

Ein modulares Messtechnik- und Prozess- steuerungssystem zur Optimierung der Betriebsführung von Großdampferzeugern

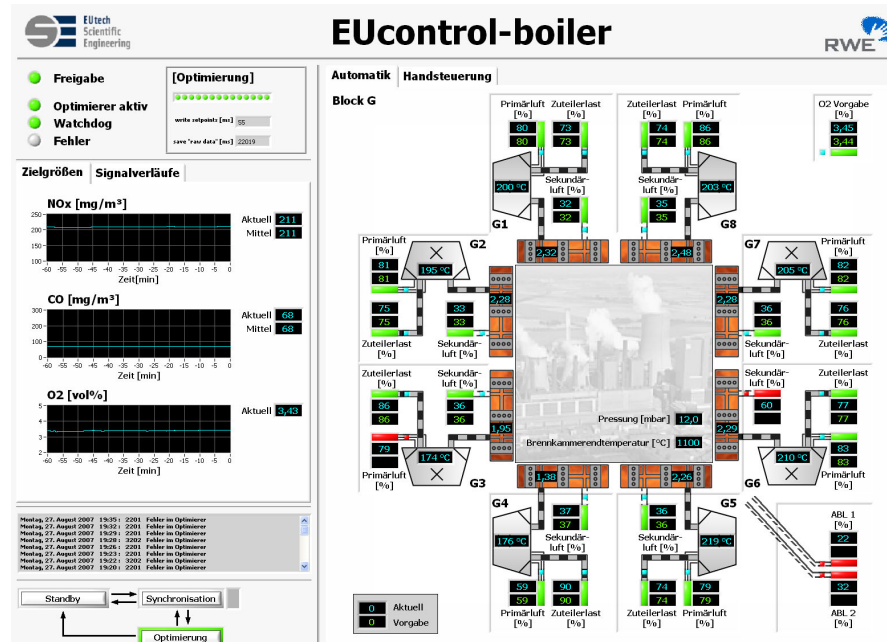
An advanced boiler monitoring and optimisation system

39. Dresdener
Kraftwerkstechnisches
Kolloquium
2007



Content

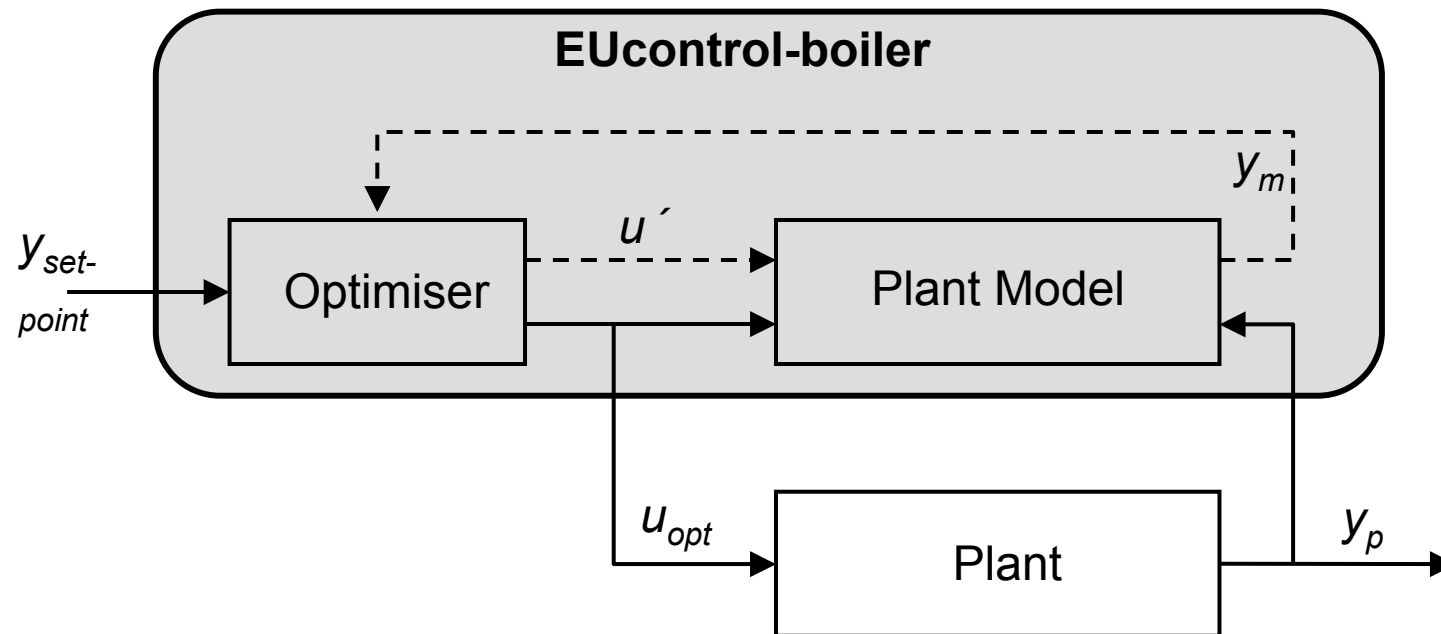
Modular, closed loop boiler optimisation



Content

- Which optimisation goals can be achieved with EUcontrol-boiler?
- What are the advantages of the modular approach?
- Which components can be integrated?

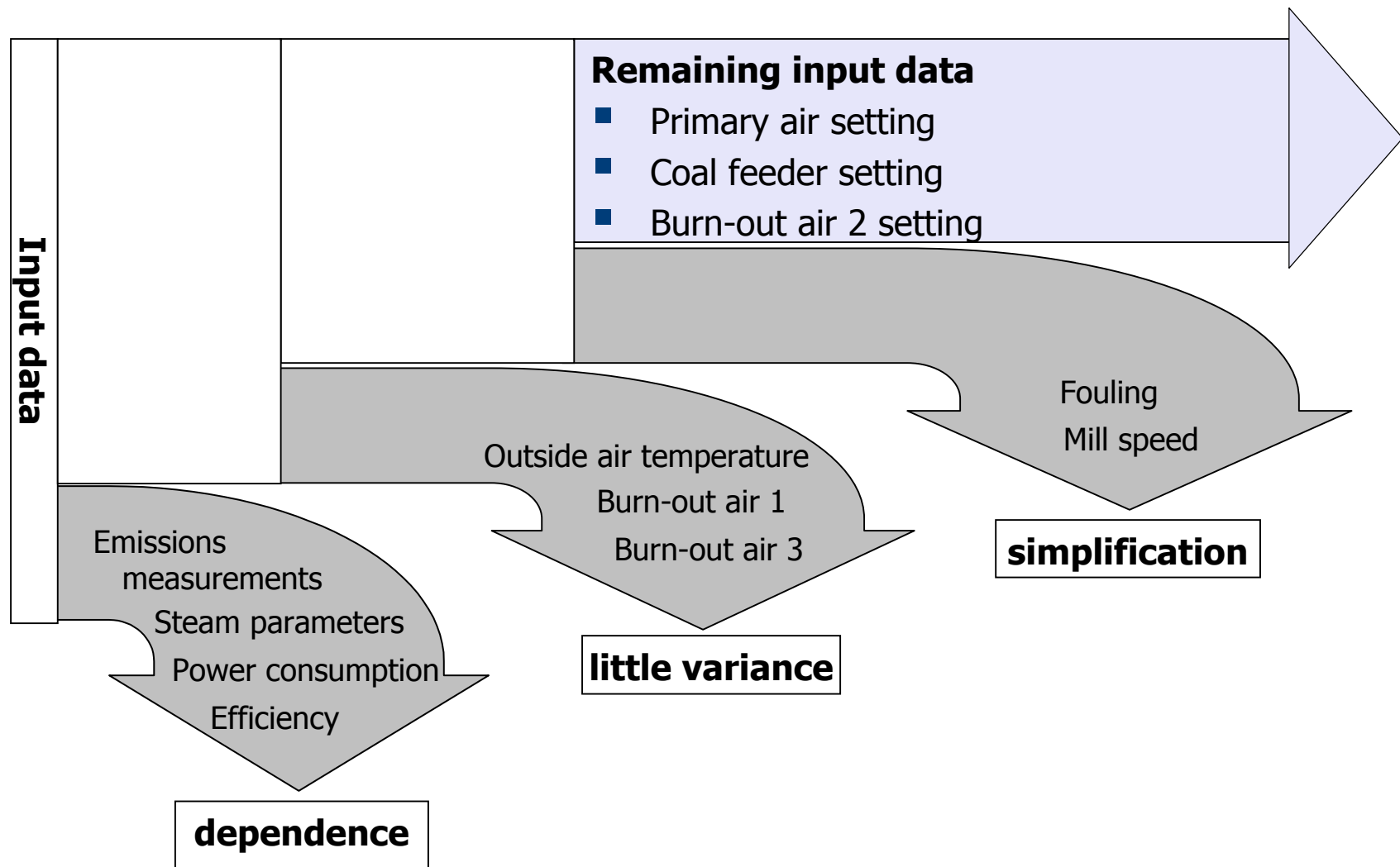
Structure of EUcontrol-boiler



The plant behaviour is predicted with an (identified) process model. An optimiser calculates the best possible combination of inputs.

Hard and soft constraints can be equally considered. Preferential adjustment of set-points is possible if the degree of freedom is sufficient.

Systematic reduction of input data



Plant model

INPUT (u)

1. Manipulated variables

- Primary air (1...8)
- Coal hopper (1...8)
- Σ Secondary air
- OFA 1
- OFA 2
- O₂ Excess

2. Measured (dist.)

- Output power
- Sooth blowers

3. Unmeasured (dist.)

- Coal quality

Plant model (Boiler)

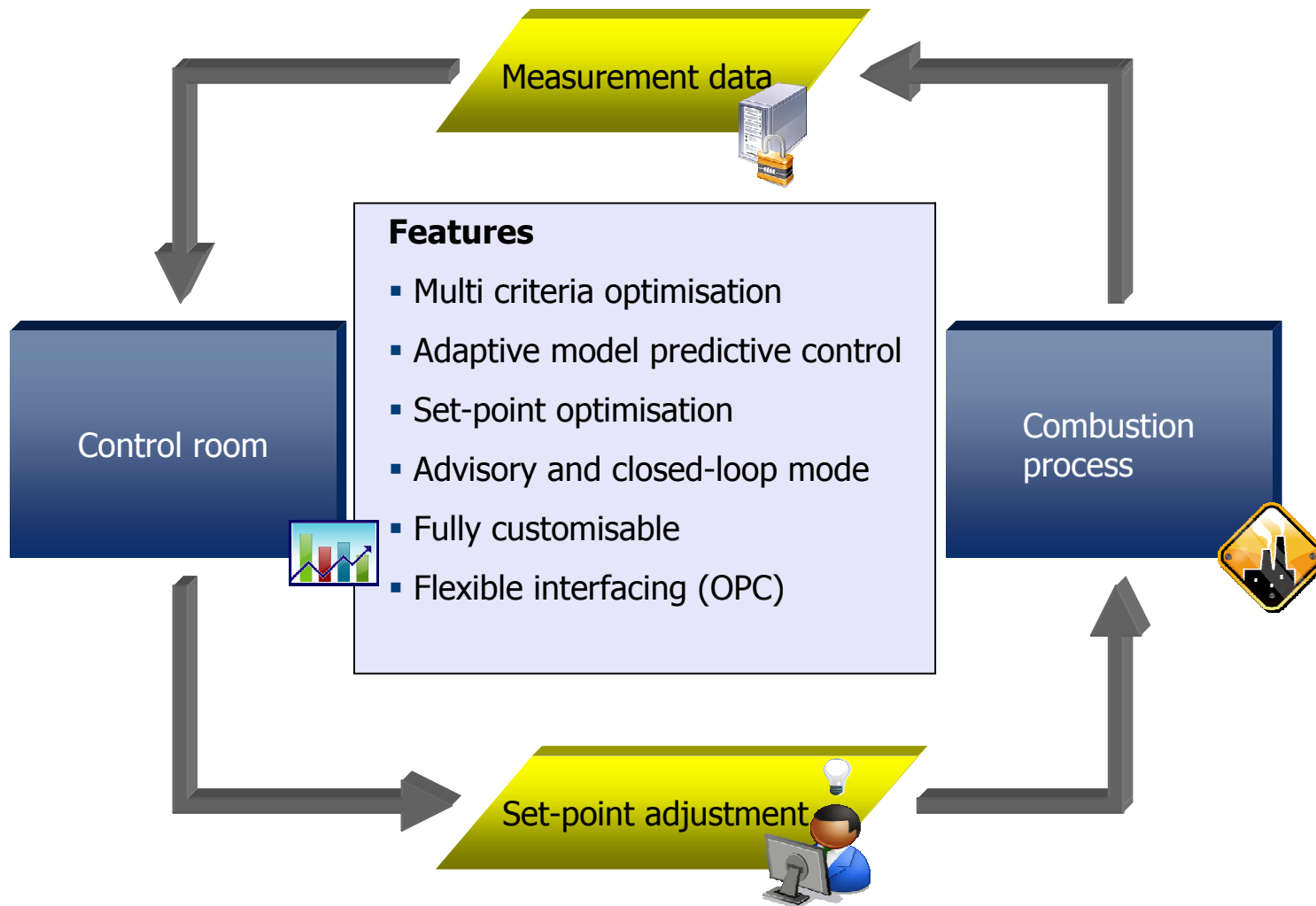
4. Constraints

- FD fan pressure drop
- Mill temperature
- Mill arrangement

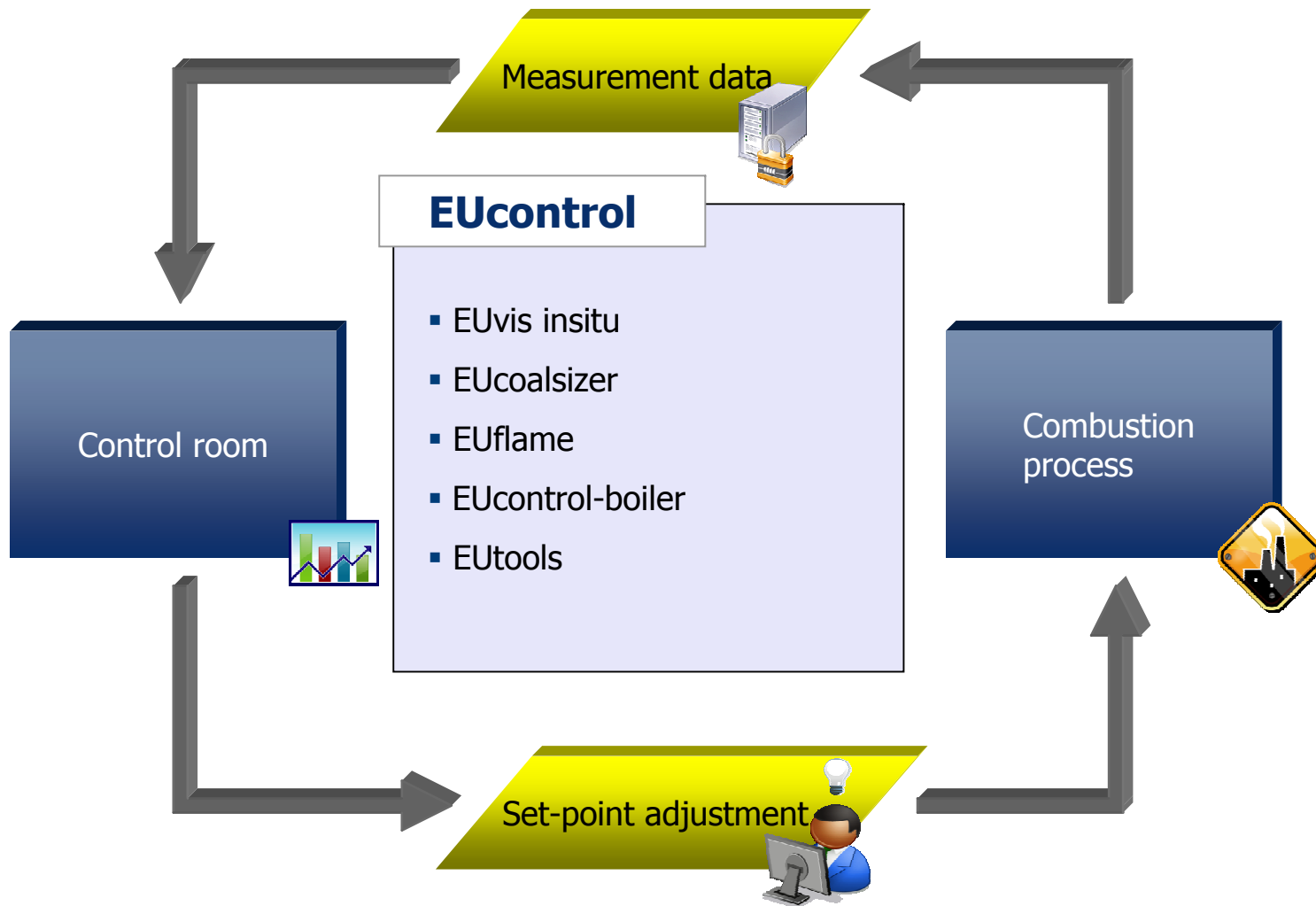
OUTPUT (y)

- NO_x
- T_{BK}
- CO
- σ_T
- T_{Mill} (1...8)

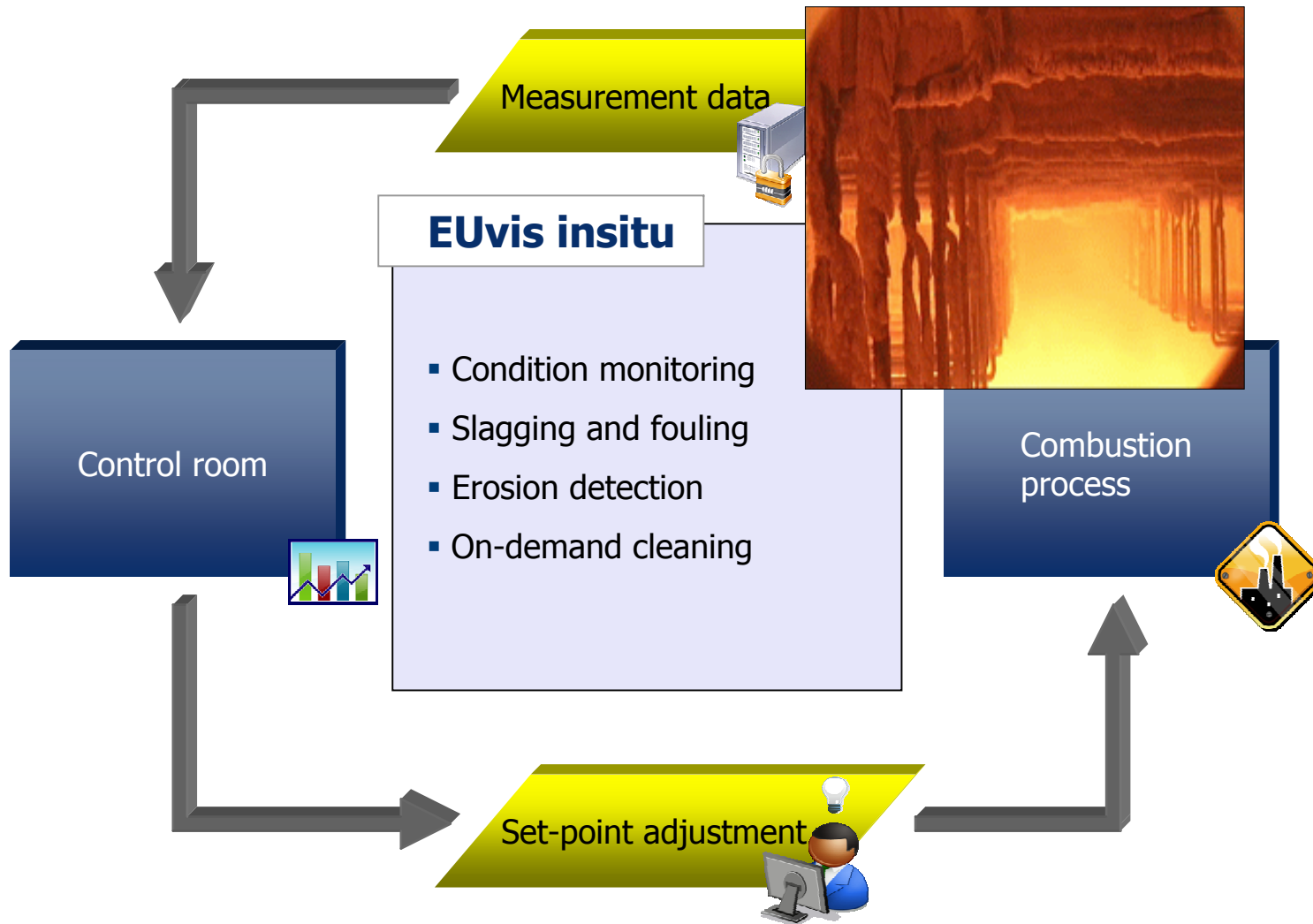
Main features



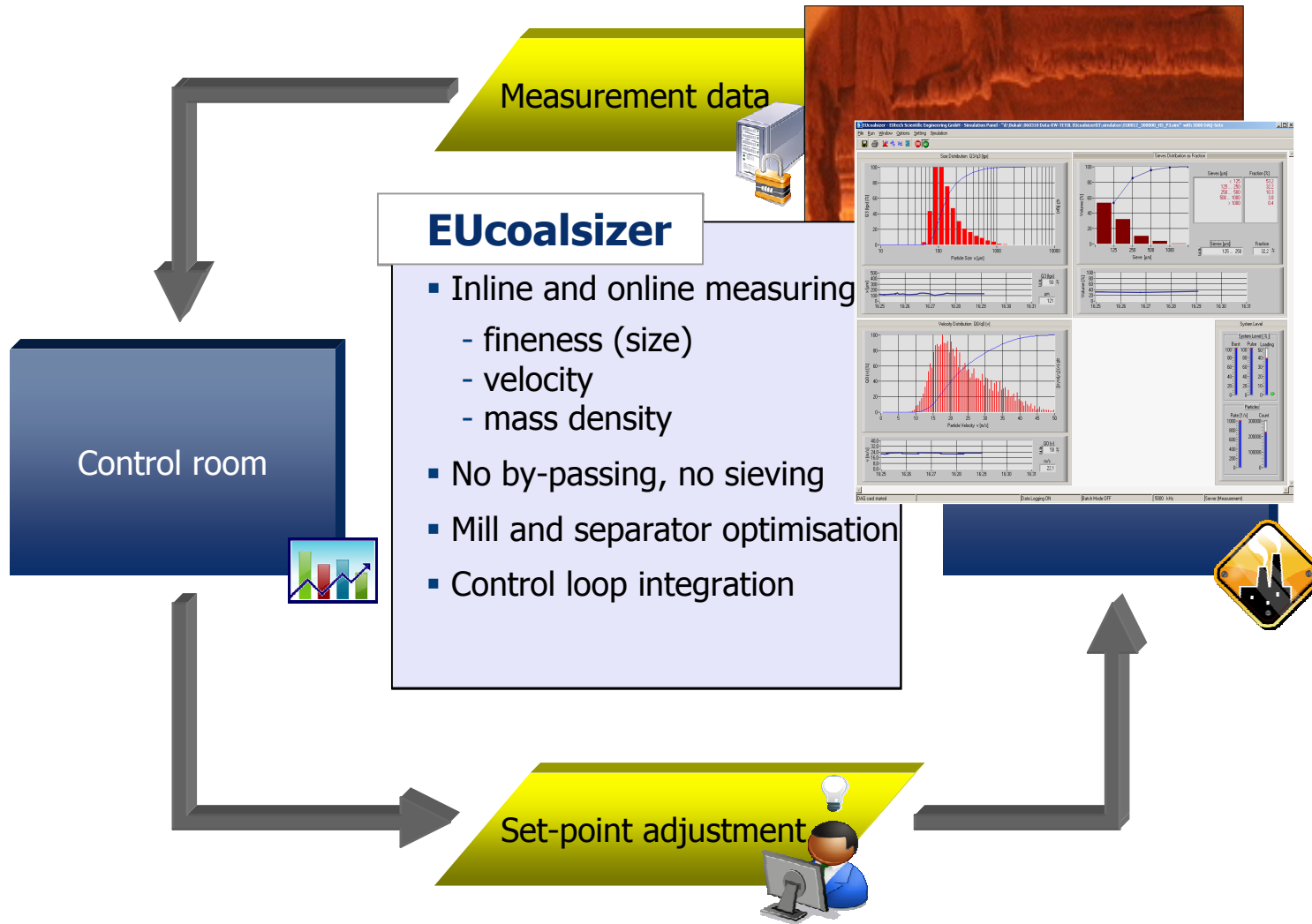
Seamless integration of tools



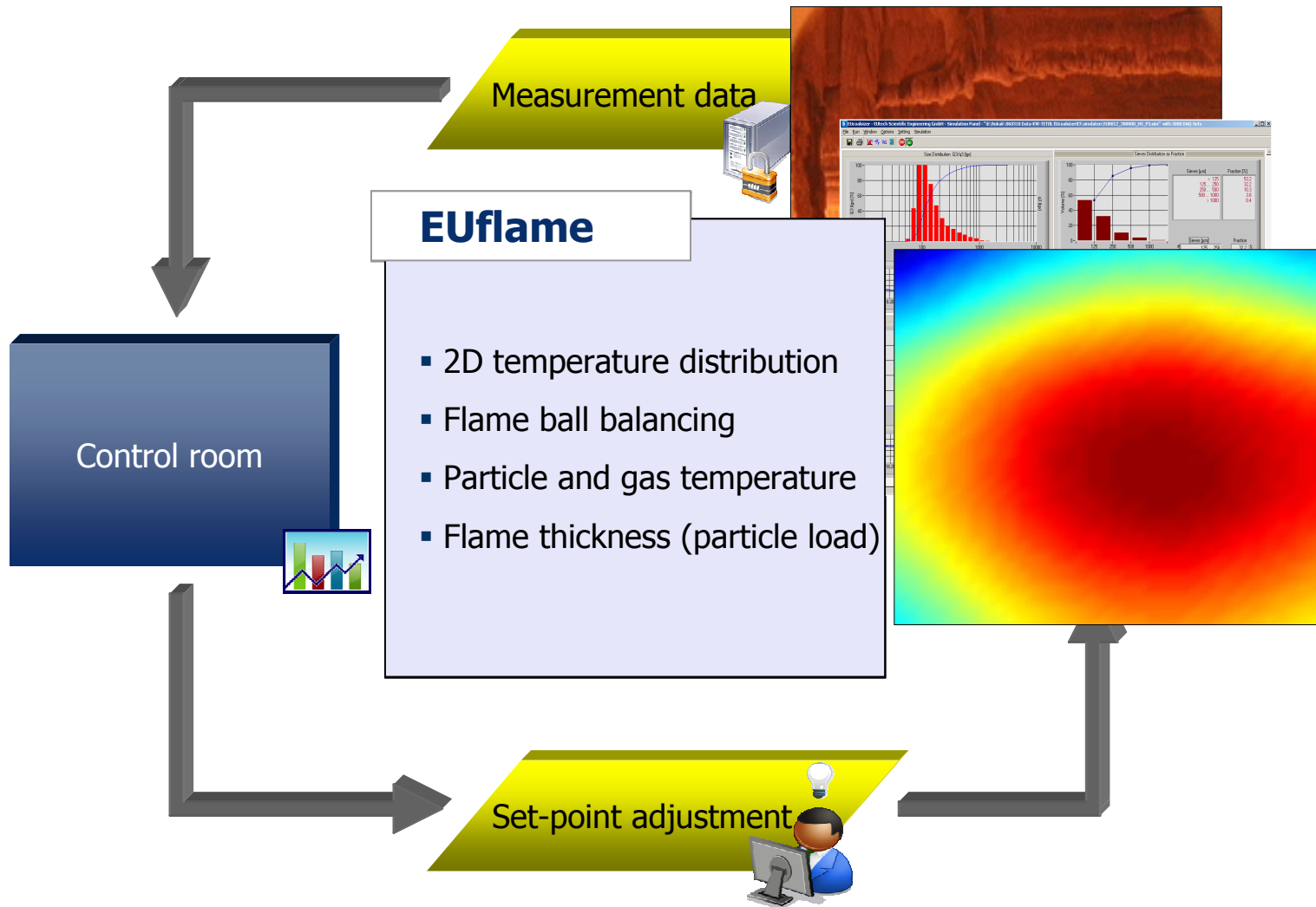
Seamless integration of tools



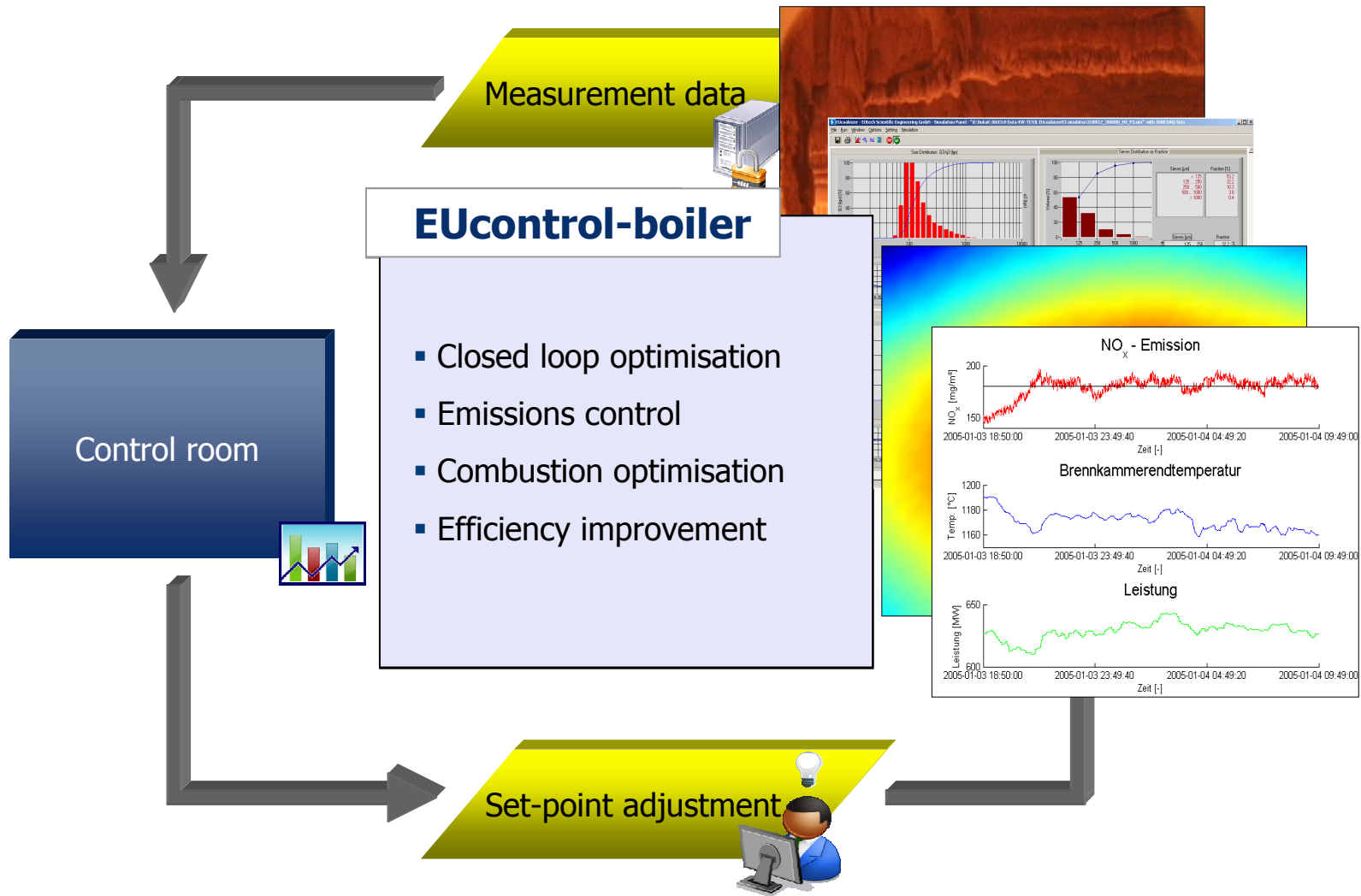
Seamless integration of tools



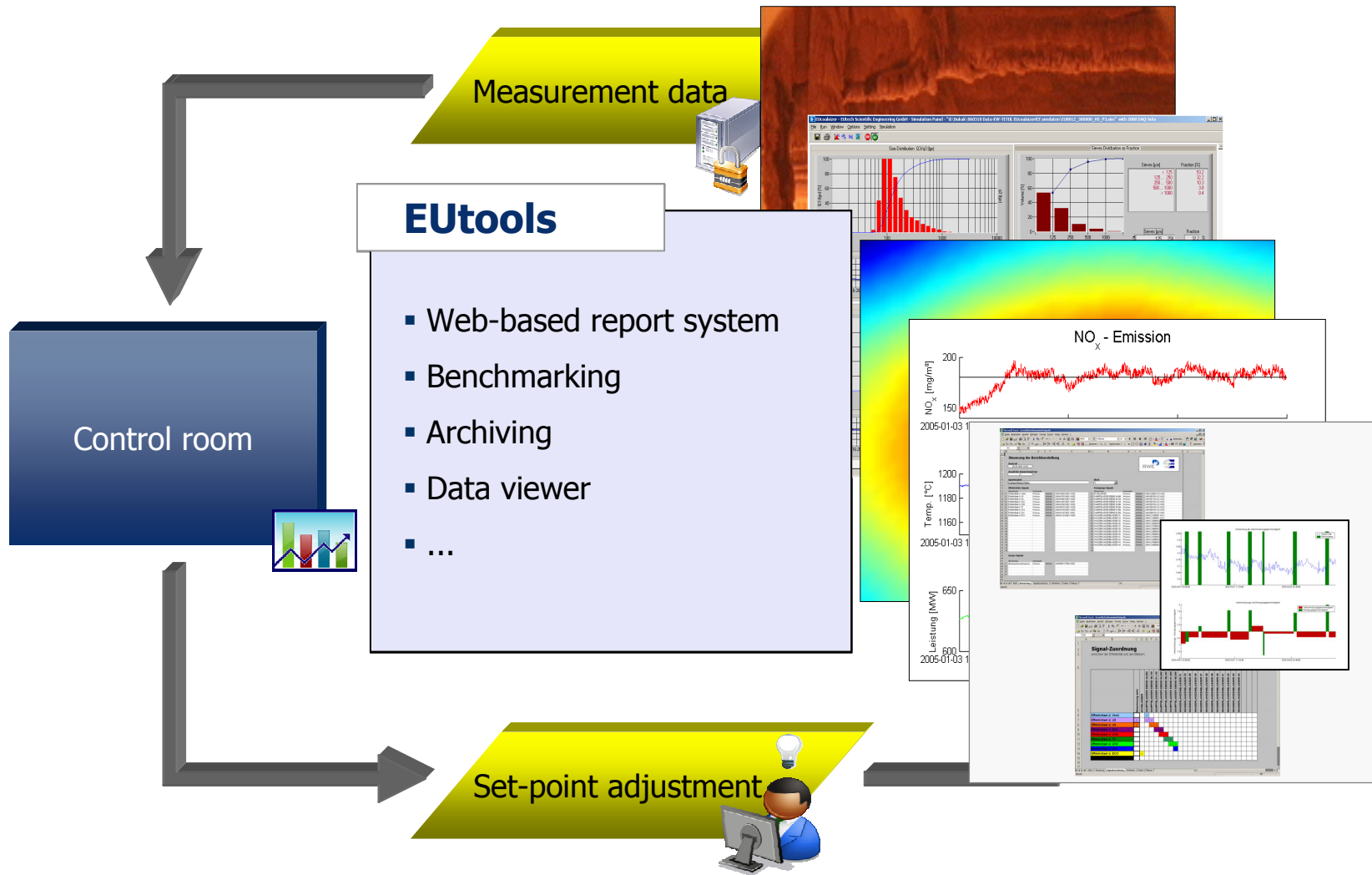
Seamless integration of tools



Seamless integration of tools



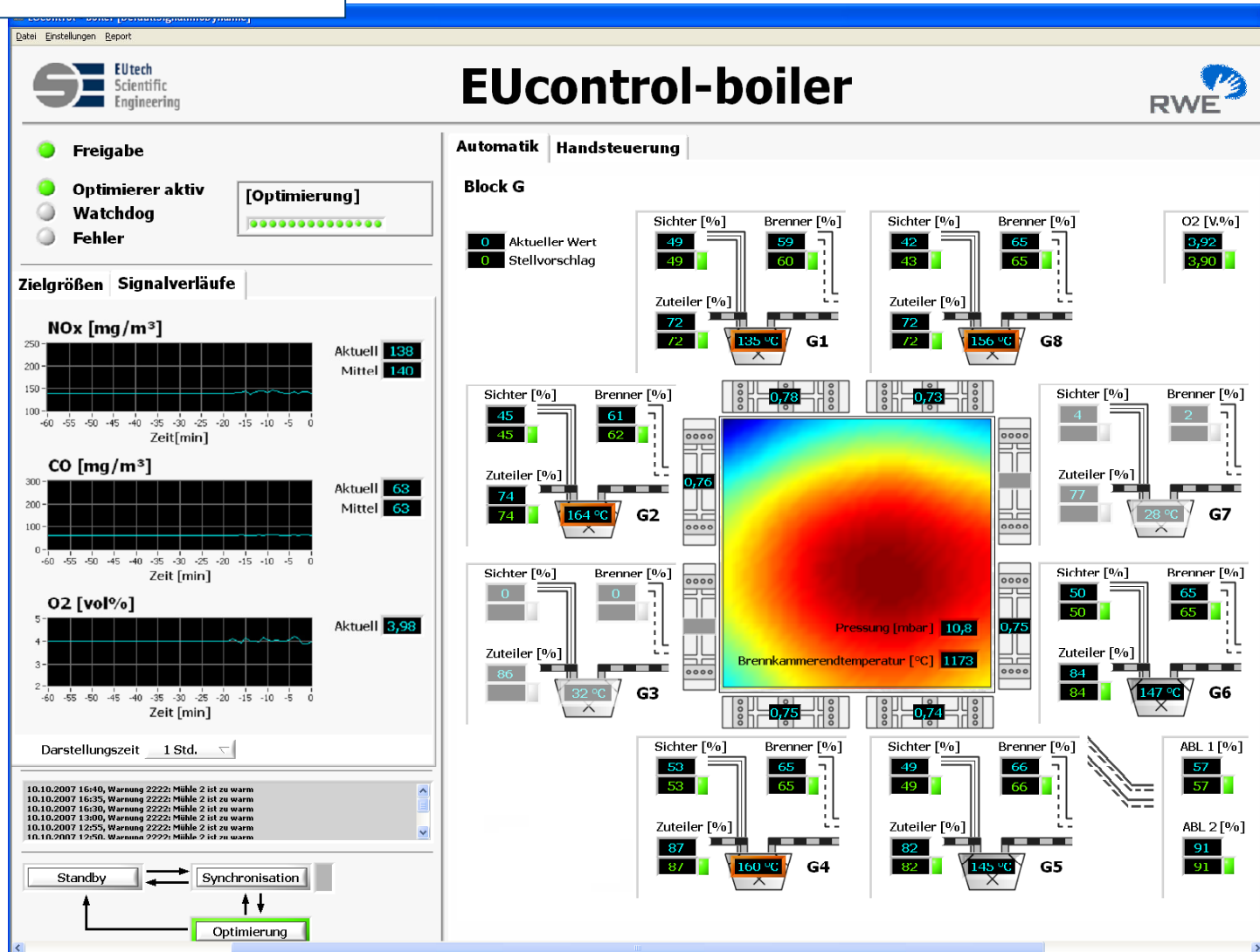
Seamless integration of tools



Snapshots ...

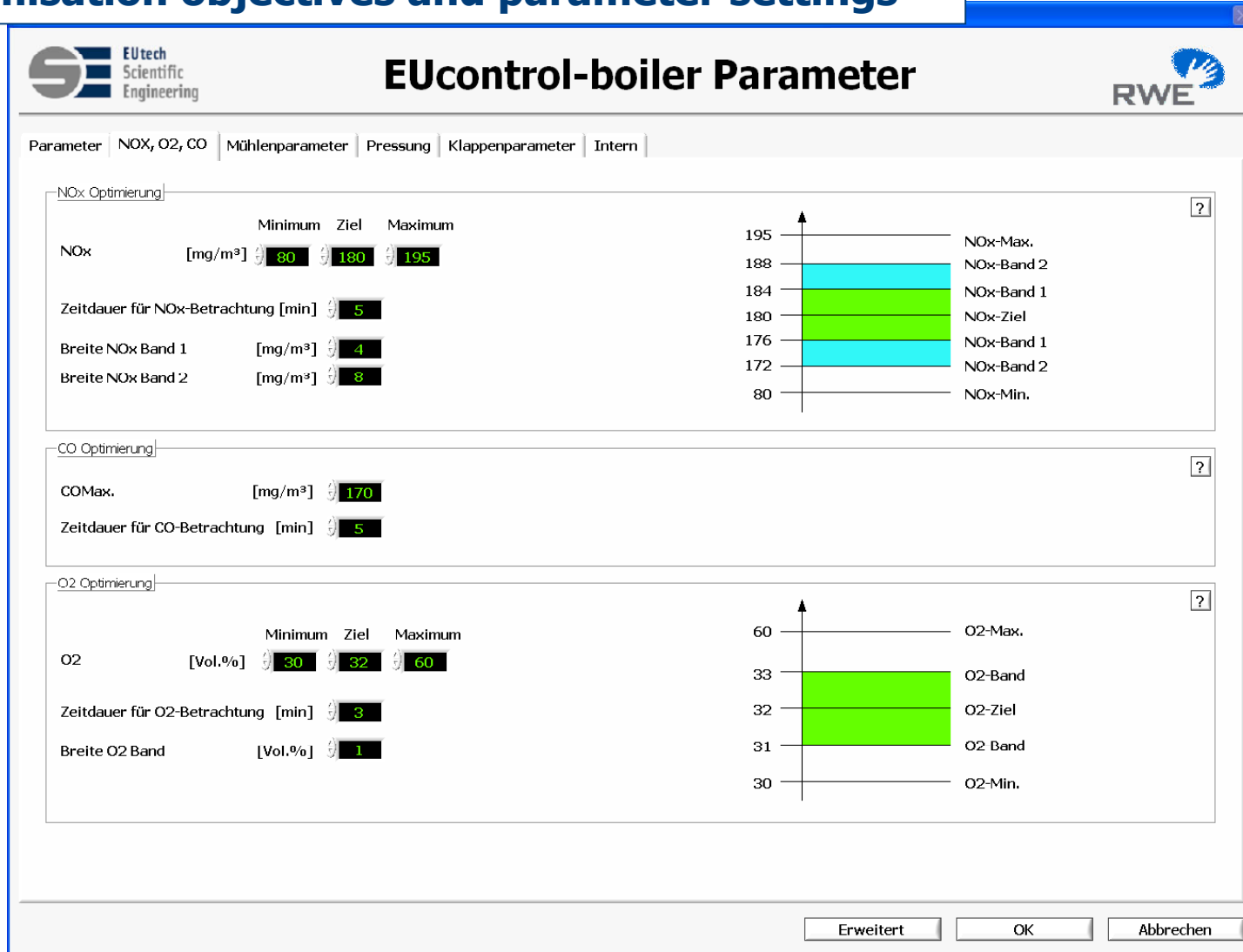
EUcontrol Boiler – Snapshots

Main user interface



EUcontrol Boiler – Snapshots

Optimisation objectives and parameter settings



The screenshot shows the 'EUcontrol-boiler Parameter' window. It has a tabbed interface with 'Parameter' selected. The window is divided into three main sections: NOx Optimierung, CO Optimierung, and O2 Optimierung. Each section contains input fields for various parameters and a corresponding graphical representation of the optimization bands and target values.

EUcontrol-boiler Parameter

Parameter | NOx, O2, CO | Mühlenparameter | Pressung | Klappenparameter | Intern

NOx Optimierung

Parameter	Minimum	Ziel	Maximum
NOx [mg/m³]	80	180	195

Zeitdauer für NOx-Betrachtung [min]: 5

Breite NOx Band 1 [mg/m³]: 4

Breite NOx Band 2 [mg/m³]: 8

Graphical representation of NOx optimization bands and target values:

- NOx-Max. (195)
- NOx-Band 2 (188 - 195)
- NOx-Band 1 (184 - 188)
- NOx-Ziel (180)
- NOx-Band 1 (176 - 180)
- NOx-Band 2 (172 - 176)
- NOx-Min. (80)

CO Optimierung

COMax. [mg/m³]: 170

Zeitdauer für CO-Betrachtung [min]: 5

O2 Optimierung

Parameter	Minimum	Ziel	Maximum
O2 [Vol. %]	30	32	60

Zeitdauer für O2-Betrachtung [min]: 3

Breite O2 Band [Vol. %]: 1

Graphical representation of O2 optimization bands and target values:

- O2-Max. (60)
- O2-Band (33 - 60)
- O2-Ziel (32)
- O2 Band (31 - 33)
- O2-Min. (30)

Buttons: Erweitert, OK, Abbrechen

EUcontrol Boiler – Snapshots

Defining damper and set-point constraints



EUcontrol-boiler Parameter



Parameter

Optimierungsziele

	Minimum	Ziel	Maximum
NOx [mg/m³]	80	180	195
O2 [Vol.-%]	30	32	60
CO [mg/m³]			170

Grenzwerte Mühlerntemperatur

	Minimum	Maximum
Mühlerntemperatur 1 [°C]	130	185
Mühlerntemperatur 2 [°C]	130	185
Mühlerntemperatur 3 [°C]	130	185
Mühlerntemperatur 4 [°C]	130	185
Mühlerntemperatur 5 [°C]	130	185
Mühlerntemperatur 6 [°C]	130	185
Mühlerntemperatur 7 [°C]	130	185
Mühlerntemperatur 8 [°C]	130	185

Grenzwerte Pressung

	Minimum	Maximum
Pressung [mbar]	11	19

Stellbereiche Luftklappen

	Minimum	Maximum
Primärluftklappe 1 [%]	30	80
Primärluftklappe 2 [%]	30	80
Primärluftklappe 3 [%]	30	80
Primärluftklappe 4 [%]	30	80
Primärluftklappe 5 [%]	30	80
Primärluftklappe 6 [%]	30	80
Primärluftklappe 7 [%]	30	80
Primärluftklappe 8 [%]	30	80
Sekundärluftklappe 1 [%]	35	95
Sekundärluftklappe 2 [%]	35	95
Sekundärluftklappe 3 [%]	35	95
Sekundärluftklappe 4 [%]	35	95
Sekundärluftklappe 5 [%]	35	95
Sekundärluftklappe 6 [%]	35	95
Sekundärluftklappe 7 [%]	35	95
Sekundärluftklappe 8 [%]	35	95
ABL1 Klappe [%]	15	60
ABL2 Klappe [%]	30	90

Stellbereiche Zuteiler

	Minimum	Maximum
Lastenteil Zuteiler 1 [%]	65	90
Lastenteil Zuteiler 2 [%]	65	90
Lastenteil Zuteiler 3 [%]	65	90
Lastenteil Zuteiler 4 [%]	65	90
Lastenteil Zuteiler 5 [%]	65	90
Lastenteil Zuteiler 6 [%]	65	90
Lastenteil Zuteiler 7 [%]	65	90
Lastenteil Zuteiler 8 [%]	65	90

Erweitert
OK
Abbrechen

Constraint definitions – pulveriser settings

EUcontrol-boiler Parameter

Parameter | NOX, O2, CO | **Möhlenparameter** | Pressung | Klappenparameter | Intern

Kalte Mühle

Sicherheitsbereich

Minimum Maximum

Kritischer Bereich

Minimum Mittel Maximum

	Temperaturen		Gradienten		
Mühle 1 [°C]	120	125	130	140	145
Mühle 2 [°C]	120	125	130	140	145
Mühle 3 [°C]	120	125	130	140	145
Mühle 4 [°C]	120	125	130	140	145
Mühle 5 [°C]	120	125	130	140	145
Mühle 6 [°C]	120	125	130	140	145
Mühle 7 [°C]	120	125	130	140	145
Mühle 8 [°C]	120	125	130	140	145

Heiße Mühle

Kritischer Bereich

Minimum Mittel Maximum

Sicherheitsbereich

Minimum Maximum

	Temperaturen		Gradienten		
	170	175	185	190	195
	170	175	185	190	195
	170	175	185	190	195
	170	175	185	190	195
	170	175	185	190	195
	170	175	185	190	195
	170	175	185	190	195
	170	175	185	190	195

Mühlentemperaturregelung

Interne Logik

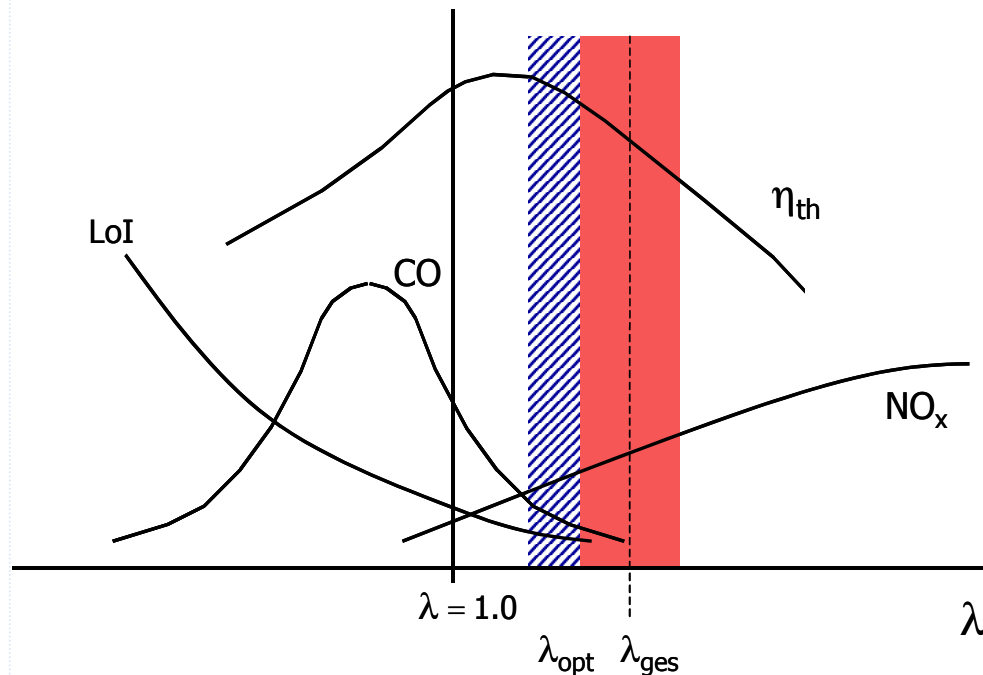
Erweitert

OK

Abbrechen

Concept of combustion optimisation....

Optimising Combustion



 Air/fuel ratio (λ) - range at optimised combustion settings

 Air/fuel ratio (λ) - range at regular combustion settings

- Combustion takes place at locally distributed microscopic scales
- Manipulated variables only adjust macroscopic parameters (e.g. overall excess air, mean temperature)
- Identify and utilise the intricate interplay of combustion parameters

Find the optimal trade-off for adjusting combustion parameters

Controlling NO_x, CO and fouling simultaneously

Strategy

- Possibility to reduce NO_x but often with a negative impact on CO, carbon-in ash (CIA) or fouling – multiobjective optimisation
- Countless possible settings of mill combinations, fuel distribution, O₂ levels and damper settings – each with different NO_x, CO and fouling gradient
- Main objective is to identify the unit specific outcomes for different settings and advise on the optimal, overall set-up
- No major modification of plant DCS as only (independent) setpoints are adjusted
- Open loop operation provides advice for operation strategy, in closed loop biases are directly controlled
- Individual adaptation to a wide range of objective functions, plant types and constraints

Case study I: Avoiding slagging and increasing efficiency ...

Avoiding slagging and increasing efficiency

- Investigations show that an increase of surplus O₂ at burner level reduces slagging
- Low temperatures at the end of the combustion chamber avoid melting of ash and glassification
- The homogenisation of combustion conditions (air-fuel ratio) at burner level improves burn-out and reduces slag formation
- Reducing excess O₂ while simultaneously reducing CO improves efficiency

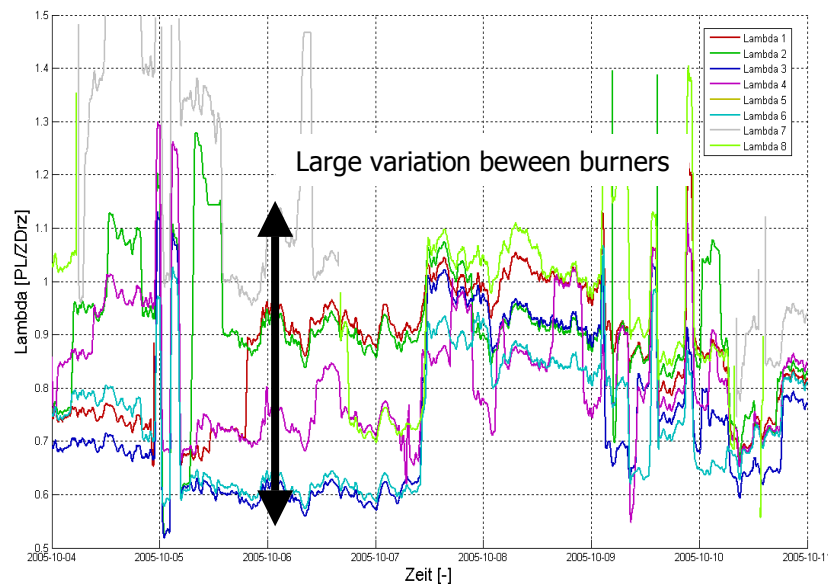


Simultaneous optimisation of a multitude of combustion objectives
(NO_x, TBK, CO, O₂) -> multi-criterial optimisation!

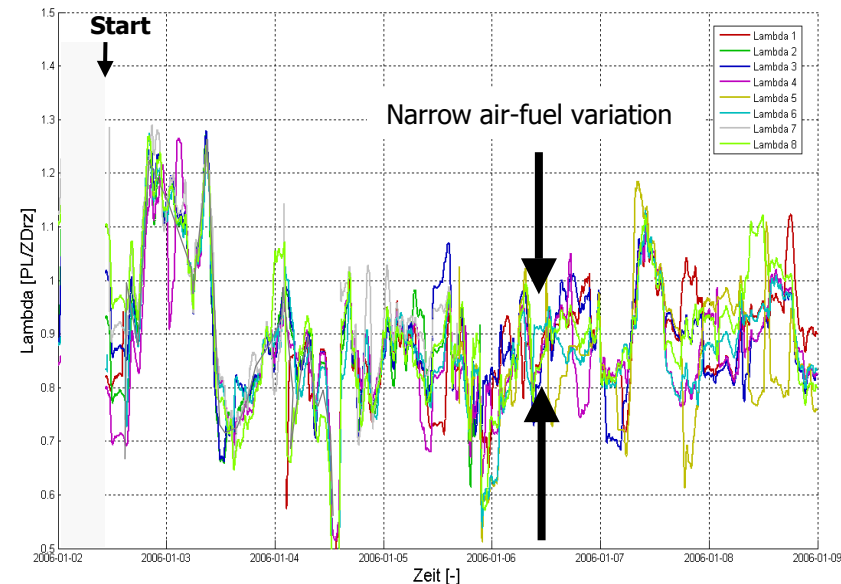
Air fuel balancing at individual burners

- The combustion is homogenised in the “horizontal” burner plane for every time step
- Primary air damper influences the mill temperatures and the air pressure drop
- Coal feeder RPM has an effect on mill temperatures, too
- Intelligent control required

Air-fuel ratio without EUcontrol-boiler

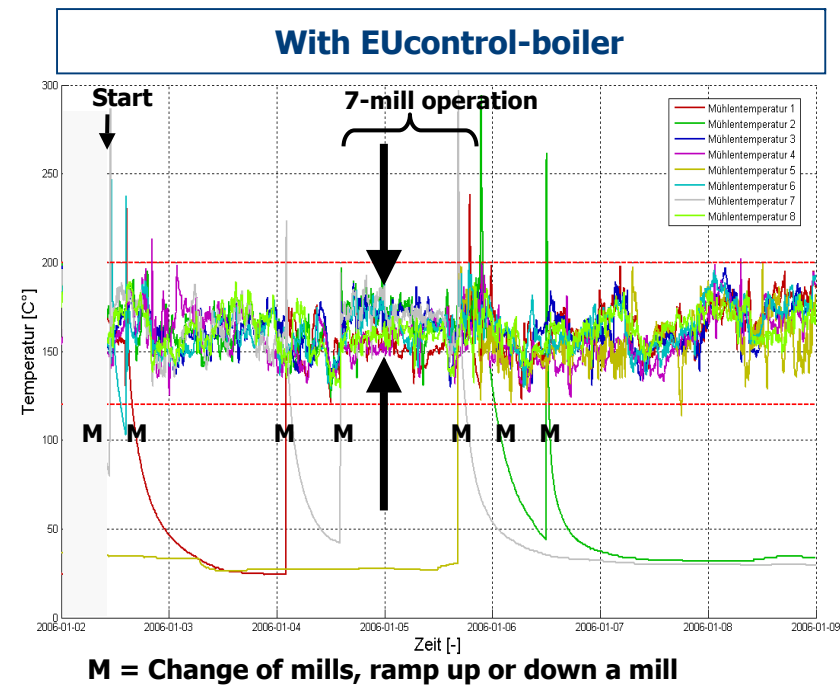
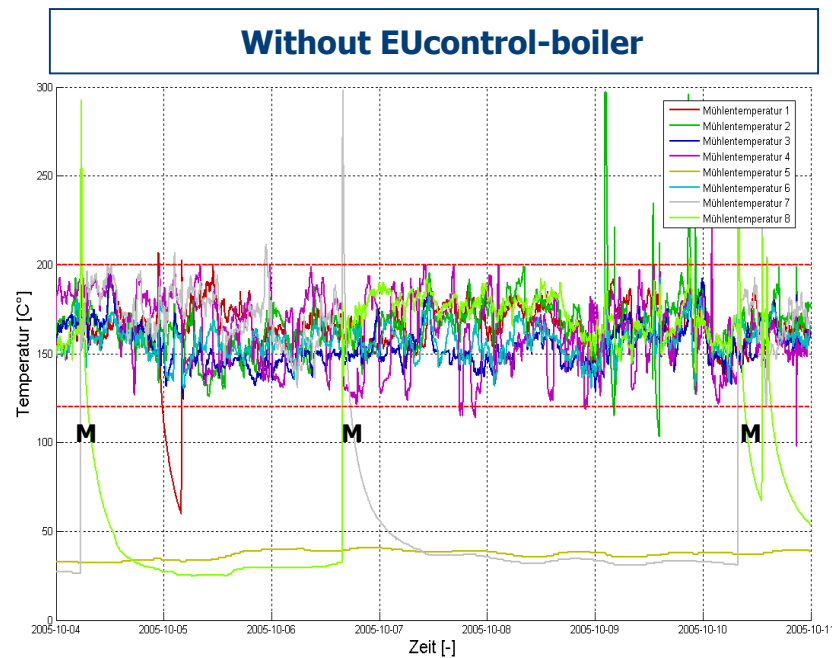


Air-fuel ratio with EUcontrol-boiler



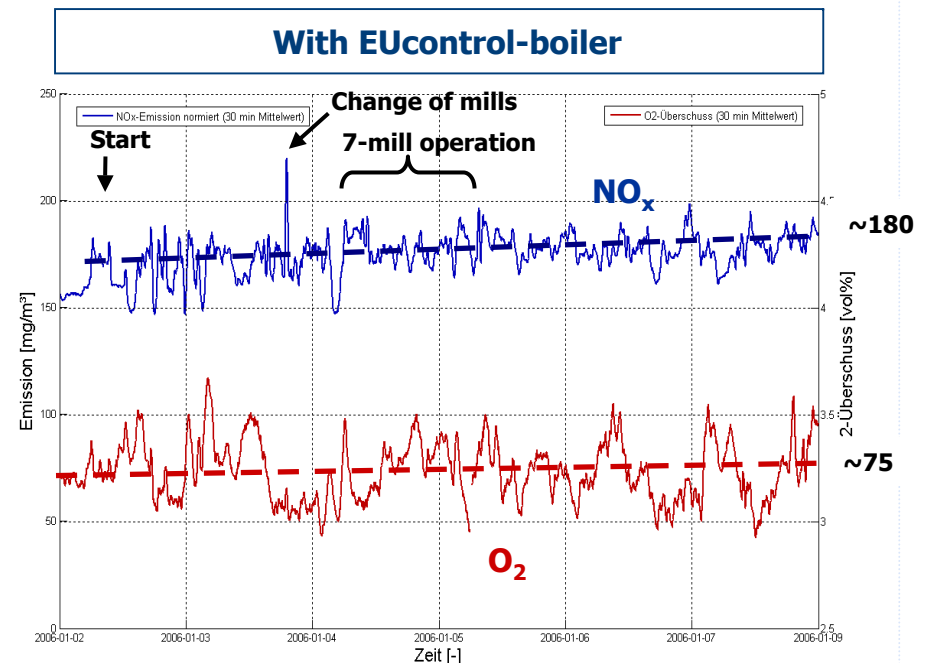
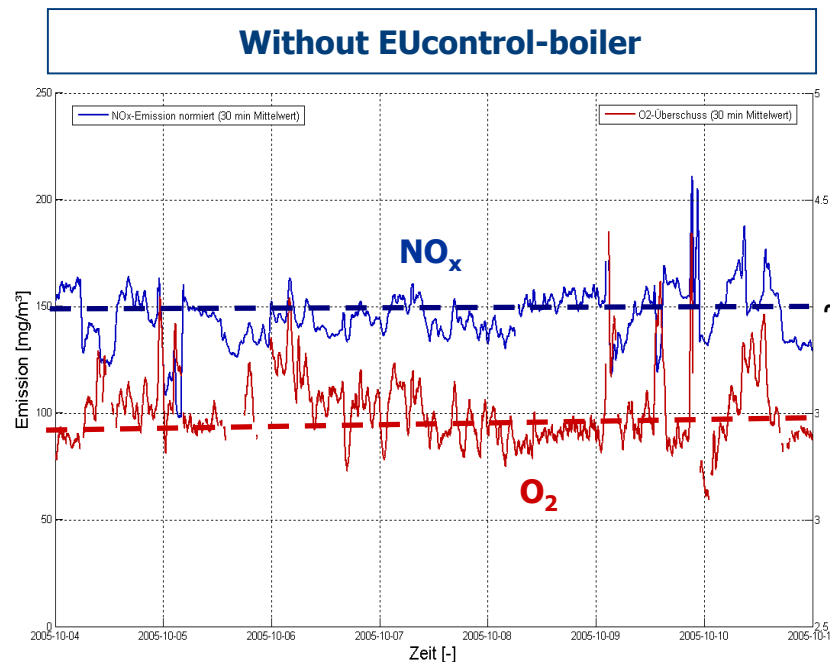
Mill temperature

- The mill temperature is controlled through primary air settings, coal feeder and mill speed. In this case it should be between 120°C - 200°C.
- Primary air affects the air-fuel ratio and the pressure distribution in the boiler
- The speed of the coal feeder affects the air-fuel ratio



NO_x and O₂

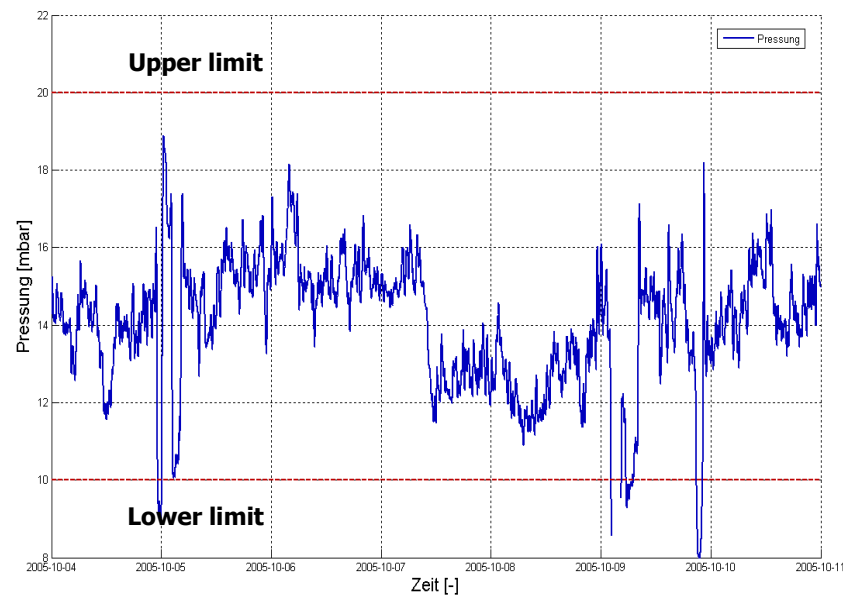
- Combustion and burn-out are improved by opening primary and secondary dampers
- As more oxygen enters at the burner level NO_x is increased to an adaptive set-point well below the emission allowance (200 mg/m³) → NO_x level becomes an indicator for good burn-out
- Simultaneously the excess air was reduced !



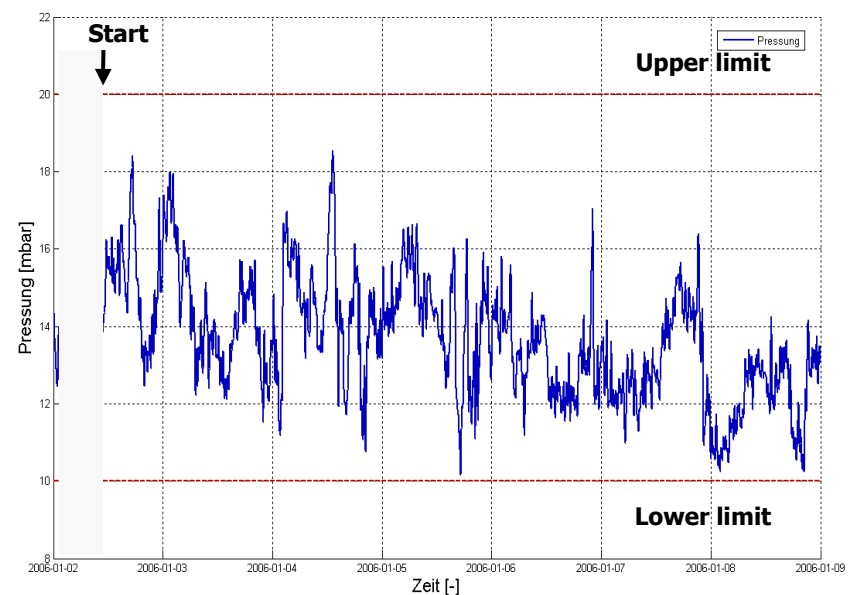
Pressure drop ID fan

- Many operational constraints must be considered while optimising combustion
- The air pressure drop is influenced by damper interaction: primary, secondary and over- fire air and ID fan setting
- The pressure limits can be parameterised

Beispiel KW40/2005: Pressung ohne EUcontrol-boiler



Beispiel KW01/2006: Pressung mit EUcontrol-boiler



Result

- Slagging and fouling of boiler walls significantly reduced
- Forced outages due to excessive on-load cleaning are at a minimum
- CO emissions reduced indicating improved burn-out
- NOx level reliably below allowance level
- Mills operated close to optimal conditions
- Balanced temperature profile reducing material stress
- Reduced level of excess O2 improves efficiency
- Operator can select combustion strategy according to situation

Case study II: Minimising furnace temperature imbalances

Minimising furnace temperature imbalances

- Asymmetric mill or burner arrangement, unequal burner loads or damper settings may bias temperature profile at furnace exit
- Non-centred flame ball leads to material stress and can cause slagging problem
- Asymmetric temperature profile at furnace exit leads to steam temperature differences in boiler sections that have to be compensated by spray water
- Spray water reduces boiler thermodynamic efficiency

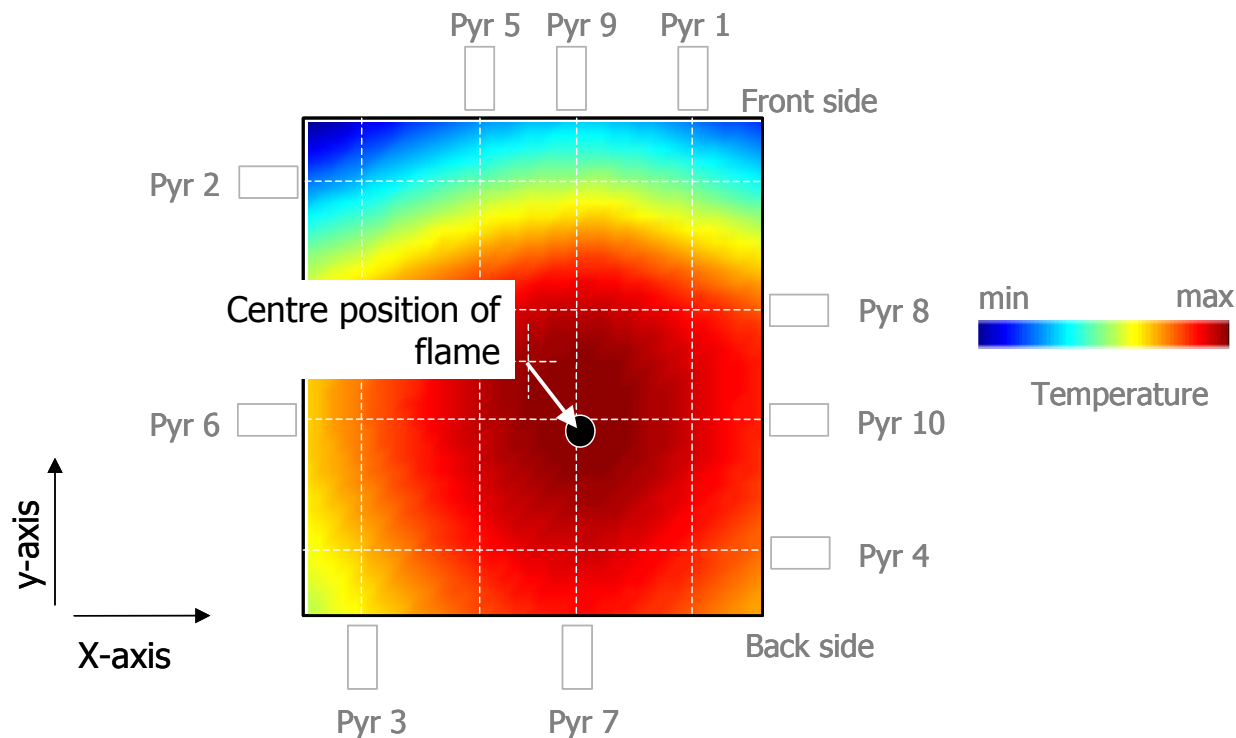
Definition of task

- Reduction of the temperature difference of four given temperature measurements (4 „AGAM zones “) in a large scale utility boiler (> 900 Mwe)
- Additional optimisation tasks (partly correlated):
 - CO (minimise)
 - Average O₂-level at the end of boiler (minimise)
 - O₂- deviation at the end of boiler (minimise)
 - Overall boiler efficiency (maximise)

Solution – Measuring temperature distribution

EUflame-2D

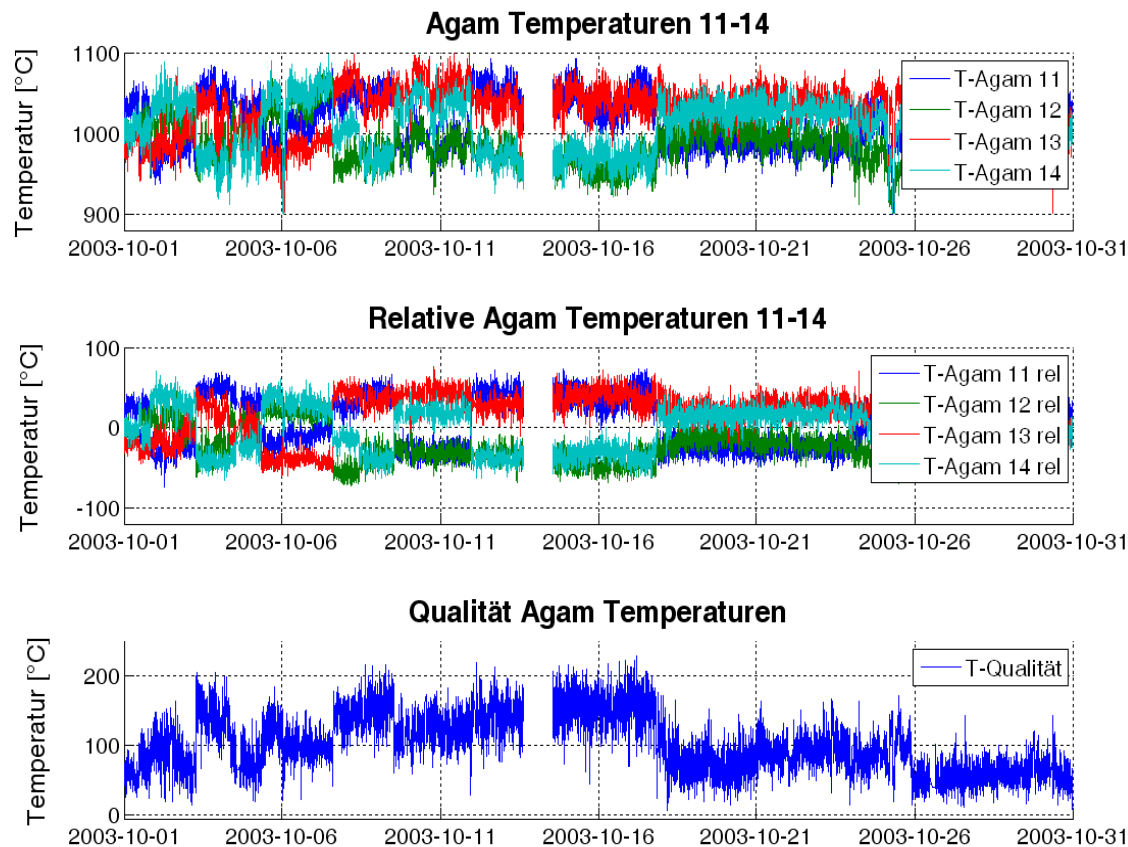
- Direct measurement of furnace exit gas temperature (FEGT) distribution
- Flame characterisation via mean value and standard deviation (max/min) of temperature and flame ball position (centre of flame)



Minimising temperature variation

Primary optimisation goal

Minimisation of FEGT temperature variation ("Agam" zones)



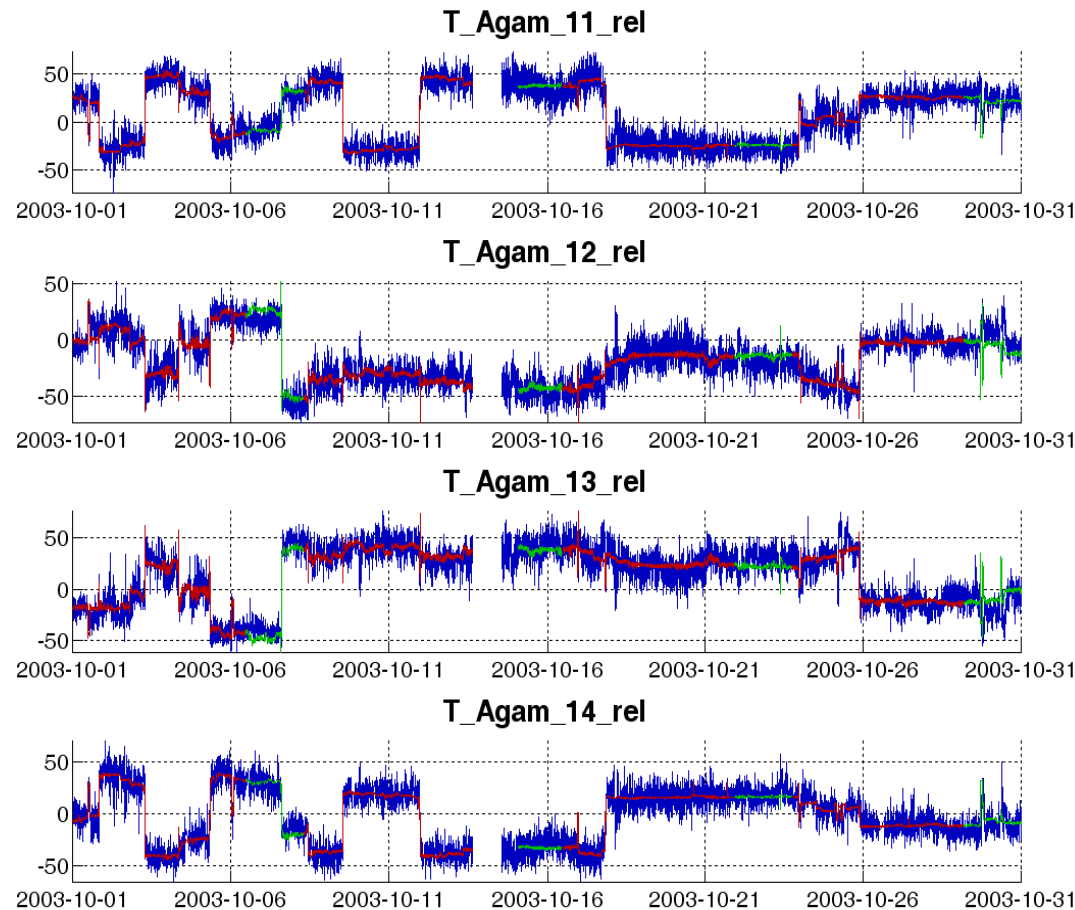
Relative temperatures

$$T_{AGAM\ rel,i} = T_{AGAM,i} - \overline{T_{AGAM}}$$

Temperature „quality“

$$T_{AGAM\ qual} = \sum |T_{AGAM\ rel,i}|$$

Model of temperature variation

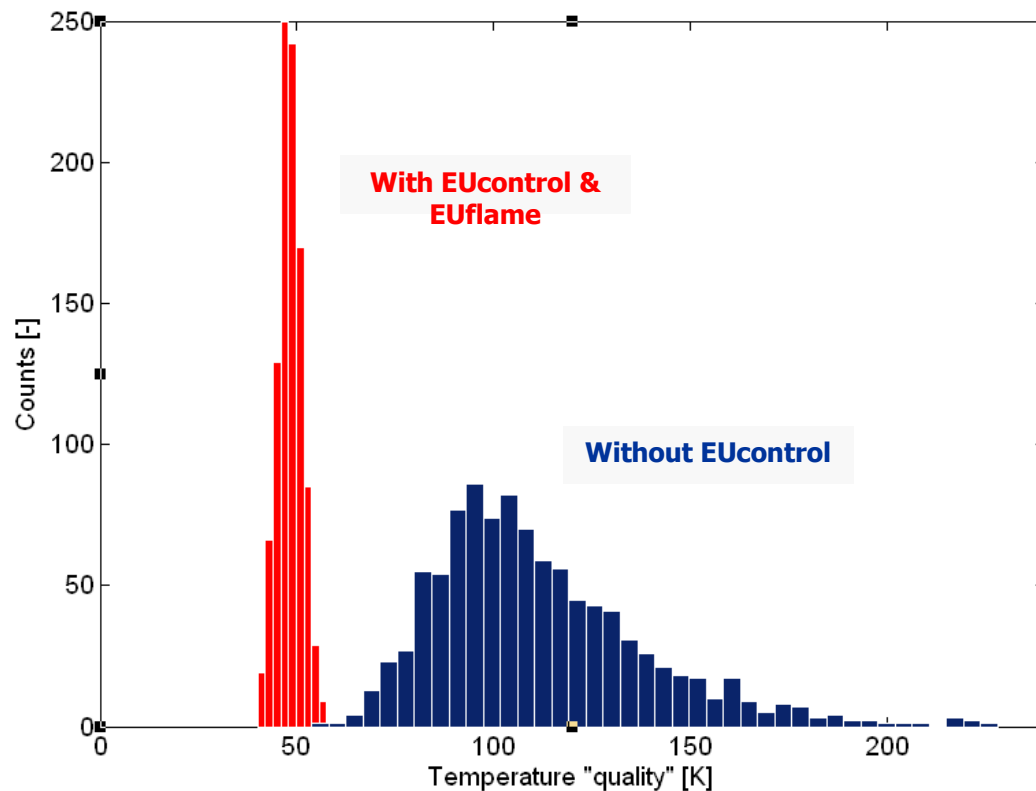


- Input data: Relative inputs
- Output data: Relative temp.
- Properties: Prognosis model of all available data sets
- Conclusion: Good model quality. Model can be directly use for optimisation.
- Quality: 92 %

— Original temperature
— Temperature during model generat.
— Temperature during model validation

Optimisation - results

Result of optimised settings (optimisation goal)



- Temperature quality = $\Sigma |T_{AGAM\ rel,i}|$
- Significant improvement of temperature quality through optimisation

Summary....

Benefits ...

- EUcontrol-boiler is an optimal cost-value ratio option for producing sustained boiler operation under desired conditions (low NOx, reduced slagging, high efficiency)
- No modification of plant DCS system required
- Highly adaptive, automatically adjusting to changing situations
- Multivariate target optimisation (low NOx AND low fouling AND high efficiency)
- Customisable to individual plant requirements

... leading to a new value proposition

- Consideration of different operational objectives (technical, commercial, environmental)
- Offering an attractive means to upgrade older boilers at low cost
- Straightforward implementation at lowest risk (model based)