	CUM IDA	Cumene Decaldehyde (Iso-)	0.085							43.19	9 0.005	0.0	25 5887
32	DAL.	Decaldehyde (n-)	0.076	6 5,500	1.000	5500	24,70	0.018	5500	42.68	B 0.004	0,0	22 6500
	DCE DAX	Decene Decyl Alcohol (all isomers) (Decanol)	0.078										23 5590
	dbz DAA	Decylbanzene (n-) Diacetone Alcohol	0,076				24.70	0.018	B 5501	42,69	9 0.004	0,0	22 5512
37	DCH	1,1-Dicholoroethane	0,168	6,500	1.198	8 6589	29.59	0.064	4 6589	51.13	3 0.015	0.0	023 5562 079 1036
	DPA DEB	Dibutyl Phthalate (ortho-) Diethybenzene	0.076						8 6500 8 5509				022 550 023 555
40	deg Den	Diethylene Glycol	0,076	6 5,500	1.000	5501	24,70	0.018	8 5501	42.69	9 0.004	0.0	22 5506
42	DBL	Disthylamine Disobulylene	0.083										25 5864 032 6654
	DIK DIP	Discbutyl Ketone Discopropanolamme	0.079										023 5623 022 550
45	DIX	Dilsopropylbenzene (all Isomers)	0.077	7 5,500	1.001	1 5503	3 24,71	0.018	8 5503	42.71	1 0.004	0,0	022 652
	DTL DOP	Olmethyl Phthalate Dioclyl Phthalate	0.076		1.000								022 5500 022 5500
	DPN DIL	Dipentene Diphenyl	0.076				24.74	0,018	8 5511	42.77	7 0,004	0.0	023 557
50	DDO	Diphenyl, Diphenyl Ether Mixtures	0,076	6 5,500	1.000	5501	1 24,70	0.018	8 5501	42,68	9 0.004		022 6504
	DMF DPE	Dimethylformamide Diphenyl Ether	0.078										023 561( 022 550)
	DPG DPX	Dipropylene Glycol 1,1-, 1,2-, 1,3-Dichloropropane	0.077	7 5,500	1.001	1 5508	24.73	0.018	8 5508	42.74	4 0.004	0.0	23 655
55	DFF	Distillates Flashed Feed Stocks	0.102	2 5,500	1.046	6 5753	3 25.83	0.026	6 5763	3 44.6	5 0,006	0.0	X60 903- X32 666
	DSR DOZ	Distillates Straight Run Dodecene (all isomers)	0.102										032 666
58	DDB EAC	Dodecylbenzene	0,240	0 5,500	1.250	6875	5 30,87	0.088	8 6876	5 53,3	5 0.021	0.1	109 1219
60	EAI	Ethyl Acrylate 2-Ethylhexyl acrylate	0.077	7 5,500	1,000	5502	2 24.71	0.018					031 654 022 552
	EEA ETG	2-Ethoxyethyl acetate Ethoxy Triglycol (crude)	0,077		0 1.000							\$ 0.0	022 551
63	ETA EAA	Ethyl Acetate	0.119	9 5,500	D 1.090	5995	5 26.92	2 0.033	3 6995	5 46,52	2 0.008	3 0.0	041 750
65	EAL	Ethyl Aceloacetate Ethyl Alcohol (Ethanol)	0.079	6 5,500	1.070	0 5885	5 26.42	2 0.023	3 5885	5 45,6			023 563 029 625
	ETB EBT	Ethyl Benzene Ethyl Butanol	0.083									ő 0. <b>C</b>	025 582 023 556
68	EBE	Ethyl tert-butyl ether Ethyl butyrate	0.078	8 5,500	1.004	4 5521	1 24,79	0.019	9 5521	1 42,8	5 0.004	0.0	023 560
70	ECY	Ethyl Cyclohexane	0.083	3 5,500	1.010	0 5555	5 24.94	4 0.020	0 6555	5 43.11	1 0,008	5 0.0	027 610 025 579
	EDC EGL	Ethylene dichloride	0,122									30,0	
73	EMA	Ethylene Glycol Butyl Ether Acetate	0,077	7 5,500	0 1.001	1 5508	3 24.72	2 0.016	8 5506	s 42,73	2 0.004	1 0.0	022 554
75	EGY	Ethytene Glycol Diacetate Ethytene Glycol Phenyt Ether	0.076	6 5,500	0 1.000	0 5501							022 550 022 550
	EEP EHX	Ethyl-3-ethoxypropionate 2-Ethylhexanol	0,076	6 5,500	1.000	0 5501	1 24.70	0.018	8 5501	1 42,69	9 0.004	4 0,0	022 551 022 551
78	EPR	Ethyl Propionate	0.086	6 5,500	0 1.070	0 5885	5 26.42	2 0,023	3 5885	5 45.63	7 0.005	5 0.0	029 625
80	ete Fam	Ethyl Toluene Formamide	0.080										024 567 022 552
81	FMS FAL	Formaldehyde Solution Furfuryl Alcohol	0,076	6 5,500	1.003	3 5517	7 24.77	7 0.018	8 5517	7 42.8	1 0.004	1 0,0	022 551
83	FFA	Furfural	0.078	8 5,500	0 1.003	3 5517	7 24.77	7 0.016	8 5517	7 42.8	1 0.004	\$ 0,0	022 552 023 557
	GAK GRF	Gasoline Blending Stocks: Alkylates Gasoline Blending Stocks: Reformates	0.217										099 <u>1161</u> 099 1161
86	GAT	Gasolines; Automotive	0.217	7 5,600	1.250	0 6875	5 30.87	7 0.080	0 6875	5 53.3	5 0.019	9.0.0	099 1161
88	GAV GCS	Gasolines: Aviation Gasolines: Casinghead	0,217	7 5,500	1.250	0 6875	5 30,87						099 1161 099 1161
	GPL GSR	Gasolines: Polymer Gasolines: StralghtRun	0.217	7 5,500	1.250	0 6876	5 30.87	7 0.080	6875	5 53,3	5 0.019	9,0	099 1161
91	GCR	Glycerine	0.076	6 5,500	1.000	5500	24.70	0.018	8 5500	0 42,64	8 0,004	0.0	099 <u>1161</u> 022 550
	HMX	Heptane (all Isomers) Heptonic Acid	0.105								2 0.000	3 0,0	034 677 022 550
94	HTX	Heptanol (all isomers)	0.077	7 5,500	1.001	1 5504	4 24,72	2 0,018	8 5504	4 42.7	2 0,004	4 0.0	022 552
	HPX	Heptene (all isomers)	0,109										035 695
96	HXS	Hexane (all isomers)	0.142							40.0	u 0.015	ղ սո	
96 97		Hexane (all isomers) Hexaonic Acid Hexanol	0.142	6 5,500	1.000	0 5501	1 24.70	0.018	8 5501	1 42.6	9 0.004	4 0.0	022 550 027 603

#### Vapor Recovery Calculations

					Pipe run #1 Description: Pipe ID: Equiv. Pipe Length (table 2a); Darcy friction factor:	8" Branch (Exp Ir stack) 7.98 170.4 0.014	(in) (feel)	Pipe run #2 Description: Pipe ID: Equiv. Pipe Length (table 2b): Darcy friction factor:	6" branch at P-V 6.07 9.4 0.015	(in) (feel)		
	Name	Density (from Table 1) (lb/ft^3)	Liquid Transfer Rate (filling) (bbi/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (öb)/hr)	Mean Velocity (ft/s)	Pressure Drop (pipe run #1) (psig)	Vapor Volumetric Flow Rate (bbl/ar)	Mean Velocity (ft/s)	Pressure Drop (pipe run #2) (psig)	Pressure Drop (Total) (psig)	Air Equiv, Volumetrio Flow Rate (bbl/hr)
100 HXG 101 IPH	Hexylene Glycol Isophorone	0.076	5,500 5,500	1.000	5501 5501	24.70	0.018		42,69		0,022	
102 JPF 103 JPV	Jet Fuels; JP-4	0,124	5,500 5,500	1.068	6874	26.37	0:033	5874	45.56	0.008	0.041	7499
104 KRS	Jet Fuels JP-5 (Kerosene, heavy) Kerosene	0.078		1.002	5511		0,018		42.77			
	Methyl Acetate Methyl Alcohol (Methanol)	0.122			6171		0.036				0.045	7812
107 MAC	Methylamyl Acetate	0.082	5,500	1,007	5536	24.86	0.020	5536	42,96	0.005	0.024	6766
	Methylamyl Alcohol Methylamyl Keytone	0,081	5,500	1.009	5547	24,91	0,019			0,005	0.024	
110 MAM	Methyl Acrylate	0,115	5,500	1,082	5951	26,72	0.032	5951	46,18	0,007	0.039	7303
	Methyl Tert-Butyl Ether (MTBE) Methyl Butyl Ketone	0.077			5504	24.72						2 5519 6012
	Methyl Bulyrate Methyl Ethyl Ketone	0.091	5,500 5,500		5639	25.32	0.023	6639	43,76	0.005	0,028	3 6168
116 MHK 1	Methyl Heptyl Ketone	0.077	5,500	1.001	5995 5507	24.73	0,018	5507	46.52	0.004		
116 Mik 117 MMM	Methyl Isobutyl Ketone Methyl methaorylate	0,089			562	25.26	0,023		43.66	0.005	0.027	6096
118 MNA	Methyl Naphthalene	0.076	5,500	1,000	5501	24.70	0.018	3 5501	42,69	0,004	0.022	2 5508
	Mineral Spirits Morpholine	0.079			5522							
121 MRE	Myrcene	0,079	5,500	1.003	5519	24.78	0,019	5519	42.83	0.004	0,023	3 5625
122 PTN 123 NSV	Naphtha: Petroleum Naphtha: Solvent	0.078			5521							
124 NSS 126 NVM	Naphtha: Stoddard Solvent Naphtha: VM&P	0.079			552							3 5633
126 NAX	Nonane (all Isomers)	0,080	5,500	1.005	5530	24.83						
127 NON 128 NNS	Nonene (all Isomers) Nonyl Alcohol (all isomers)	0.082			5539 551							
129 NNP	Nonyl Phenol	0.076	5,500	1.000	550	24.70	0.011	8 5501	42,69	0.004	0,022	2 5612
130 NPM 131 OAX	1-, 2-Nitropropane Octane (all isomers)	0,086	5,500	0 1.021 0 1.016	5610							
	Octanol (all isomers)	0.076	5,500	1,000	550	24.70	0.01	650	42.6	0.004	0.022	2 5507
134 OTW	Octene (all isomers) Oil, fuel: No. 2	0,088		1.018								
	Oll, fuel: No. 2-D Oll, fuel: No. 4	0.084			557						0.025	5 5853
137 OFV	Oll, fuel; No, 5	0,078	5,500	1.003	551	24.77	0.01	8 5517	42.8			
138 OSX 139 OIL	Oll, fuel: No. 6 Oil, miso: Crude	0.078			551							3 5577 5 6951
140 ODS	Oil, Misc: Diesel	0.084	5,500	1.014	557	5 25.04	0.02	5570	43,2	0,005	0.02	5854
	Oli, Miso: Lubricating Oli, Miso: Residual	0.076										
	Oll, Mise: Turbine Pentane (all isomers)	0.062						553	42.9	0,005	5 D.024	4 5754
145 PTE	Pentene (all Isomers)	0.310	5,500	1.499	824				0 65.73 5 63.94			
146 PIN 147 PLB	Pinene Polybutene	0.083							2 43.0 I 42.6			4 5777
148 PGC	Polypropylene Glycel	0.076	5,500	1.002	551	1 24.74	0,01	8 551	42.7	7 0.004	0.02	2 5511
149 IAC 150 PAT	Propyl Acetate (Iso-) Propyl Acetate (n-)	0.097										
151 IPA 152 PAL	Propyl Alcohol (iso-)	0.091	6,500	1.060	583	26.1	3 0.02	4 5830	45,24	40.006	6 0.030	0 6382
153 PBY	Propyl Alcohol (n-) Propylbenzene (all isomers)	0.079	5,50	1.004	i 552	2 24,79	0.01	9 5523	2 42.8	5 0.004		
154 IPX 155 PPG	iso-Propylcyclohexane Propylene Glycol	0.076				24.70	0.01	8 650	42,6	9 0.004	0.022	2 5501
156 PGN	Propylene Glycol Methyl Ether Acctate	0,083	5,500	1.014	557	25.04	0,02	0 557	43.2	B0.005	0.02	5 5826
157 PTT 158 SFL	Propylene Teiramer Sulfolane	0.076										
159 STY 160 TTG	Styrone Tetraethylona Glycol	0,08	5,50	1.008	554	4 24,8	9 0.01	9 654	43,0	2 0.005	0,02	4 5719
161 THN	Tetrahydronaphthalene	0.077	6,50	1.001	550	4 24.73	2 0.01	8 550-	4 42.7	2 0,004		
162 TOL 163 TCN	Toluene 1,2,3-Trichloropropane	0.091		0 1.030					5 43,9	5 0.005	0.02	8 6201
164 TCP	Tricresyl Phosphate (less than 1% of ortho isome	r 0,077	5,50	1.000	550	1 24.70	0,01	8 550	1 42.6	9 0.004	0.022	2 5521
165 TEB 166 TEN	Triethylbenzene Triethylamine	0.077										
167 TEG 168 TPS	Triethylane Glycol Triethyl Phosphate	0,076	5 5,50	1.000	550	1 24.7	0.01	8 550	1 42,6	9 0.004	0.02	2 5508
169 TRE	Trimethylbenzene (all isomers)	0.078	5,50	1.003	551	5 24.70	0.01	9 551	5 42.8	0.004	0,02	3 5588
170 TRP 171 THF	Trixylenyl Phosphate Tetrahydrofuran	0,076									0,022	2 5500
172 UDC	Undecene	0.077	5,50	1.001	550	5 24.73	2 0,01	8 550	6 42.7	2 0,004	0.02	2 5542
173 UND 174 VAM	Undecyl Alcohol Vinyl Acetate	0.078	5,500	1.110								
176 XLX	Xylenes (ortho-, meta-, para-)	0,083								2 0.005	5 0.02	4 5786
Greates	pressure drop to P-V valve:		(psig)	Pentane (all iso	mers)					max =	0.24	1 18150
Back pre Total ba	ocity P-V valve pressure setting; essure Imposed by P-V valve @ highost flow rate ck pressure Imposed on cargo tank by venting ign working pressure of tanks;	0.79	) (psig) ) (psig) 3 (psig) ) (psig)	Conclusion:		cargo loading rat pressure of the ta		pressure imposed	by the tank ventin	ng system does no	ot exceed th	e maximum

righ volucity F-v valve plessure setting;
Back pressure imposed by P-V valve @ highest flow rate
Total back pressure imposed on cargo tank by venting
Max design working pressure of lanks:

0,5 (pslg)

4300 (bbi/hr) 0,61 (psig)

<u>Check vacuum relieving capacity at maximum discharge rate:</u> Opening vacuum setting for PV Valve: В.

Maximum discharge rale (total); Corresponding vacuum at max discharge rate; (see attached PV valve flow capacity curve)

10

# Calculation of the Maximum Liquid Transfer Rate as Imposed by the pressureTable 4drop between the most remote tank and the facility vapor connection (Ref: 46CFR 39.30-1(d)(3):

Note: Darcy's equation will be used to estimate the pressure drop of the vapor-air mixture through the vent piping from the farthest tank in terms of equivalent pipe length (#1P) to the facility connection. Equivalent length for this path is calculated using Crane's Technical Paper 410 (Ref. 4) and Cameron Hydraulic Data handbook (Ref. 9)

# Calculate equivalent lengths of pipe:

a. <u>Pipe run #1</u>

Description: Pipe size, nominal: Pipe ID (inches): 8" Piping 8" sch. 40 pipe 7.98

ltem	Description	Size (in)	Qty		Total Equivalent Length (ft)
1	Entrance	. 8	1	23.3	23.3
2	Straight Pipe	8	1	195.0	195.0
3	Tee, branch	8	2	39.9	79.8
4	Tee, run	8	3	13.3	39,9
5	Elbow, 45 deg.	8	2	10.2	20.4
6	Valve, Gate	8	1	8.6	8.6
7	Hose	8	1	50.0	50.0
	Sum (pipe run #1)				417.0

#### Vapor Recovery Calculations

# Calculation of the Maximum Liquid Transfer Rate as Imposed by the pressure drop between the most remote tank and the facility vapor connection (Ref: 48 CFR 39.30-1(d)(3) (continued):

1. <u>Ca</u>	alculate	pressure drop using Darcy's equation:				Pipe run #1		·]		
						Description;	8" Piping			
						Pipe ID:	7.98	(in)		
						Equivalent Length of Pipe (from Table 4a):	417.0	(feet)		
		<u></u>		<u></u>		Darcy friction factor:	0.014			_
	HRIS	Name	Vapor-air Mixture Weight Density (from Table 1) (ib/ft^3)	Liquid Transfer Rate (filling) (bbl/hr)	Vapor Growth Rate	Vapor Volumetric Flow Rate (bbl/hr)	Mean Velocity (ff/s)	Pressure Drop (pipe run #1) (psig)	Pressure Drop (Total) (psig)	Air Equivatent Volumetric Flow Rate (bbl/hr)
1 A 2 A		Acrylonitrile Acetone	0,095	5,500 5,500	1,100	6050 6600	27.16	0.066	0.066	675
3 A 4 A	CP	Acetophenone Adiponitrile	0.085	5,500 5,500	1.012	5566	24,99	0.050	0.050	588
5 A 6 A	EC	Amyl acetate (all isomers)	0.075	5,500	1.007	5536	24.88	0.044	0.044	550
7 A	TN 1	Amyl Alcohol (iso-, n-, sec-, primary) Acetonitrile	0,076	5,500 5,500	1,001	5503		0.044	0.046	563
8 B. 9 B	NZ	Benzyl Alcohol Benzene	0.077	5,500	1.250	6875	30,87	0,103	0.045	655
10 B 11 B		Benzene, Toluene, Xylene mixtures (10% Benzene Butyl Acrylate (iso-, n-)	0.138	5,500			30,87		0.124	925
12 B	AX	Butyl Acetate (all isomers) Butyl Alcohol (Iso-)	0,085		1.012	5566	24.99 25.14	0.050	0.050	56
14 B	IAN	Butyl Alcohol (n-)	0.074	5,500	1.010	5555	24,94	0.044	0,044	547
15 B 16 B	AT	Butyl Alcohol (sec-) Butyl Alcohol (tert-)	0.086	5,500	1.056	5808		0.063	0,052	599 656
17 B 18 B	AD	Butyl Benzyl Phthalate Iso-Butyraldehyde	0.077	5,500 5,500	1.156	6358	28.55	0.101	0.044	55
19 B 20 B	UE	n-Butyraldehyde Butyl Toluene	0.131	5,500	1.156	5511	28,55	0.101	0,101	834
21 0	LS	Caprolactam Solutions Cyclohexanone	0.077	5,600	1.001	5506	24.72	0,044	0.044	55
23 C 24 C	HA	Cyclohexalanine Cyclohexalamine Cyclohexane	0.083	5,500	1.012	5568	25.00	0.049	0,049	582
25 C	ЖN	Cyclohexanol	0.078	5,500	1.003	6517	24.77	0.045	0.080	74
26 C	MP	1,3-Cyclopentadiene dimer (molten) p-Cymene	0.080	5,500 5,500	1.002	5512	24.75	0.045	0,047	56
28 C		Chlorobenzene Cresols	0.087	5,500					0.052	59
46 C 47 C		Dimethyl Phthalate Dioclyf Phthalate	0.076	5,500	1.000	5500	24.70	0.044	0,044	550
48 D 49 D	<b>PN</b>	Dipentene Diphenyl	0.076	5,500	1.002	5511	24.74	0,045	0,045	55
60 D	DO	Olphenyl, Diphenyl Ether Mixtures	0.076	6,500	1,000	5501	24.70	0,044	0.044	55
51 C 62 C	)PE	Dimethylformamide Diphenyl Ether	0,078	5,500	1.000	5501	24,70		0.046	56
53 D 54 D		Dipropylene Glycol 1.1-, 1.2-, 1.3-Dichloropropane	0.077	5,500					0,045	55
55 C	OFF DSR	Distillates Flashed Feed Stocks Distillates Straight Run	0.102	5,500	1,046	5763	25.83	0,064	0.064	66
57 C	00Z	Dodecene (all isomers)	0.077	5,500	1.000	5502	24.71	0.044	0.044	55
59 E	AC	Dodecylbenzene Ethyl Acrylate	0.240	5,500	1.040	5720	25,68	0.062	0.062	121
60 E 61 E	EA	2-Ethylhexyl acrylate 2-Ethoxyethyl acetate	0.077	5,500	1,000	5503	24.71	0,044		<u>55</u>
62 E 63 E		Ethoxy Triglycoi (crude) Ethyl Acetate	0,076							55 75
64 E		Ethyl Acetoacetate Ethyl Alcohol (Ethanol)	0.079				2 24,79	0.046	0,046	56
66 E	ETB	Ethyl Benzene Ethyl Butanol	0,083	5,500	1.012	5566	24.99	0.049	0.049	58
68 E	EBE	Elhyl tert-butyl ether	0.078	5,500	1.004	5521	24.79	0,046	0.046	55
69 E 70 E	ECY	Ethyl butyrate Ethyl Cyclohexane	0.090	5,500	1.010	5555	i 24.94	4 0.049	0.049	61
71 E 72 E		Ethylene dichloride Ethylene Glycol	0.122						0.082	75
73 E 74 E		Ethylene Glycol Butyl Ether Acetate Ethylene Glycol Diacetate	0.077					0.045	0.045	
75 E 76 E		Ethylene Glycol Phenyl Ether Ethyl-3-ethoxypropionate	0.076				24.70		0.044	55
77 E 78 E	EHX	2-Ethylhexanol Ethyl Propionate	0,076	5,500	1.000	5502	24.7	0.044	0.044	55
79 E	ETE	Ethyl Toluene	0.080	5,500	1,000	5531	24.83	3 0,047	0.057	62 56
80 F 81 F	-MS	Formamide Formaldehyde Solution	0,076	5,600	1.003	5517	24.7	7 0.044	0.044	5
82 F 83 F		Furfuryl Alcohol Furfural	0.077							55
84 C		Gasoline Blending Stocks: Alkylates Gasoline Blending Stocks: Reformates	0,217		1.250	687	30.8	7 0.196	0,196	110
86 0	GAT	Gasolines: Automotive Gasolines: Aviation	0.217	5,500	) 1.250	6875	5 30,8	7 0,196	0,196	110
88 0	GCS	Gasolines: Casinghead	0,217	5,500	1.250	6876	30.8	7 0.196	0.196	110
89 C 90 C	3SR	Gasolines: Polymer Gasolines: StraightRun	0.217	5,500	1.250	6875	30,8	7 0.196	0,196	110
91 C 92 P		Glycorine Heptane (all Isomers)	0,076		0 1.000				0.044	5
93   94	ΗĒΡ	Heptonic Acid Heptanol (all isomers)	0.076	5,500	1.000	550	24.70	0.044	0,044	5
95   96	IPX	Heptene (all isomers) Hexane (all isomers)	0.105	5,500	1.058	3 5819	26.1	3 0.070	0.070	6
97	-ixo	Hexaonic Acid	0,076	5,600	1,000	550	24.70	0.044	0.044	B: 5:
98 H 99 H	HEX	Hexanol Hexene (all isomers)	0,088	5,500	1.160	6386	28,65	5 0.115		6
100 H	HXG	Hexylene Glycol Isophorone	0.076	5,500	1.000	550	1. 24.70	0.044	D.044	5
102 103 J	IPF	Jet Fuels; JP-4 Jet Fuels JP-5 (Kerosene, haavy)	0.124	5,500	1,068	3 5874	26.3	7 0,082	0.082	7
104 M	KRS	Kerosene	0.079	5,50	1.003	551	7 24.7	7 0.046	0,046	5
105 M	MAL	Methyl Acetate Methyl Alcohol (Methanol)	0.122	5,500	1.13	8229	27,9	7 0,059	0.059	
107 M	MAA	Methylamyl Acetate Methylamyl Alcohol	0.082							57
109 M		Methylamyl Keytone Methyl Acrylate	0.076	5,50	1.001	5500	3 24.7:	2 0.044	0,044	55

Pipe run #1		
Description: Pipe ID:	8" Piping	7.98 (in)
Equivalent Length of Pipe (from Table 4a):		417.0 (feet

Table 4a):	417.0
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				Darcy	friction factor:	0.014			
111 MBE	Methyl Tert-Butyl Ether (MTBE)	0.077	6,500	1.001	5504	24.72	0.044	0.044	6519
	Methyl Butyl Ketone	0.088	5,500	1.019	5607	25,17	0,053	0.053	6012
	Methyl Butyrate	0.091	5,500	1.025	5639	25,32	0.055	0.055	6165
	Methyl Ethyl Ketons	0.108	5,500	1,090	5995	26.92	0.074	0.074	7135
	Methyl Heptyl Ketone	0.077	5,500	1.001	5507	24.73	0.045	0.045	5548
	Methyl Isobutyl Ketone	0,089	5,600	1.023	5627	25.26	0.054	0,054	6096
	Methyl methacrylate	0,099	5,500	1.040	5722	25,69	0.062	0.062	6538
	Methyl Naphthalene	0.076	5,500	1.000	5501	24,70	0.044	0.044	5508
	Mineral Spirits Morpholine	0.079	5,500	1.004	5522	24,79	0.046 0.050	0.046	5633
	Myrcene	0.079	5,500	1.003	5519	25.09 24.78	0.050 0.046	0.050	5857
	Naphtha: Petroleum	0.078	5,500	1.003	5521	24.79	0.046	0.046	5625
	Naphtha: Solvent	0.078	5,500	1.004	5522	24.79	0.046	0,046	5600
	Naphtha: Stoddard Solvent	0.079	5,500	1.004	5522	24.79	0.046	0.046	5633
	Naphtha: VM&P	0.079	5,500	1.004	6521	24.79	0.046	0.046	562
	Nonane (all isomers)	0,080	5,500	1.005	6530	24.83	0,047	0.047	5684
	Nonena (all isomers)	0.082	5,500	1.007	6539	24.87	0.048	0.048	573
	Nonyl Alcohol (all isomers)	0.078	5,500	1.002	6511	24.74	0.045	0.045	557
	Nonyl Phenol	0.076	5,500	1,000	5501	24.70	0.044	0.044	5512
	t-, 2-Nitropropane	0,086	5,500	1,021	5616	25.21	0.052	0.052	5971
131 OAX	Octane (all Isomers)	0,087	5,500	1.016	5587	25.09	0.052	0,052	596
132 OCX	Octanol (all Isomers)	0,076	5,500	1.000	5501	24.70	0.044	0,044	550
	Octene (all somers)	0.088	5,500	1.018	5599	25.14	0,053	0.053	603
	Oil, fuel: No. 2	0.095	5,500	1.011	5562	24.97	0.056	0.056	619
	Oil, fuel: No. 2-D	0.084	5,500	1.014	5576	25.04	0.050	0,050	585
136 OFR	Oil, fuel: No. 4	0.078	6,500	1.003	5517	24.77	0.045	0.045	557
137 OFV	Oll, fuel: No. 5	0.078	5,500	1.003	5517	24,77	0.045	0.045	557
	Oil, fuel: No. 6	0.078	5,500	1,003	5517	24.77	0.045	0.045	557
139 OIL	Oil, misa: Crude	0.078	6,600	1.250	6875	30.87	0.070	0,070	695
140 ODS 141 OLB	Oll, Mise; Diesel Oll, Mise; Lubricating	0.084	5,500 5,500	1.014	5576 5517	25.04	0.050	0,050	585
	Oil, Misc: Lubricaurig Oil, Misc: Residual	0.076	5,500	1.003	5517	24,77	0.044	0.044	551
	Oil, Misc: Turbine	0.078	6,600	1,005	5533	24.77	0.044	0.044	551
144 PTY	Pentane (all isomers)	0.350	5,500	1,540	8470	38,03	0.040	0,048	675- 1815
145 PTE	Pentene (all isomers)	0.310	5,500	1.499	8245	37,02	0,402	0,402	1664
146 PIN	Pinene	0.083	5,500	1,008	5542	24.88	0.048	0.048	577
147 PLB	Polybutene	0.076	5,500	1,000	6501	24.70	0.044	0.044	550
148 PGC	Polypropylene Glycol	0.076	5,500	1,002	5511	24.74	0.044	0.044	551
149 IAC	Propyl Acetate (iso-)	0.097	5,600	1.036	5698	25,58	0.060	0.060	644
150 PAT	Propyl Acetate (n-)	0,098	5,500	1.037	5704	25,61	0,061	0.061	647
151 IPA	Propyl Alcohol (iso-)	0.091	5,500	1,060	5630	26.18	0,059	0.059	638
152 PAL	Propyl Alcohol (n-)	0.082	5,500	1,024	5632	25.29	0.050	0.050	585
153 PBY	Propylbenzene (all Isomers)	0,079	5,500	1,004	5522	24.79	0.046	0.046	562
154 IPX	iso-Propylcyclohexane	0,076	5,500	1.000	5501	24.70	0.044	0,044	550
155 PPG	Propylene Glycol	0,076	5,500	1,000	6501	24,70	0.044	0.044	550
158 PGN	Propylene Glycol Methyl Ether Acetate	0.083	5,500	1.014	5577	25,04	0,049	0.049	582
157 PTT	Propylene Tetramer	0.076	5,500	1,000	5502	24.71	0,044	0.044	550
158 SFL 169 STY	Sulfolane Styrene	0.076	5,500	1,000	5501	24.70	0.044	0.044	550
169 STY 180 TTG	Styrene Tetraethylene Glycol	0:081	5,500	1.008	5544	24,89	0,048	0,048	571
161 THN	Tetrahydronaphthaleno	0.078	5,500	1.000	5604			0.044	551
162 TOL	Toluene	0.091	5,500	1.001	5665	24,72	0.044	0.044	552
163 TCN	1,2,3-Trichloropropane	0.079	5,500	1.003	5517	23.44	0.036	0,046	620 563
164 TCP	Tricresyl Phosphate (less than 1% of ortho isomer)	0.077	5,500	1.000	5501	24.70	0.046	0.046	552
165 TEB	Triethylbenzene	0.077	5,500	1.000	5502	24.71	0.044	0.044	551
166 TEN	Triethytamine	0.105	5,500	1,050	5775	25.93	0,067	0.067	67
167 TEG	Triethylene Glycol	0,076	5,500	1.000	5501	24.70	0.044	0.044	550
168 TPS	Triethyl Phosphate	0,077	5,500	1.001	5503	24.71	0.044	0.044	553
169 TRE	Trimethylbenzene (all isomers)	0.078	6,500	1.003	5515	24,76	0.045	0.045	558
170 TRP	Trixyleny Phosphate	0.076	5,500	1.000	5500	24.70	0.044	0.044	550
171 THE	Tetrahydrofuran	0,090	6,500	1.170	6435	26.89	0.071	0.071	700
172 UDG	Undecene	0,077	5,500	1.001	5506	24.72	0.045	0.045	554
173 UND	Undecyl Alcohol	0.076	5,500	1.000	5501	24,70	0.044	0.044	550
174 VAM	Vinyl Acetate	0.130	5,500	1,116	6138	27,56	0,093	0.093	B01
175 XLX	Xylenes (ortho-, meta-, para-)	0.083	5,500	1.010	5556	24.95	0.049	0.049	578
							max	= 0,479	18

Compare pressure drop to P-V valve pressure settings: a, High-velocity P-V Valve pressure setting: b, Cargo tank P-V Valve pressure setting: c, 80% of lowest P-V Valve Pressure Setting: d. Highest Pressure Drop from Tank to Facility Connection: e, Max Allowable Back Pressure at Facility Connection: 2.

1.50 (peig) 1.50 (peig) <u>1.20 (peig)</u> 0.48 (peig) 0.72 (psig)

for

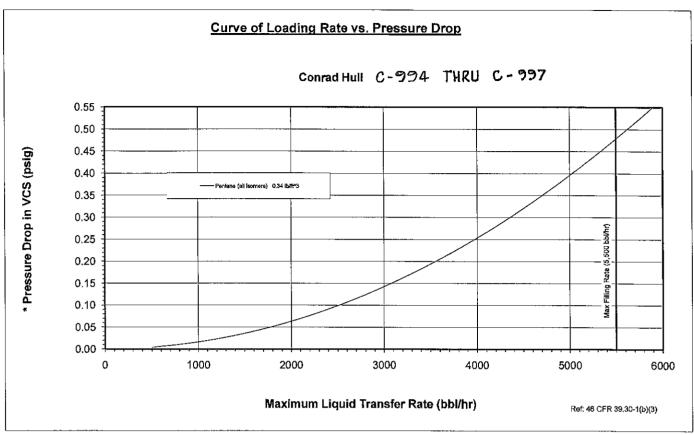
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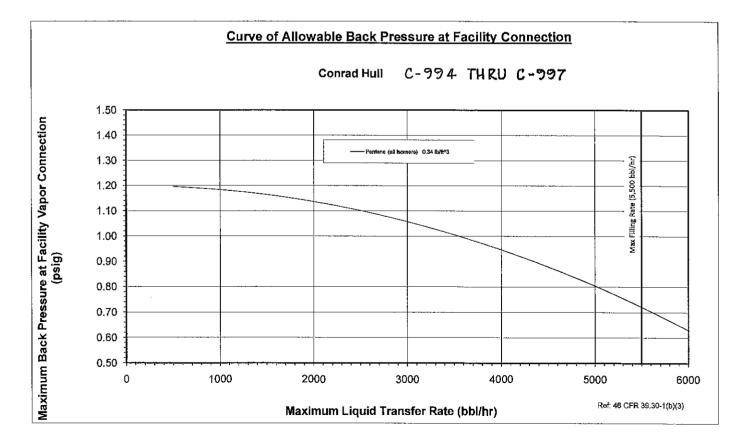
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Pentane (all isomers)

Conclusion: For the cargo with the highest pressure drop (Pentane), the pressure drop is 0.48 psig. This, when added to the back pressure at the facility vapor connection must not exceed 80% of the pressure setting of any P-V valve in the cargo tank venting system. Therefore, the maximum allowable back pressure at the shore facility must not exceed 0.72 psig when loading with Pentane at the maximum liquid transfer rate (5,600 bb/hm).

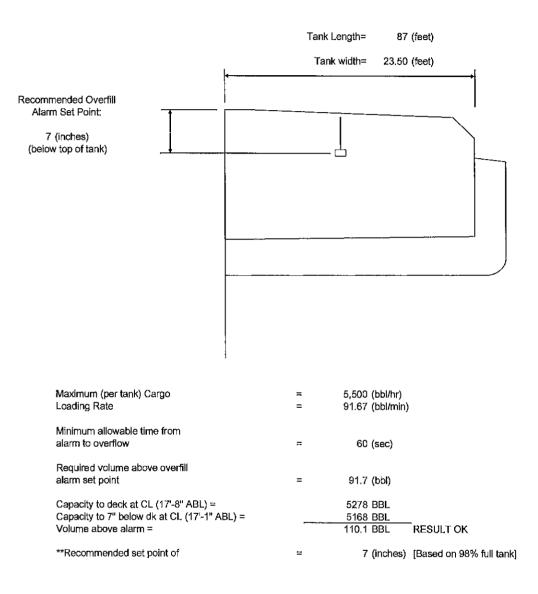
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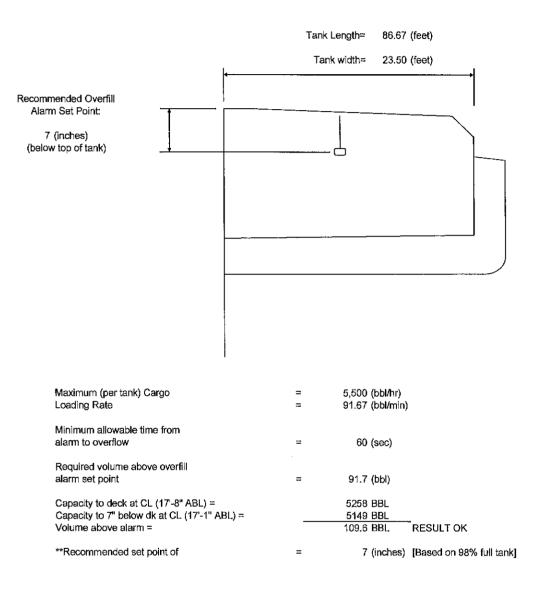
Graphs as required by 46 CFR 39.30-1(b)(3)

# Conrad C~994 THRU C**~997** <u>Calculation of Overfill Alarm Set Point</u> (Cargo Tank No. 1 P/S)

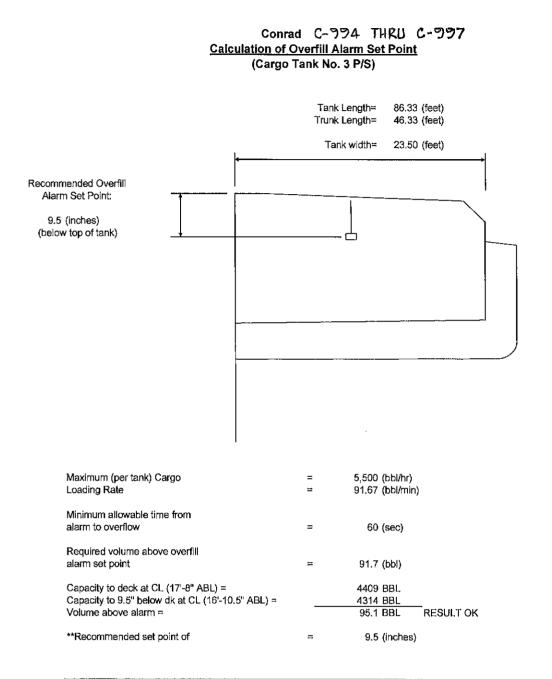


**Note: Or 98.5%, whichever is lower (to	comply with 33CFR155.775)
Capacity at 98.5% =	5199 BBL
Dist from TT at CL =	0.49 ft.

# Conrad C-994 THRU C-997 Calculation of Overfill Alarm Set Point (Cargo Tank No. 2 P/S)



**Note: Or 98.5%, whichever is lowe	r (to comply with 33CFR155.775)
Capacity at 98.5% ≂	5179 BBL
Dist from TT at CL =	0.49 ft.



**Note: Or 98.5%, whichever is low	er (to comply with 33CFR155.775)
Capacity at 98.5% =	4343 BBL
Dist from TT at CL =	0.63 ft.

# **REFERENCES**

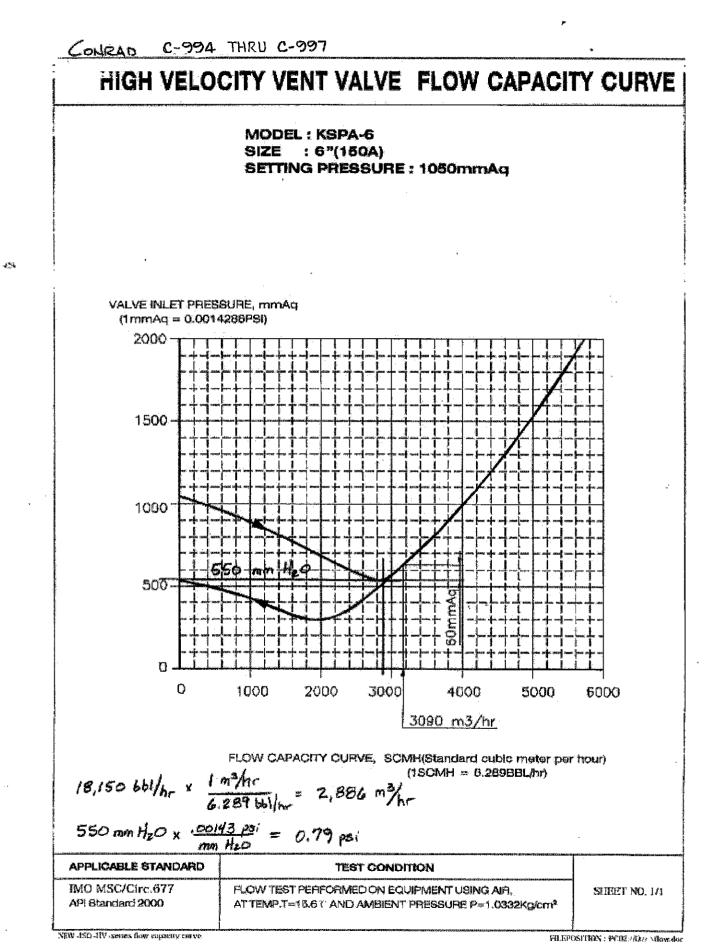
- 1. 46 CFR 32.55-25, Venting of cargo tanks of tank barges constructed on or after July 1, 1951 B/ALL
- 2. 46 CFR 39.20-11, Vapor overpressure and vacuum protection TB/ALL
- 3. 46 CFR 39.30-1, Operational Requirements TB/ALL
- 4. Flow of Fluids Through Valves, Fittings, and Pipe; Crane Technical Paper No. 410
- 5. USCG Guidelines for Determining the Maximum Liquid Transfer Rate for a Tank Vessel Transferring a Flammable or Combustible Cargo Using a Vapor Control System
- 6. Conrad Dwg. 994-P3 Vapor Control Piping
- 7. USCG CHRIS (Chemical Hazards Response Information System) Manual.
- 8. 46 CFR 39.20-9, Tank Barge Liquid Overfill Protection B/ALL
- 9. Cameron Hydraulic Data, 15th edition

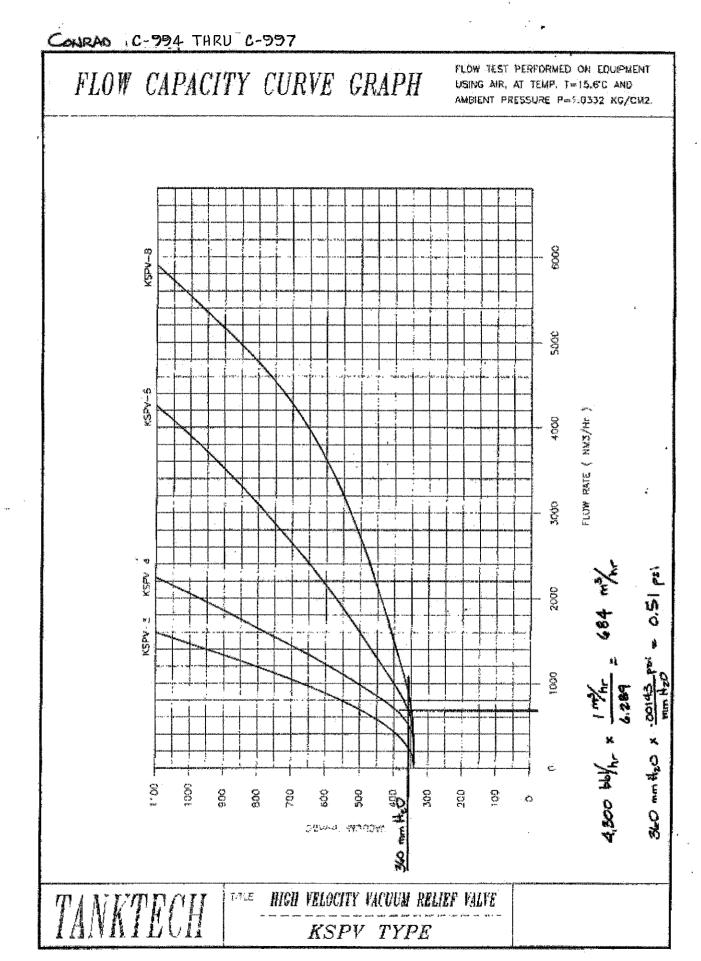
# LIST OF ATTACHMENTS

- 1. Flow Capacity Curves for High-Velocity P-V Valve
- 2. Vacuum flow diagram for High-Velocity P-V Valve

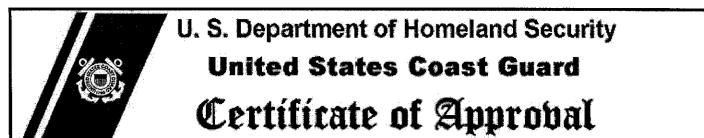
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3. USCG Approval Certificate for High-Velocity P-V Valve





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Coast Guard Approval Number: 162.017/144/3

Expires: 17 March 2016

PRESSURE-VACUUM RELIEF VALVES FOR TANK VESSELS

TANKTECH CO., LTD. #1506-2 SONGJEONG-DONG GANGSEO-GU BUSAN 618-270 KOREA, REPUBLIC OF

Model KLPH-6 ND 150 high velocity pressure/vacuum relief valves. AISI 304 Stainless steel, wt.-loaded construction.

Identifying Data: Drwg: KSP #PHZZ3000 dtd. Nov 04, 1995, Korea Inst. of Mach. & Metals Test report #s 95139250, 95139250-1, 95139250-2, & 95139250-3, dtd. August 7, 1995 and report dated December 19, 2000.

Pressure setting: 700-2100 mm H2O (1-3 psig), Vacuum setting: 344 mm H2O (0.5 psig).

This certificate supersedes approval number 162.017/144/2, dated January 28, 2006.

\*\*\* END \*\*\*

THIS IS TO CERTIFY THAT the above named manufacturer has submitted to the undersigned satisfactory evidence that the item specified herein complies with the applicable laws and regulations as outlined on the reverse side of this Certificate, and approval is hereby given. This approval shall be in effect until the expiration date hereon unless sooner canceled or suspended by proper authority.



GIVEN UNDER MY HAND THIS 17<sup>th</sup> DAY OF MARCH 2011, AT WASHINGTON D.C.

C. R. O'NEIL Assistant Chief, Tank Vessel and Offshore Division U.S. Coast Guard Marine Safety Center